



**CDM
MONITORING REPORT # 30
of
“N2O Emission Reduction in Paulinia,
SP, Brazil”
UNFCCC 0116**

Revision 1

**From: October 14, 2009
To: November 18, 2009**

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Date: November 23rd, 2009

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1 Introduction

The purpose of this monitoring report is to calculate and clarify GHG emission reduction quantity achieved by this project for periodic verification.

This monitoring report covers the activity from October 14th, 2009 to November 18th, 2009 as the 30th period.

Duration of the project activity period

The starting date of the project is defined as 11/19/2006.

Note: In the PDD the original starting date of the project activity is 01/01/2007. A demand to the UNFCCC for anticipating the actual start up of the project activity to 11/19/2006 was made and approved. The new starting date of the project activity has been updated on the UNFCCC website.

2. Reference

Approved Baseline methodology :

Baseline Methodology for decomposition of N₂O from existing adipic acid production plants (AM0021/version 1)

Approved Monitoring methodology :

Monitoring Methodology for decomposition of N₂O from existing adipic acid production plants (AM0021/version 1)

Project Design Document :

N₂O Emission Reduction in Paulinia, SP, Brazil.

Version number of the document : 4

Date : October 12th, 2005

CDM registration number :

“N₂O Emission Reduction in Paulinia, SP, Brazil” – UNFCCC ref number 0116

Directly related EB guidance:

EB45 Annex13 “Guidance to calculate adipic acid production in cases where it cannot be measured directly” version 1, February 13th 2009

3. Definition

y : Monitoring period (in this report, see dates § 1)

PDD : Project Design Document of this project “N₂O Emission Reduction in Paulinia, SP, Brazil.” Version number of the document: 4, issued on October, 12th, 2005



4. General description of project

4.1 Project activity

Nitrous oxide (N₂O) is a by-product of adipic acid production. It is of low toxicity but is a greenhouse gas (GHG), whose GWP is large (GWP=310 in the IPCC 2nd Assessment Report). Emissions of N₂O will be controlled under the Kyoto Protocol. As far as we are aware, there are however no national or regional regulations or restrictions on the emission of N₂O in Brazil. There are in fact no governmental regulations with quantified emission limits in any non-Annex I countries at this point.

In this project, Rhodia Poliamida e Especialidades Ltda. additionally installed N₂O collection and a thermal decomposition process equipment to the currently operating adipic acid manufacturing plant. This installation reduces the GHG emissions, which would otherwise be released to the atmosphere if the project were not implemented.

The decomposition facility was installed in the factory site of Paulinia Rhodia Poliamida e Especialidades Ltda. in October 2006 and destruction of N₂O was started in November 2006. The starting date of the project as well as the starting date of the first crediting period is defined as November 19th, 2006. It should be noted that the original starting date of the project activity is 01/01/2007 according to the PDD. However the start up of the project activity was anticipated to 11/19/2006, as formalized to and approved by the UNFCCC.

This project activity was registered at UNFCCC on December 25th, 2005 with the number 0116.

4.2 Technical description of the project

Location of the project activity

The decomposition facilities were installed in the factory site Rhodia Poliamida e Especialidades Ltda in Paulínia, SP, Brazil in October, 2006.

Technology employed by the project activity

A thermal oxidizer with 2 chambers is the technology used to decompose N₂O.

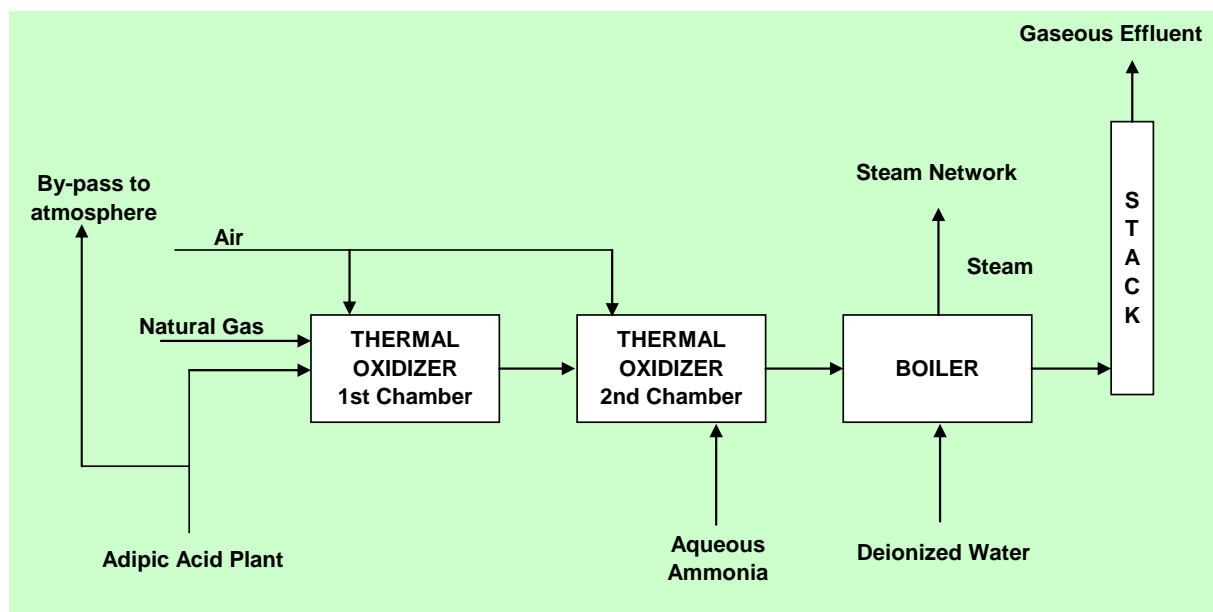
Natural gas is fed with the off gas adipic acid production containing N₂O and some air in a reduction chamber, where it burns (oxidizes) to carbon dioxide CO₂ and water vapour. N₂O is used as an oxidizer. Being oxygen deficient, the oxidation is not complete and carbon monoxide and hydrogen are present.



The temperature in the furnace is kept at about 1300°C and under fuel rich conditions, so as to promote the complete decomposition of N₂O while minimizing the formation of unwanted combustion by-products such as NO and NO₂.

The gas is then quenched with air to complete the combustion of carbon monoxide and hydrogen at a temperature of about 950°C in a second chamber. Aqueous ammonia is injected to control the emission of NO and NO₂.

Before release to the stack, the flue gas coming from the thermal oxidizer is used to produce superheated steam, which is fed into the existing on-site steam network.



