

Tambun LPG Associated Gas Recovery and Utilization Project

Clean Development Mechanism (CDM)

CER Monitoring Report

(Certified) Emission Reductions

Monitoring Period: 16 February 2009 – 30 September 2009

CDM Registration No: 1144

Date: 16 October 2009
Version 1

A project designed to meet the baseline and monitoring requirements of UN CDM Approved
Methodology

AM0009 Version 2
“Recovery and Utilization of Gas from Oil Wells that would otherwise be flared”

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Annex A Parameters Monitored/Retention

1. General Project Activity Information

1.1 Title of Project Activity

Project 1144 : Tambun LPG Associated Gas Recovery and Utilization Project - Indonesia.

1.2 CDM Registration date and crediting period

Registration Date: 01 Feb 2008.
Crediting Period: 01 Feb 2008 – 31 Jan 2018 (fixed)

1.3 Contact Details

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1.4 Short Description of the project activity

The purpose of the project activity is the recovery and utilization of gases produced as a by-product of oil production activities at the Tambun and Pondok Tengah Oil fields.

The Tambun Oil Field is located about 40 km west of Jakarta in West Java Province. This field started production in 2003 at 4,000 barrels per day. Associated gas was flared, initially at 6 to 7 mmscfd (millions of standard cubic feet per day); increasing to 12 to 15 mmscfd as oil production increased to 8,000 barrels per day in 2006. The Pondok Tengah Oil field (PDT), located about 10 km North of Tambun, has come on stream at a faster rate than planned. A geographical overview of the project location is provided overleaf.

The technology consists of a mini Liquefied Petroleum Gas (LPG) plant with a designed input capacity of 15 mmscfd, condensate removal facilities, a 35 km 8" diameter steel pipeline and associated auxiliary equipment including compressors, metering stations and safety valves.

The processing plant and pipeline is constructed in full compliance with the local environmental regulations and was subject to environmental appraisals as per Indonesian environmental regulations. The processing plant is powered by the gas supply, with back-up diesel for generators and fire pumps. The supply pipeline runs 35 km to the main east-west supply line. The pipeline is constructed from carbon steel, with a mid-wall diameter of 8 inches.

Emergency shutdown valves are located at the start and finish of the pipeline and two line break control valves (LBCV) installed at approximately 12km and 24km from the start.
In December 2006 the back-up generators have been converted to run on gas. No diesel has been used for on-site power generation since then.

Location of the project activity

The LPG plant is located at 107 01' 40" E, 06 07' 55" S. Tambun Oil Field comprises several wells, located within a few km of the LPG plant. Pondok Tengah Oil Field is located at adjacent to, and to the north of Tambun Oil Field.