4.3 Implementation of the project

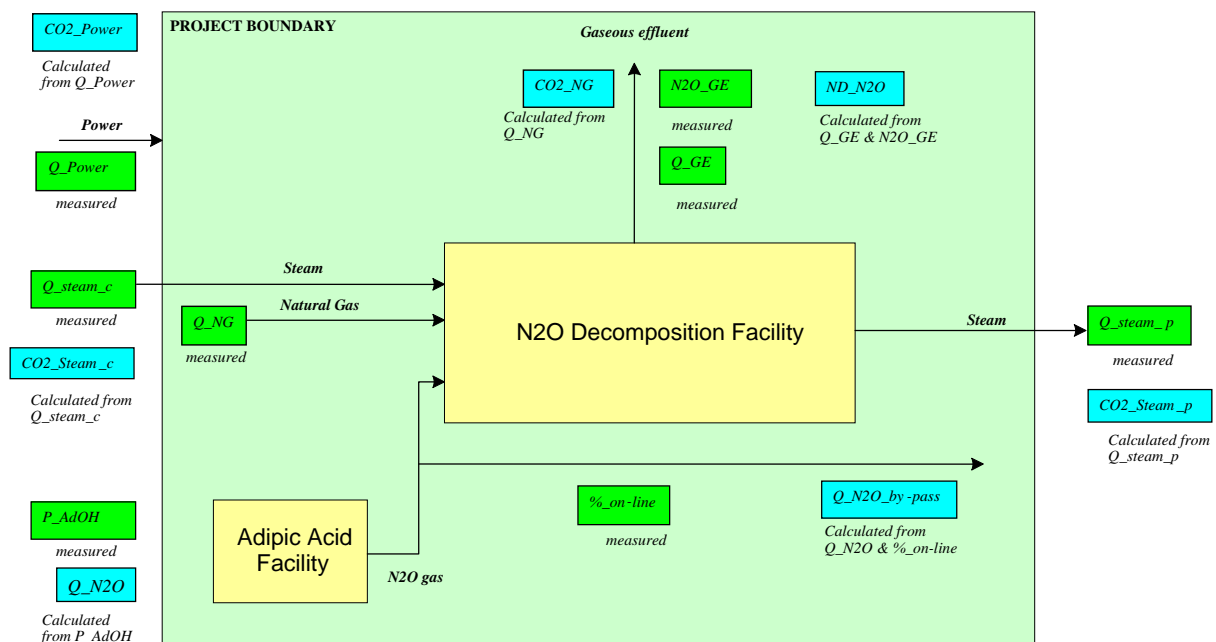
The project is fully implemented according to the description presented in the PDD. The project activity is completely operational.

5. Baseline methodology

Approved baseline methodology AM 0021 / version 1: “Baseline methodology for decomposition of N₂O from existing adipic acid production plants” is applied to this project.

The project boundary related to the baseline methodology is shown below and this project boundary is used and explained in the PDD.

Potential sources of anthropogenic emissions by sources of GHG within the project boundary and emissions which are not included in the project boundary are also shown in below.



6. Applicability of the methodology

Approved monitoring methodology AM 0021 / version 1 is applied to this project.

This methodology is applicable to projects which decompose N₂O from an adipic acid production plant under the following conditions:

- either catalytic or thermal decomposition of the N₂O by-product of adipic acid production at existing production plants
- The methodology is spatially generic, being applicable across regions where the data (both related and project activity as well) exist to undertake the assessment
- The methodology is applicable only for installed capacity (measured in tonnes of adipic acid per year) that exists by the end of the year 2004.

The present project satisfies these conditions as:

- Thermal decomposition of the N₂O by-product of adipic acid production was implemented in an existing production plant
- All required data (see following paragraph) are available and used
- The production of adipic acid within the current year is below the installed capacity that exists by the end of the year 2004 as defined in the PDD.

For the sake of clarity, the amount of Emission Reductions can exceed the amount calculated in a year period in the PDD in "SECTION E. Estimation of GHG emissions by sources" as all data in the PDD were conservative, in particular the performance of the N₂O abatement unit (in fact, the actual efficiency has been > 85%, and the destruction rate > 99%).

7. Monitored Parameters

According to the methodology AM 0021/version 1 and the Monitoring Plan, the data being collected to monitor the GHG reduction are given in the table below:

ID	Data variable	Source of data	Data unit	Recording frequency	Reference
Q_GE	Volume of effluent gas leaving the stack	Flow meter	Nm ³	Monthly	Appendix 1
N ₂ O_GE	Concentration of N ₂ O in the effluent gas	Laser diode online analyzer	ppm	Monthly	Appendix 2
ND_N2O	Quantity of N ₂ O in the effluent gas leaving the stack	Calculated from Q_GE and N ₂ O_GE	kg	Monthly	Appendix 3
Q_NG	Amount of natural gas burned	Natural gas meter	Nm ³	Monthly	Appendix 4
NGC	Natural gas composition required for calculation of E_NG	Gas supplier	-	Monthly	Appendix 5
%_on-line	% of production time the position switch on the by-pass valve is closed	Position switches on bypass valve	% of production time	Monthly	Appendix 6
Q_N2O_by-pass	N ₂ O by passing the decomposition facility	Calculated from Q_N2O and %_on-line	kg	Monthly	Appendix 7

ID	Data variable	Source of data	Data unit	Recording frequency	Reference
P_AdOH	Amount of adipic acid production	Excel workbook for calculation of nylon salt production, AA slurry production and dry AA production	ton	Monthly	Appendix 8
Nitric acid consumption (HNO ₃ _consumption) & physical losses in the adipic acid production process (HNO ₃ _physical)	All data required for calculation of HNO ₃ chemical and the N ₂ O emission factor N ₂ O_AdOH	Excel workbook based on the raw material consumption, DCS data and Lab data	ton	Monthly	Appendix 9
Q N ₂ O reg	Per Brazilian regulation allowed N ₂ O emissions	Brazilian regulation	kg/a	Date when relevant legislation is in place	Appendix 10
N ₂ O reg/AdOH	Per Brazilian regulation allowed N ₂ O emissions per kg of adipic acid produced	Brazilian regulation	kg/kg	Date when relevant legislation is in place	Appendix 10
r _y	Per Brazilian regulation required share of N ₂ O emissions to be destroyed	Brazilian regulation	%	Date when relevant legislation is in place	Appendix 10
P N ₂ O	Market price of N ₂ O	Estimated	€/t	Yearly	Appendix 11
Q_Steam_p	Amount of steam produced by the decomposition process	Steam meter	kg	Monthly	Appendix 12

ID	Data variable	Source of data	Data unit	Recording frequency	Reference
Steam supplier data	All data required for calculation of E_Steam	Rhodia Industrial Platform of Paulínia	-	Yearly	Appendix 13
Q_Power	Electric consumption of the decomposition facility	Electricity meter	kWh	Monthly	Appendix 14
Electricity grid data	All data required for calculation of E_Power according to ACM0002 version 2 and the Monitoring Plan	Brazilian ONS (Operador Nacional do Sistema Elétrico)	-	Yearly	Appendix 15
Q_Steam_c	Amount of steam consumed by the decomposition facility	Steam meter	kg	Monthly	Appendix 16
Steam suppliers data	All data required for calculation of E_Steam_c	Rhodia Industrial Platform of Paulínia	-	Yearly	Appendix 17

8. Quality Control (QC) and Quality Assurance (QA)

8.1. Quality Management System

The Rhodia site is ISO 9001:2000 certified covering also the adipic acid plant and the N₂O decomposition unit. The Quality Management System helps Rhodia to continually improve its product, processes and services, which includes quality planning, management responsibility, documentation and data control, resources management, product realization, process analysis and improvement Rhodia site is also ISO 14000 certified.

The thermal oxidation plant is operated by Rhodia operating personnel. Rhodia has assigned the responsibility for operating, monitoring and reporting to the Adipic Acid Plant Manager.

The operation, data transfer and reporting procedures are incorporated into the ISO 9001 procedures of the Paulínia Adipic Acid plant

The personnel have been trained by Rhodia engineers who have been trained by the technology supplier i.e. John Zink Company LLC.



8.2. Quality control (QC) and quality assurance (QA) procedures that are being undertaken for data monitored

The Paulinia adipic acid plant is certified according to ISO9001 and applies appropriate QA & QC procedures.

The equipment and analytical methods given by the technology supplier John Zink Company LLC, USA as well as those supplied by Rhodia are done according to internationally accepted standards.

The QA & QC procedures are set and implemented in order to:

1. Secure a good consistency through planning to implementation of this CDM project and,
2. Stipulate who has responsibility for what and,
3. Avoid any misunderstanding between people and organization involved.

Data (Indicate table and ID number e.g. 3.-1.; 3.2.)	Uncertainty level of data (High/Medium/ Low)	Explain QA/QC procedures planned for these data, or why such procedures are not necessary.
2a.1. (D.2.1.1) Q_GE	Low	<i>This flow rate is measured with an Averaging Pitot tube. This instrument is a critical instrument in the QA/QC procedure.</i>
2a.2. (D.2.1.1) N ₂ O_GE	Low	<i>Measured using Laser Diode technology Specific procedures are applied to this analyzer for QA & QC following the manufacturer's recommendation.</i>
2a.4. (D.2.1.1) Q_NG	Low	<i>Is measured using natural gas meter from the supplier and as such is part of a regular procedure control between the Natural Gas supplier and Rhodia.</i>
2b.1. (D.2.1.3) P_AdOH	Low	<i>Is obtained from production records of the Paulinia Adipic Acid plant where the N₂O waste originates. A QA/QC procedure is implemented. Production quantity is based on the packaged product plus slurry production used for the Nylon Salt production. Both dry adipic acid and nylon salt are weighed.</i>
2a.5. (D.2.1.1) %_on-line	Low	<i>Use high integrity performance by-pass valve to limit leaks. Procedures currently in place in Chalampé for monitoring N₂O emissions have been implemented in Paulinia to periodically check their tightness and assure their good operation. They have been added to the QA/QC existing procedures.</i>
2b.7. (D.2.1.3) Q_Steam_p	Low	<i>Steam meter placed on the list of critical instrument data in the QA/QC procedures</i>
3.1. (D.2.3.1) Q_Power	Low	<i>Electricity meter. Standard procedures are used. No QA/QC procedures implemented as this flow represents less than 0.01% of the baseline emissions.</i>
3.4. (D.2.3.1) Q_Steam_c	Low	<i>Steam meter placed on the list of critical instrument data in the QA/QC procedures.</i>

Main QC and QA procedures specific to the project activity:

Data Handling Protocol ISAL-ADOH-QA-007

Data Review Protocol ISAL-ADOH-QA-008



8.3. Calibration/Maintenance of Measuring and Analytical Instruments

All measuring and analytical instruments are being calibrated as per the methodology AM0021/version 1 and the PDD using either existing or specifically created protocols in Paulínia's Quality Management System procedures.

The maintenance methods and procedures have been incorporated as part of the ISO 9001 procedures and form an integral part of the systems and procedures for the organization.

The Monitoring Equipment Calibration and Maintenance status is presented on Appendix 18.

8.4. Environmental Impact

After commissioning the thermal oxidation plant, online analysis of the NO_x content in the gaseous effluents is carried out to verify such discharge from the plant. Monitoring of the NO_x content in the waste gas is required by local environmental legislation stated in the Commitment Agreement (TAC) signed with the Public Attorney of the State of São Paulo. NO_x in the gaseous effluent can be randomly checked by the environmental agency Cetesb through sampling and analysis by an external laboratory. Analytical data show that the plant complies with the established environmental standard.

Table showing analysis of Gaseous Emission for Thermal Oxidation plant

Parameter	Unit	Limit as per applicable standard	Analytical results in this period
NO _x	vppm	300 max at least 95% of time	Average of 44 and less than 300 for 99,9% of time

9. GHG Calculations

A spreadsheet Excel file "WORKBOOK ER PAULINIA" containing all the values of the monitoring parameters and the emission reduction calculation according to the methodology (AM0021/version 1) and the PDD is submitted to the DOE and to the UNFCCC for the request of issuance.

Statement of GHG emission reduction in this monitoring period.

As suggested by the methodology (AM0021/version 1), the GHG emission reduction, (ER_y), achieved by the project activity for the period is
$$ER_y = BE_y - PE_y - L_y$$

9.1. Calculation of Q_N2Oy

It has been checked that there are no Brazilian regulation into place that would limit the quantity of N₂O emitted that can be taken into account for the calculation of the baseline emissions (see D.2.1.4. in the PDD).

The quantity Q_N2Oy of N₂O emitted over the period can then be calculated by (AM0021/version 1 equation (2)):

$$Q_N2Oy = P_AdOH \times N2O_ / AdOH$$

Over the period of reference the emission factor from the adipic acid plant was above the capped value of 0.27 kg N₂O/kg AdOH (see Appendix 9). So the capped value is being used according to AM 0021/version 1.

Parameter	Value	Reference
Q_N2Oy	2 386 078 kg	Calculated
P_AdOH	8 837.327 t	Appendix 8
N2O_/AdOH	0.27 kg N ₂ O/kg AdOH	Appendix 9
Q_N2O reg	No limit	Appendix 10
N ₂ O_reg / AdOH	No limit	Appendix 10
r _y	NA	Appendix 10

The Executive Board has confirmed on EB36 the application of a yearly Adipic acid production cap as required by the methodology. The 3rd project year period started on November 19, 2008 and ended on November 18, 2009. The accumulated production of adipic acid in this project year period starting on November 19, 2008 and ending on November 18, 2009 (the last day of this monitoring period) is 83 498 tons, lower than 87 308 tons which is the yearly capped value as stated in the decision made by the EB47th meeting on May 28th 2009. This cap value is consistent with the clarification published in the EB 48th meeting report § 24 of July 17th 2009. Therefore the total production of this period can be used as such (see details in Appendix 8). This approach is consistent with the definitions and requirements of the "Guidance on accounting eligible HFC-23" AM0001 (EB39 Annex 8): the year of the crediting period is defined on the basis of the starting date of the crediting period of a project activity (in the present case November 19th).

9.2. Calculation of baseline emissions

The amount of baseline emissions in the given period y (measured in t CO₂ eq.) is calculated by (AM0021/version 1 equation (1)):

$$BEy = Q_N2Oy \times GWP_N2O + Q_Steam_py \times E_Steamy$$

and rounded down in t CO₂ eq. to get conservative consistency of final calculation of emission reductions formula.

Parameter	Value	Reference
BE_y	741 146 t CO₂ eq.	Calculated
Q_N ₂ O _y	2 386 078 kg	Calculated in 9.1
GWP_N ₂ O	310 kg CO ₂ eq./ kg N ₂ O	Kyoto Protocol Rule. Decision 2/CP.3 and IPCC
Q_Steam _{p_y}	10 083 500 kg of steam	Appendix 12
E_Steam _y	0.145 kg-CO ₂ /kg of steam	Appendix 13

9.3. Calculation of (Q_N₂O x (1-%_on-line))_y

The quantity of N₂O that has by-passed the decomposition facility is calculated from the adipic acid production made while by-passing the decomposition facility.