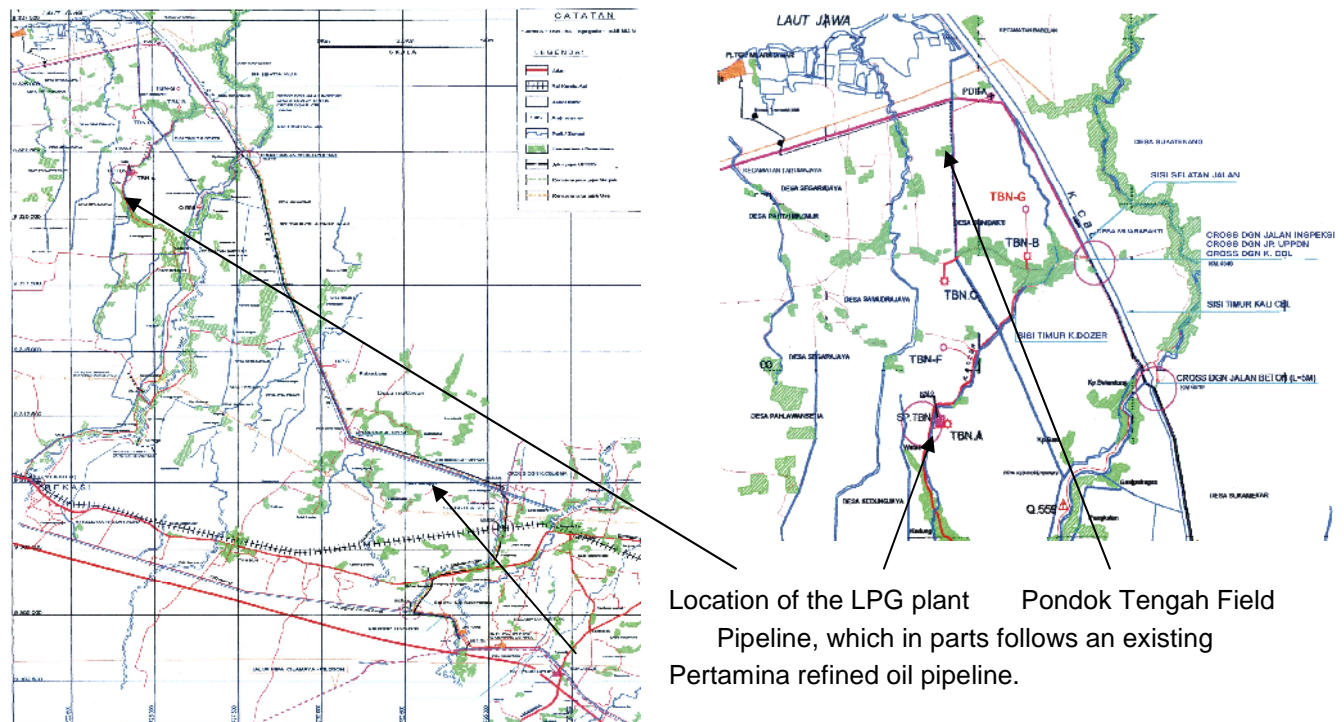


Figure 1 **Location of the project activity**

The project participants are:

PT. Odira Energy Persada, an Indonesian private gas company which was established under the laws of Indonesia and having its registered office at Jl. Patal Senayan No.38, Jakarta 12210, Indonesia (hereinafter referred to as "Odira").

Sindicatum Carbon Capital Ltd, a company incorporated under the laws of England and having its registered office at 33 Duke Street, London, W1U 1JY, United Kingdom (hereinafter referred to as "SCC").

1.5 Monitoring Period Covered

The monitoring period covered by this monitoring report: 16 February 2009 – 30 September 2009 (inclusive). This is the fifth monitoring report.

1.6 Methodology Applied to the Project Activity

AM0009 ver. 2 - Recovery and utilization of gas from oil wells that would otherwise be flared.

1.7 Deviations or Revisions to the Registered PDD or Monitoring Plan

N/A.

1.8 Special (Accidental) Events occurred during this reporting period

During the monitoring period, no accidental events occurred.

1.9 Changes Since Last CER Verification

No changes. This is the fifth monitoring report.

2. Monitoring Plan

2.1 Parameters Monitored

The parameters monitored and the monitoring procedure applied for determination of the emission reductions is described in detail in section B.6.1 of the Project Design Document v3.12 dated 13th December 2007, and available upon the UNFCCC website (<http://cdm.unfccc.int/Projects/DB/LRQA%20Ltd1180000727.07/view>).

As described in the registered PDD , associated gas feed the Tambun LPG plant originates from 2 separate oil fields, a permanent associated gas feed from the Tambun oil field and an additional temporary associated gas feed from the Pondok Tengah oil field.

At the time of project registration (1 February 2008) , the Pondok Tengah associated gas feed supply was expected to continue until year 3, however the contract terms for this supply allowed for early termination and for reasons out of project control, the contract and associated gas supply has now terminated (31 March 2008). Monitoring of the 6" supply from Pondok Tengah is therefore no longer required since the pipeline has been decommissioned and the measurement device has been removed. Despite these changes, a similar volume of gas is still being supplied so the estimates of total gas flow remain the same as in the original PDD, but all gas is routed through the Tambun pipelines.

An overview of the parameters monitored is provided in section 3 (and Annex A). The location of measurement devices installed is presented in figure 2 below:

[illegible]

On 31 March 2008 the contract for PDT previously flared gas ended and no further gas has been supplied through the 6" pipeline since then. Contract termination has been reviewed by SGS in previous verifications.
On 17 October 2008, the 4 inch line gas input to Odira has been shut off.
At the site one weighbridge is installed.

All data is compared from month to month using trend analysis to show where parameters have deviated significantly from preceding values. Any values identified as being unusual in this manner are re-checked and corrected if necessary, following the procedures in the monitoring plan.

Fugitive emissions of methane from the processing plant and pipelines and from accidental releases of methane from the transmission pipelines are calculated using the EPA approach¹ as per AM0009v2.

Any significant differences between daily / weekly / monthly or periodic values will be reviewed. An overview of the data collection process is provided in table 1 underneath. Detailed formulas for the calculation of emissions are presented in Section 3 below.

Table 1 Data collection process

| Parameter | Reference | Procedure / Frequency | Registration | Check and correct primary measurements |
|--------------------|---|--|---|--|
| Baseline Emissions | The baseline emissions are calculated using the formulae described in the PDD, section B6.1 - using the CDM spreadsheet | Primary data (weekly reports) are entered by the SCC officer in the CDM spreadsheet at the start of each month | CDM spreadsheet stored at SCC Project File S-Server | The SCC project officer performs a consistency check based upon previous months. In case of irregularities data is double checked with Odira and if needed corrected |
| Leakage | Leakage is calculated using the formulae described in the PDD, section B6.1 - using the CDM spreadsheet | Primary data (weekly reports) are entered by the SCC officer in the CDM spreadsheet at the start of each month | CDM spreadsheet stored at SCC Project File S-Server | The SCC project officer performs a consistency check based upon previous months. In case of irregularities data is double checked with Odira and if needed corrected |
| Project Emissions | The project emissions are calculated using the formulae described in the PDD, section B6.1 - using the CDM spreadsheet | Primary data (weekly reports) are entered by the SCC officer in the CDM spreadsheet at the start of each month | CDM spreadsheet stored at SCC Project File S-Server | The SCC project officer performs a consistency check based upon previous months. In case of irregularities data is double checked with Odira and if needed corrected |