The quantity of adipic acid produced while by-passing the destruction facility is monitored and the quantity of N₂O that by-pass the decomposition facility is registered daily:

$$Q_{N_2O_by-pass} = P_{AdOH} \times (1 - \%_{on-line}) \times N_{2O_AdOH}$$

This value is a value by excess as during each connection/ disconnection phases the production is counted as completely by-passed.

The quantity of N₂O that by-passed the decomposition facility over the period is:

$$(Q_{N_2O} \times (1 - \%_{on-line}))_y = Q_{N_2O_by-pass}_y$$

The %_on-line_y equivalent over the period is calculated as:

$$\%_{on-line}_y = 1 - (Q_{N_2O_by-pass}_y / Q_{N_2O}_y)$$

Parameter	Value	Reference
Q_N ₂ O_by-pass _y	2 210 kg	Appendix 7
P_AdOH	8 837.327 t	Appendix 8
N ₂ O_AdOH	0.27 kg N ₂ O/kg AdOH	Appendix 9
%_on-line _y	99.907 %	Appendix 6

9.4. Calculation of project emissions

The emissions due to the decomposition process PE_y are the emissions due to the N₂O that has not been sent to the decomposition process, the N₂O non destroyed by the decomposition process and the emissions due to the use of natural gas.

$$PE_y = ((Q_{N_2O} \times (1 - \%_{on-line}))_y + (Q_{GE} \times N_{2O_GE} \times Specific_gravity_of_N_{2O})_y) \times GWP_{N_2O} + Q_{NG}_y \times E_{NG}_y \quad (AM0021/version 1 equation (6))$$

$$PE_y = (Q_{N_2O_by-pass}_y + (Q_{GE} \times N_{2O_GE} \times Specific_gravity_of_N_{2O})_y) \times GWP_{N_2O} + Q_{NG}_y \times E_{NG}_y$$

The non-destroyed N₂O (ND_N₂O_y) is constantly monitored and obtained from the constant monitoring of the flow (Q_GE) and the concentration of N₂O (N₂O_GE) of the effluent gas:

$$ND_N_2O = Q_GE \times N_2O_GE \times \text{Specific_gravity_of_}N_2O$$

$$PE_y = (Q_N_2O_by-pass_y + ND_N_2O_y) \times GWP_N_2O + Q_NG_y \times E_NG_y \quad (\text{AM0021/version 1 equation (5)})$$

PE_y is rounded up in t CO₂ eq. to get conservative consistency in final calculation of emission reductions formula.

Parameter	Value	Reference
PE_y	2 463 t CO₂ eq.	Calculated
Q_N ₂ O_by-pass _y	2 210 kg	Appendix 7
Q_GE	11 823 392 Nm ³	Appendix 1
N ₂ O_GE	14.3 vppm	Appendix 2
Specific gravity of N ₂ O	1.963 x 10 ⁻⁶	Appendix 2 and 3
ND_N ₂ O _y	332 kg N ₂ O	Appendix 3
GWP_N ₂ O	310 kg CO ₂ eq./ kg N ₂ O	Kyoto Protocol Rule. Decision 2/CP.3 and IPCC
Q_NG _y	756 820 Nm ³	Appendix 4
E_NG _y	2.204 kg CO ₂ eq./ Nm ³	Appendix 5

Note:

- 1) The value of E_NG_y shown above is the yearly moving average of E_NG as required by the PDD for calculation of E_Steam. The project emissions are more accurately calculated using the monthly values of E_NG shown in Appendix 5, following methodology AM0021/version 1 and the Monitoring Plan.
- 2) The value of ND_N₂O_y is calculated by the DCS using every 10 second data of Q_GE and N₂O_GE (see Appendix 2 and 3) and is more accurate than the value calculated using total average values.

9.5. Calculation of leakage

Leak emissions comprise the emissions associated with the energy sources used to generate any steam and electricity used by the decomposition plant.

Leakage amounts to (AM0021/version 1 equation (7)):

$$L_y = Q_Power \times E_Power + Q_steam_c_y \times E_steam_c_y$$

L_y is rounded up in tCO₂ eq. to get conservative consistency in final calculation of emission reductions formula.

Parameter	Value	Reference
Ly	55 t CO₂ eq.	Calculated
Q Power	44 067 kWh	Appendix 14
E Power	1.095 kg CO ₂ /kWh	Appendix 15
Q Steam c _y	30 400 kg	Appendix 16
E Steam c _y	0.215 kg CO ₂ / kg of steam	Appendix 17

9.6. Calculation of emission reduction

Following the PDD section D.2.4, the total emission reduction achieved by this project activity during this monitoring period is therefore,

$$ER_y = BE_y - PE_y - L_y$$

Or,

$$ER_y = 741\,146 \text{ t CO}_2 \text{ eq.} - 2\,463 \text{ t CO}_2 \text{ eq.} - 55 \text{ t CO}_2 \text{ eq.}$$

Or,

$$ER_y = 738\,628 \text{ t CO}_2 \text{ eq.}$$

The above emission reduction covers the generation of N₂O during this monitoring period.

9.7. Comparison of the emission reduction with the PDD estimates

In the PDD section E, the annual emission reduction is estimated to be 5 961 165 tCO₂eq. So the PDD-estimated emission reduction relative to the monitoring period of 36 days is around 587 949 tCO₂eq. The 150 679 tCO₂eq variance of the actual emission reduction is explained by:

PE: PDD value = 115 101 tCO ₂ eq Period = 2 463 t CO ₂ eq	
Variance	Explanation
104 586	The significant higher performance of the N ₂ O abatement unit (the actual %_on-line of 99.907% in this period is significantly higher than the value of 85% estimated in the PDD due to excellent operational performance). The estimate of 85% in the PDD assumed a low performance rate of the destruction equipment due to the lack of experience with such equipment.
7 480	A higher destruction rate of the N ₂ O which is in excess of 99.98 % during this period versus 99 % taken conservatively in the PDD.
572	Difference in the natural gas consumption estimate and actual in the period
112 638	Total PE variance

BE: PDD value = 703 171 tCO ₂ eq		Period = 741 146 t CO ₂ eq
Variance	Explanation	
37 980	The adipic acid production used for the ex-ante emission reduction was conservatively taken as 85 000 t/y (232.8 t/d) which is only 89.6 % of the nameplate capacity (260 t/d). To meet the market demand the plant produced 245.5 t/d on average during this period.	
- 5	Slight impact of the steam production	
37 975	Total BE variance	

L: PDD value = 121 tCO ₂ eq		Period = 55 t CO ₂ eq
Variance	Explanation	
66	Difference mainly due to the quantity of steam consumed	
66	Total L variance	

It is important to note that according to the methodology AM0021/version 1, the eligible adipic acid production that can be used in the baseline is yearly capped, so it limits on a yearly basis the emission reduction calculation claimed for CERs. Please see Appendix 8 for further detail

Moreover, given the general experiences with constant overestimation of CER volumes in the first years of CDM project development, Rhodia wanted to set the CER estimates in the PDD in a conservative fashion, especially regarding performance of the abatement equipment.



Appendix 1

Name of item	Q_GE
Description	Volume of effluent gas leaving the stack
Value in period	11 823 392 Nm ³
Method of monitoring	Annubar flow meter
Recording frequency	measured continuously, aggregated daily and monthly
Background data	Log sheet record / flowmeter

Period	Quantity of gaseous effluent Nm ³
October 14 th – October 31 st , 2009	5 776 772
November 1 st – November 18 th , 2009	6 046 620



Appendix 2

Name of item	N2O_GE
Description	Concentration of N ₂ O in the effluent gas
Value in period	14.3 vppm
Method of monitoring	Laser diode online analyzer
Recording frequency	Monthly
Background data	Log sheet record
Calculation method	<p>According to AM0021/version1, the instant values of the on-line analyzer is used to calculate the quantity of ND_N2O every 10 sec:</p> $ND_N2O = Q_GE \times N2O_GE \times Specific_gravity_of_N2O$ <p>N2O_GE need to be converted in kg/Nm³ according to AM0021/version1 note 2 table 2a, using the</p> $specific_gravity_of_N2O = 44/22.414 \times 10^{-6}$ <p>The analyzer has a range of 0-500 ppm with a detection limit of 5 ppm (1% of range). We use 5 ppm as a default value when the measured value is below the detection limit.</p> <p>Cumulated value for ND_N2O is recorded (see appendix 3).</p> <p>At the end of the month/period based upon the flow Q_GE, and ND_N2O the concentration of N2O equivalent for the month/period is calculated.</p> $N2O_GE = ND_N2O / (Q_GE \times N2O_GE \times Specific_gravity_of_N2O)$ <p>This value is for information as the constant calculation of ND_N2O is more accurate.</p>

Period	ND_N2O Kg	Quantity of gaseous effluent Nm ³	Average concentration of N ₂ O_GE vppm
October 14 th – October 31 st , 2009	272	5 776 772	24.0
November 1 st – November 18 th , 2009	60	6 046 620	5.0



Appendix 3

Name of item	ND_N2O
Description	Quantity of non-destroyed N2O emitted by the decomposition facility
Value in period	332 kg N ₂ O
Method of monitoring	On-line DCS calculation
Recording frequency	Monthly
Background data	Log sheet record
Calculation method	According to AM0021/version1, the actual quantity of non destroyed N2O is calculated on-line in the DCS from the concentration of N2O and the flow rate of the gaseous effluent, both measured on a wet basis (Method D of EB47 – “Tool to determine the mass flow of a greenhouse gas in a gaseous stream”) : $ND_N2O = Q_GE * N2O_GE * Specific_gravity_of_N2O$ N2O_GE need to be converted in kg/Nm ³ according to AM0021/version1 note 2 table 2a, using the $specific_gravity_of_N2O = 44/22.414 \times 10^{-6}$

Period	ND_N2O kg
October 14 th – October 31 st , 2009	272
November 1 st – November 18 th , 2009	60



Appendix 4

Name of item	Q_NG
Description	Amount of natural gas used by the decomposition process
Value in period	756 820 Nm ³
Method of monitoring	Natural gas consumption data
Recording frequency	Monthly
Background data	Log sheet record / flowmeter

Period	Q_NG Nm ³	CO2_NG t CO2 e
October 14 th – October 31 st , 2009	375 258	827.1
November 1 st – November 18 th , 2009	381 562	847.8

Appendix 5

Name of item	E_NGy with NGC
Description	Emissions coefficient for natural gas combustion Natural Gas Composition (NGC) is informed by the natural gas supplier
Value in period for E_NG _y	2.204 kg CO ₂ /Nm ³
Method of monitoring	Natural Gas Composition (NGC)
Recording frequency	Monthly
Background data	Composition data received from COMGAS (supplier)
Calculation method	Following the PDD Monitoring Plan The average number of C in a mole of NG is calculated from the composition = $\sum (\text{number of C in each mole}) \times (\text{volume ratio})$ The CO ₂ specific gravity in standard state is 1.965 $E_{NG} = 1.965 \times (\text{average number of C in a mole of NG})$ The yearly value (E_NG _y) is calculated as the average weighted by the natural gas consumption of the twelve months available prior to the beginning of the period. E_Steam is calculated yearly as per the Methodology and needs a yearly value of E_NG (see Appendix 13). All monthly values of E_NG for the year are within +/- 0.5% of the yearly value of E_NG _y . For this monitoring period, natural gas composition from November are not yet available, so to be conservative, the NGC of the month of August 2008 was used for November because it gives the highest E_NG value since the beginning of the crediting period (November 19 th , 2006). These E_NG values are used in the calculation of the project emissions (part due to the natural gas combustion of the N ₂ O unit)

Component	October NGC (%)	November NGC (%)	Number of C
CH ₄ (Methane)	88.91	88.30	1
C ₂ H ₆ (Ethane)	6.14	6.35	2
C ₃ H ₈ (Propane)	1.82	1.99	3
I-C ₄ H ₁₀ (I-Butane)	0.27	0.29	4
N-C ₄ H ₁₀ (N-Butane)	0.38	0.42	4
I-C ₅ H ₁₂ (I-Pentane)	0.11	0.12	5
N-C ₅ H ₁₂ (N-Pentane)	0.08	0.08	5
C ₆ H ₁₄ + (Hexane)	0.07	0.10	6
N ₂ (Nitrogen)	0.64	0.76	0
CO ₂ (Carbon dioxide)	1.59	1.58	1
Average number of C	1.121	1.131	
E_NG (month)	2.204	2.222	



Appendix 6

Name of item	%_on-line
Description	% of production time that the N2O is sent to the decomposition facility
Value in period	99.907 %
Method of monitoring	Position of limit switch on the valve allowing to by-pass the decomposition facility
Recording frequency	Monthly
Background data	Log sheet record
Calculation method	%_on-line is determined following the PDD. Based upon the position of the limit switch on the valve by-passing the decomposition facility, the % of time that the production is connected to the facility is continuously counted and used to calculate the daily value of Q_ N2O_by-pass (See Appendix 7). The daily values of Q_ N2O_by-pass are added to determine the monthly values of Q_ N2O_by-pass, as required by the PDD.

At the end of the period, %_on-line for the period y is calculated as:

$$\%_{\text{on-line}_y} = 1 - (Q_{\text{N2O_by-pass}_y} / (P_{\text{AdOH}_y} \times \text{N2O_AdOH}))$$

Period	Q_ N2O_by-pass _y Kg	P_ AdOH _y t	%_on-line _y %
October 14 th – October 31 st , 2009	0	4 384.508	100.000
November 1 st – November 18 th , 2009	2 210	4 452.819	99.816



Appendix 7

Name of item	Q_N2O_by-pass
Description	N2O by-passing the decomposition facility
Value in period	2 210 kg
Method of monitoring	Production record and %_on-line DCS monitoring
Recording frequency	Monthly
Background data	Production & %_on-line log sheet record
Calculation method	<p>The quantity of N2O that by-pass the facility is then recorded daily and calculated following AM0021/version1.</p> $Q_N2O_by-pass_d = Q_N2O_d \times (1 - \%_on-line)$ <p>or</p> $Q_N2O_by-pass_d = P_AdOH_d \times N2O_/AdOH \times (1 - \%_on-line)$ <p>At the end of the period the quantity of N2O that by-passed the facility is:</p> $Q_N2O_by-pass_y = \Sigma (Q_N2O_by-pass_d)$

Period	Q_N2O_by-pass _y Kg
October 14 th – October 31 st , 2009	0
November 1 st – November 18 th , 2009	2 210

Appendix 8

Name of item	P_AdOH
Description	Adipic acid production
Value in period	8 837.327 t
Method of monitoring	Packed production and slurry used to nylon salt production
Recording frequency	Monthly
Background data	Log sheet record
<p>The production of adipic acid over the year ending with the last day of this period (from November 19th, 2008 to November, 18th 2009) is 83 498 t lower than the yearly capped value of 87 308 t as stated by the EB 47th meeting decision on May 28th (detailed information is available in the Excel file "Workbook ER Paulinia", sheet BE, line 22, submitted to UNFCCC). The value of 87 308 t was calculated in the Validation Report as the maximum daily production in 2004 x 365 days x the operational rate (260 t/day x 365 x 92%) which is consistent with the clarification of the EB48th meeting report §24 of 17th July 2009. Therefore, the total production of this period can be used as such. The Executive Board has confirmed on EB36 the application of a yearly Adipic acid production cap as required by the methodology. This approach is consistent with the definitions and requirements of the "Guidance on accounting eligible HFC-23" AM0001 (EB39 Annex 8): the year of the crediting period is defined on the basis of the starting date of the crediting period of a project activity (November 19th); the current period ends on November 18th, which is the end date of the year of the crediting period.</p>	

Month - year	Adipic acid production t
October 14 th – October 31 st , 2009	4 384.508
November 1 st – November 18 th , 2009	4 452.819

As described in the PDD (Section A.2, Section B.2 Table 3 and annex4 Monitoring plan), the adipic acid production is measured by adding the dry adipic acid production, the slurry adipic acid production contained in the Nylon salt, and the in-process product inventory variations. In this case:



- Dry adipic acid: is the product which was packaged (determined by weigh scales).
- Slurry adipic Acid: is the product used to be mixed in fixed proportions with Hexamethyldiamine and make Nylon salt on Paulinia site. Nylon salt quality is very accurately analyzed and controlled. Daily Nylon salt production is obtained by the sum of the weight of the truckloads plus the variation of Nylon salt storage tank levels. Both the concentration of Nylon salt as well as adipic acid content are controlled in the Nylon salt production process: the Nylon salt concentration is monitored online by refractive index measurement and the adipic acid slurry content is monitored through precise pH measurement. Furthermore, following the Quality Control procedure to guarantee the Nylon salt specification, the content of the storage tank F5300 is analyzed every 2 hours for pH and concentration using very accurate instruments in the laboratory, according to the Quality Document “ISAL-HMD-SAL-QA-006” as stated in the PDD, section D3 line 2b.1. Should a parameter show a deviation, the Nylon salt unit operator would immediately correct the concentrations in the process to correct Nylon salt concentration and/or adipic acid content. The Nylon salt specification is very narrow (± 0.02 for pH and $\pm 0.2\%$ for concentration) and the analysis of the storage tank present a very low variability within those limits. This accuracy was checked by the auditor during the Initial Verification. Rhodia follows the PDD annex 3 and the monitoring plan and utilizes the Excel file “SAP-HMD.xls” to determine the nylon salt produced and automatically the corresponding adipic acid slurry. The calculation of the quantity of adipic acid in nylon salt on dry basis is based on a constant ratio of adipic acid in Nylon salt which is constant as fixed by the very precise value of the pH of the Nylon salt. The analytical results of pH and concentration of the Nylon salt solution for each period of one month are kept in an Excel file named “Qualidade SALN_month.xls” which is shown to the DOE for verification along with the file “SAP-HMD.xls”. The ratio of Adipic Acid in Nylon Salt is 0.55748 in the Excel file “SAP-HMD.xls” in compliance with the guidance issued by the Executive Board in its 45th meeting of February 2009.

The details of the calculation of the production amount are as follows.

The total daily adipic acid made by the nitric oxidation reaction is the sum of two terms (Equation (1)):

Total Production [P_AdOH] = [Finished Product] + [Variation of the In-Process Product]	(1)
--	-----

The finished adipic acid production is obtained by adding the production of dry and slurry adipic acid, according to Equation (2).

[Finished Product] = [Dry Adipic Acid] + [Slurry Adipic Acid]	(2)
---	-----

The in-process adipic acid is obtained by adding the amount of adipic acid contained in all process equipment where adipic acid is present at different concentrations.

The variation of the In-Process Product inventory of day N is obtained by subtracting the total In-Process Product of day N minus In-Process Product of day (N-1) as in Equation (3):

$[\text{Variation of the In-Process Product}] = [\text{In-process Product of day N}] - [\text{In-process Product of day (N-1)}]$	(3)
--	-----

Therefore, according to described in the sections above, the total production of adipic acid is the sum of the following terms described in Equation (4), after rewriting Equation (1) using Equation (2):

$\text{Total Production [P_AdOH]} = [\text{Dry Adipic Acid}] + [\text{Slurry Adipic Acid}] + [\text{Variation of the In-Process Product}]$	(4)
---	-----

The total production is normally different from the finished product on a daily basis since the in-process product is always varying. The total production can be higher or lower than the finished product. On a long term basis however those differences compensate each other and the accumulated total production will of course approach the sum of dry + slurry.

For the purpose of determining the daily amount of N₂O generated by the nitric oxidation of the raw materials, it must be used the total production, not the finished adipic acid production, since N₂O is generated by the reaction and is independent of the finished production for a limited time (up to 1 or 2 days). In fact during such limited time the adipic acid made at the reaction can be accumulated in the process equipments awaiting to be processed through purification and drying.

Appendix 9

Name of item HNO₃_consumption & HNO₃_physical
 Description Nitric acid consumption and losses in the adipic acid process (see table below)
 Value in period
 Method of monitoring Excel workbook based on monitoring data and analysis
 Recording frequency Monthly

Background data Log sheet records
 Calculation method Nitric acid physical losses (HNO₃_physical) in the aqueous wastes, the off gases, the adipic acid and the by-product are monitored.
 Those losses are deducted from the nitric acid consumption, (HNO₃_consumption) to get the chemical consumption, (HNO₃_chemical) (AM0021/version 1 equation (3)).

Period	HNO ₃ _consumption T	HNO ₃ _physical t	HNO ₃ _chemical t
October 14 th – October 31 st , 2009	3 883.0	61.5	3 821.5
November 1 st – November 18 th , 2009	3 921.1	63.54	3 857.51
Rolling year November 18 th , 2009	74 344	3 720	70 624

Name of item N₂O_AdOH
 Description N₂O emission factor for adipic acid production
 Value in period 0.270 kg N₂O/kg AdOH
 Method of monitoring Adipic acid production, nitric acid consumption and physical losses
 Recording frequency Yearly

Calculation method The N₂O emission factor is then calculated over the period on one year using the last rolling year data (AM0021/version 1 equation (4)):

$$N_2O_AdOH = HNO_3_chemical / P_AdOH / 63 / 2 \times 0.96 \times 44$$

The calculated value for this period is above 0.270 and is then capped by the value of KE_N₂O = 0.27, as specified in the PDD table D.2.1.3 and required by the methodology AM0021/version 1 referring to the IPCC Good Practice Guidance.

Period	Value N ₂ O_AdOH calculated kg N ₂ O/kg AdOH	KE_N ₂ O kg N ₂ O/kg AdOH	N ₂ O_AdOH kg N ₂ O/kg AdOH
Rolling year November 18 th , 2009	0.283	0.270	0.270



Appendix 10

Name of item	Q_N ₂ O reg, N ₂ O_reg / AdOH and r _y
Description	<p>Evolution of Brazilian legislation that may require limitation of N₂O emissions using one of the following criteria:</p> <ul style="list-style-type: none"> - Q_N₂O reg : allowed N₂O emissions - N₂O_reg / AdOH: allowed N₂O emissions per kg of adipic acid produced - r_y: share of N₂O emissions required to be destroyed
Value in period	not applicable
Method of monitoring	Survey
Recording frequency	When relevant
Background data	<p>Brazilian legislation</p> <p>No evolution of legislation since PDD emission.</p>

Period	Q_N ₂ O reg Kg	N ₂ O_reg / AdOH kg	r _y %
October 14 th – November 18 th , 2009	No limit	No limit	0

Note: Rhodia follows the evolution of Brazilian legislation about N₂O emissions that could affect the project Emission Reduction through the parameters N₂O_reg / AdOH, Q_N₂O reg, or r_y as part of the ISO 14000 requirements.

Rhodia has hired an external company specialized in regulations. It sends to GSIMAP (Rhodia Industrial Platform) all the changes in regulations that may impact Rhodia. GSIMAP team evaluates the changes and discusses the applicability to the Rhodia operations in a steering committee. The conclusions from this steering committee are then presented to the Quality representatives of all plant units in a formal meeting that happens every three months.

Furthermore GSIMAP experts on environmental issues participate on meetings held on external organizations (such as ABIQUIM - Brazilian Association of Chemical Industries, CETESB - local environmental agency) that discuss draft regulations. Those experts know in advance what comes next in terms of environmental laws.



Appendix 11

Name of item

Description

Value in period

Method of monitoring

Recording frequency

Background data

P_ N₂O

Market price of N₂O in waste gas

0 €/t

Market survey

Yearly

Refer to study “N₂O market study NITROUS OXIDE Brazil” –update September 2009

The N₂O market is rather small and limited, requires highly pure N₂O, not waste gas. The largest market usage is for the medical use (anesthetic and analgesic) then for food and electronics.

Beside the very high investment cost in a purification-concentration-liquefaction unit to extract the N₂O from the exhaust flow of the adipic acid plant, neither the process as the product will get the necessary certifications for the pharmaceutical and food markets.

The market study concludes that there is no N₂O market for the N₂O produced as by-product of adipic acid.

Year	P N ₂ O
2009	0



Appendix 12

Name of item	Q_Steam_p
Description	Amount of steam produced by the decomposition facility
Value in period	10 083 500 kg
Method of monitoring	Flowmeter
Recording frequency	Monthly
Background data	Log sheet record

Period	Q_Steam_p Kg	CO2_Steam_p t CO2 e
October 14 th – October 31 st , 2009	5 035 000	730
November 1 st – November 18 th , 2009	5 048 500	732



Appendix 13

Name of item	E_Steam
Description	CO ₂ emission factor for steam produced by the facility
Value in period	0.145 kg CO ₂ /kg of steam
Method of monitoring	Supplier data
Recording frequency	Yearly
Background data	Data supplied by the Rhodia Paulínia Industrial Platform
Calculation method	<p>Calculation is made according to the monitoring plan, section 6.3.</p> <p>We first calculate the amount of natural gas required to generate steam in Nm³/t of steam in a very efficient boiler</p> $QNG_steam = \Delta H \text{ (kJ/t)} / (\text{LHV (kJ/Nm}^3\text{)} \times \eta \text{ (\%)})$ <p>The LHV data is the yearly average value for the gas supplied by COMGAS.</p> <p>The yield η (%) of the boiler is conservatively taken as 97%, while the yield is generally below 90%.</p> <p>E_NG_y is the yearly average value for the gas supplied by COMGAS (see appendix 5).</p> <p>The yearly value of E_Steam is calculated with the data available for the year prior to the beginning of the period in order to assure to have the data.</p> $E_Steam = QNG_steam \times E_NG_y$
Comment	LHV data is supplied by COMGAS in kcal/m ³ at 20 °C. Data were converted to kJ/Nm ³ .

Year ending	LHV kJ/Nm ³	ΔH kJ/t	η %	QNG_tsteam Nm ³ /t of steam	E_NG _y kg- CO ₂ /Nm ³	E_Steam kg-CO ₂ / kg of steam
October 13 th , 2009	38 650	2624000	97	65.85	2.204	0.145



Appendix 14

Name of item	Q_Power
Description	Electricity consumption by the decomposition facility
Value in period	44 067 kWh
Method of monitoring	Power consumption data
Recording frequency	Monthly
Background data	Log sheet record / counter

Period	Q_Power kWh	CO2_Power t CO2 e
October 14 th – October 31 st , 2009	20 967	23.0
November 1 st – November 18 th , 2009	23 100	25.3



Appendix 15

Name of item	E_Power
Description	CO ₂ intensity for electric generation
Value in period	1.095 kg CO ₂ /kWh
Method of monitoring	Survey of data publication
Recording frequency	Yearly
Background data	<p>Two sources of data are needed to up-date E_Power value:</p> <p>1. ONS (Operador Nacional do Sistema Elétrico) http://www.ons.com.br/biblioteca_virtual/publicacoes_operacao_sin.aspx</p> <p>2. Brazilian Ministry of Mines and Energy (MME) http://www.mme.gov.br/mme/menu/todas_publicacoes.html</p> <p>The data of ONS are available for 2008, but the latest data available from MME are for 2007. As a result, 2007 data are used for this period.</p>
Calculation method	<p>Calculated according to the PDD monitoring plan based on ACM0002 version 2. E_Power is calculated by taking into account only the emission factors of the fossil-fuel electricity generation (simple OM). As explained in the PDD Monitoring Plan, ONS still does not supply the plant-specific data required for BM (build margin) calculation. This is a very conservative approach since only 4% of the total electricity supplied to the grid is generated using fossil fuels (96% of Hydro and Nuclear).</p> <p>The detailed calculation is available in the Excel file “Workbook ER Paulínia” of this period (in the worksheet “E_Power”) which is a confidential document communicated to the DOE and to the CDM Executive Board. The data and the calculations were verified by the DOE prior to their utilization.</p>

Date (year)	E_Power kg CO ₂ /kWh
2009	1.095



Appendix 16

Name of item	Q_Steam_c
Description	Amount of steam consumed by the decomposition facility
Value in period	<div>30 400 kg</div>
Method of monitoring	Mass flowmeter
Recording frequency	Monthly
Background data	Log sheet record

Period	Q_Steam_c kg	CO2_Steam_c t CO2 e
October 14 th – October 31 st , 2009	15 000	3.2
November 1 st – November 18 th , 2009	15 400	3.3



Appendix 17

Name of item	E_Steam_c
Description	CO ₂ intensity for steam consumed in the facility
Value in period	0.215 kg CO ₂ /kg of steam
Method of monitoring	Calculated from steam supplier data
Recording frequency	Yearly
Background data	Data supplied by the Rhodia Paulínia Industrial Platform
Calculation method	<p>This steam is supplied by existing boilers on site. Steam production, natural gas, fuel oil and by-products consumptions are monitored. From the monthly consumption of all fuels, the monthly value of E_NG and of the carbon content of each liquid fuel, monthly emissions of CO₂ for steam production are calculated and cumulated over the year. E_Steam_c is obtained from the ratio of yearly CO₂ emission over the yearly steam production.</p> <p>According to the PDD we calculate E_steam_c as a weighted average of the coefficients E_steam_c_NG (emission factor of steam produced by the boilers running on natural gas) and E_steam_c_chem&oil (emission factor of the steam produced by the boilers running on by-products and fuel oil) with the real share of the steam generated with each type of fuel.</p> $E_steam_c = E_steam_c_NG \times \%_gen_NG + E_steam_c_chem\&oil \times \%_gen_chem\&oil$ <p>where $\%_gen_chem\&oil = 100\% - \%gen_NG$</p> <p>The yearly value of E_Steam_c is calculated with the data available for the year prior to the beginning of the period in order to assure to have the data.</p>

Year ending	E_Steam_c_NG kg CO ₂ /kg of steam	E_Steam_c_chem&oil kg CO ₂ /kg of steam	%_gen_NG Share of steam generated using natural gas	E_Steam_c kg CO ₂ / kg of steam
October 13 th , 2009	0.210	0.267	93.6	0.215

Appendix 18 INSTRUMENT CALIBRATION & MAINTENANCE STATUS

INSTRUMENT CALIBRATION & MAINTENANCE STATUS

Related PDD parameter	Description	Tag Number	Parameter in PDD	Period	Done by	2008												2009												Remarks
						1	2	3	4	5	6	7	8	9	10	11	12	1	2	3	4	5	6	7	8	9	10	11	12	
						•	•	•	•	•	•	•	•	•	•	•	•	•	•	•	•	•	•	•	•	•	•	•	•	
P_AdOH	Packaging machine 25 kg	Z-3110	Dry AA (P_AdOH)	1/month	Third party	•	•	•	•	•	•	•	•	•	•	•	•	•	•	•	•	•	•	•	•	•				
P_AdOH	Packaging machine 25 kg	G-2532	Dry AA (P_AdOH)	1/month	Third party	•	•	•	•	•	•	•	•	•	•	•	•	•	•	•	•	•	•	•	•	•	•			
P_AdOH	Weigh scale 1000 kg	Z-3120	Dry AA (P_AdOH)	4/year	Third party	•			•	•		•				•		•			•			•		•				
P_AdOH	Trucks weigh scale	BB-0090	N-salt production (P_AdOH)	2/year	Third party						•				•					•										
P_AdOH	Trucks weigh scale	BB-0335	N-salt production (P_AdOH)	2/year	Third party						•				•					•										
P_AdOH	Level of tank R-5300	LT-4500	N-salt production (P_AdOH)	Yearly	Rhodia						•													•						
P_AdOH	Level of tank R-5310	LT-4509	N-salt production (P_AdOH)	Yearly	Rhodia			•																						
P_AdOH	Refractometer	Lab equipment RFM-340	N-salt production (P_AdOH)	Weekly 2/Year	Rhodia Third party	•	•	•	•	•	•	•	•	•	•	•	•	•	•	•	•	•	•	•	•	•	•		The maintenance done by third part was anticipated from April to end of March (26March09).	
P_AdOH	pH meter (PHLAC1 / PHLAC2 / PHLAC3)	Lab equipment 780	N-salt production (P_AdOH)	3x/Week 2/year	Rhodia Third party	•	•	•	•	•	•	•	•	•	•	•	•	•	•	•	•	•	•	•	•	•	•			
HNO3_cons	Nitric acid mass flowmeter	FQ-2179	Nitric Cons	2 years	Third party						•																		Next calibration August, 2010	
HNO3_cons	Fresh nitric acid conc analyzer	AI-2179	Nitric Cons	2 years	Third party						•																		Next calibration August, 2010	
HNO3_physical	Flowmeter of effluent to biological WWT	FQ-2973	Nitric Loss	Yearly	Rhodia						•													•						
HNO3_physical	Flowmeter of effluent to neutralization	FQ-2974	Nitric Loss	Yearly	Rhodia						•													•						
HNO3_physical	Waste gas flowmeter	FQ-3450	Nitric Loss	Yearly	Rhodia											•														
HNO3_physical	Nitric analyzer on effluent to neutralization	AI-2974	Nitric Loss	2/month	Rhodia	•	•	•	•	•	•	•	•	•	•	•	•	•	•	•	•	•	•	•	•	•	•			
HNO3_physical	Nitric analyzer on effluent to neutralization	AI-2974B	For failure of AI-2974	2/month	Rhodia															•	•	•	•	•	•	•	•		The back-up analyzer was installed in March, 2009.	
HNO3_physical	NOx analyzer in the waste gas stream	AI-2195AB	Nitric Loss	1/month	Rhodia	•	•	•	•	•	•	•	•	•	•	•	•	•	•	•	•	•	•	•	•	•	•		* Failure of AI-2195AB on February 4th, 2009, Equipment has been sent to supplier for repairing. It was reinstated on March 13th.	
HNO3_cons	Level of nitric acid storage tank F-1769	LI -3350	Nitric Cons (backup)	Yearly	Rhodia						•													•						
HNO3_cons	Flowmeter of fresh nitric acid to storage	FQ-3318	Nitric Cons (backup)	Yearly	Third party			•				•								•									Calibration was done during Nitric Acid Shutdown due to ending of campaign	
Q_NG	Natural gas flowmeter	FQ-3408	Project emission	2 years	Third party								•																Next calibration October, 2010	
Q_Steam_p	40 bar steam flowmeter	FQ-3470	Baseline emission	Yearly	Third party								•													•				
Q_Steam_c	6,5 bar steam flowmeter	FQ-3409	Leakage	Yearly	Third party	•										•														
Q_GE	Stack effluent gas flowmeter	FQ-3490	Project emission	Yearly	Third party										•												•			
N2O_GE	Stack N2O analyzer (in-situ, laser diode)	AI-3490B	Project emission	Yearly	Rhodia									•												•				
N2O_GE	Stack N2O analyzer (extractive, infrared)	AI-3490G	Project emission (backup)	Monthly	Rhodia	•	•	•	•	•	•	•	•	•	•	•	•	•	•	•	•	•	•	•	•	•	•		Calibration in November will be done during Period #31	
Q_GE, Q_steam_p	Stack O2 analyzer (in-situ, laser diode)	AI-3460	Project emission (backup), steam production (backup)	Yearly	Third party								•													•				
Q_N2O_bypass	By-pass valve leak test	HV-3402	Project emission	Yearly	Third party			•											•											
Q_Power	Electricity meter	JI-3461	Leakage	2 years	Third party							•																	Next calibration September, 2010	
HNO3_physical	Waste gas flowmeter	FIC-3401	For failure of FQ-3450	Yearly	Rhodia											•										•				
Q_NG	Natural gas flowmeter	FIC-3406	For failure of FQ-3408 and FQ-3460	2 years	Third party			•																					Next calibration March, 2010	
Q_NG	Natural gas flowmeter	FQ-3460	For failure of FQ-3408	2 years	Third party								•																Next calibration August, 2010	
Q_Steam_p	Boiler feed water flowmeter	FQ-3410	For failure of FQ-3470	Yearly	Rhodia								•													•				
P_AdOH	Level of tank RE-2422	LI-2422	Inventory variation	Yearly	Rhodia							•													•					

Source of data: Quality Management System and SAP