¹ Document EPA-453/R-95-017 available at <http://www.epa.gov/ttnchie1/publications.html>.

| | | | | |
|----------------------|--|--|---|--|
| Emissions Reductions | The emission reductions are calculated using the formulae described in the PDD, section B6.1 - using the CDM spreadsheet | Primary data (weekly reports) are entered by the SCC officer in the CDM spreadsheet at start of each month | CDM spreadsheet stored at SCC Project File S-Server | The SCC project officer performs a consistency check based upon previous months. In case of irregularities data is double checked with Odira and if needed corrected |
|----------------------|--|--|---|--|

Accuracy and calibration of instruments

All measurement devices are maintained to ensure a high level of accuracy. All meters are subject to a quality control regime that include a regular maintenance and calibration according to manufacturer's instructions.

A record is available showing the location and unique identification number of each meter, the calibration status of that meter (when last calibrated, when next due for calibration).

Annual calibrations of continuous flow meters and weighbridge are performed (as locally required) by the Indonesian 'Direktorat Metrologi' (State organization). All calibration records are retained for until two years after the end of the crediting period and are available for verification by the DOE. Additional instrument verification, flow calculation and configuration checks are carried out periodically by SCC staff.

Archiving of data

Data is archived periodically to a secure and retrievable storage format for a period 2 years after crediting period (see also Annex A).

Document Control

A document control system has been introduced ensuring that the current versions of necessary documents are available at the point of use.

Treatment of missing or corrupted data

Where data in the on-line system are corrupted or missing whilst the plant is operating, the corrupt or missing data can be corrected using the installed back-up metering devices (e.g. Barton Chart, calibrated weighbridge, manual daily recordings). In case errors are identified, both corrective and preventive actions are taken.

Internal Audit

An audit of the data collection and QC/QA system is performed periodically, at least once per year. A copy of the internal audit report(s) is available for the verifying DOE.

Internal Training

Relevant process operators have received training to ensure compliance with the tasks and procedures set out in the monitoring plan.

3. Formulas Utilized to calculate Emission Reductions

The formulas used for calculation are in accordance with the approved methodology CDM-EB AM0009 version 2 “recovery and utilization of gas from oil wells that would otherwise be flared”.

3.1 Baseline Emissions

The formula used for determination of the baseline emissions are described in section B.7.1 of the Project Design Document v3.12 dated 13th December 2007, and available upon the UNFCCC website (<http://cdm.unfccc.int/Projects/DB/LRQA%20Ltd1180000727.07/view>).

Baseline emissions are calculated as follows:

$$BL_y = V_{A,y} \cdot W_{carbon,A,y} \cdot \frac{44}{12} \cdot \frac{1}{1000}$$

where:

BL_y Are the baseline emissions during the period y in tons of CO₂ equivalents.

$V_{A,y}$ Is the volume of gas recovered from the oil field during the period y in m³.

$W_{carbon,A,y}$ Is the average content of carbon in the gas recovered during the period y in kg-C/m³.

The average methane content in the gas $w_{CH_4,A,y}$ is determined from regular measurements of the composition of the gas, taking into account the molecular weight of all fractions of the gas.

3.2 Project Emissions

The formulas used for determination of the project emissions are described in section B.7.1 of the Project Design Document v3.12 dated 13th December 2007, and available upon the UNFCCC website (<http://cdm.unfccc.int/Projects/DB/LRQA%20Ltd1180000727.07/view>).

Project emissions are calculated as follows:

$$PE_{CO_2,gas,y} = \frac{m_{carbon,A,y}}{m_{carbon,A,y} + m_{carbon,X,y}} \cdot (m_{carbon,A,y} + m_{carbon,X,y} - m_{carbon,B,y}) \cdot \frac{44}{12} \cdot \frac{1}{1000}$$

with

$$m_{carbon,A,y} = V_{A,y} \cdot W_{Carbon,A,y}$$

$$m_{carbon,B,y} = V_{B,dry\ gas,y} \cdot W_{carbon,dry\ gas,B,y} + m_{LPG,B,y} \cdot W_{carbon,LPG,B,y} + m_{condensate,B,y} \cdot W_{carbon,condensate,B,y}$$

$$m_{carbon,X,y} = \sum_i V_{Xi,y} \cdot W_{Carbon,Xi,y}$$

where:

| | |
|--------------------------------|---|
| $PE_{CO_2, gas, y}$ | Are the CO ₂ emissions from the project activity due to combustion, flaring or venting of recovered gas during the period y in tons of CO ₂ . |
| $m_{carbon, A, y}$ | Is the quantity of carbon in the recovered gas from the project area in during the period y in kg. |
| $m_{carbon, B, y}$ | Is the quantity of carbon in the products (dry gas, LPG, condensate) leaving the gas processing plant during the period y in kg. |
| $m_{carbon, X, y}$ | Is the quantity of carbon in recovered gas from other oil wells at all points Xi during the period y in kg. |
| $V_{B, dry\ gas, y}$ | Is the quantity of dry gas that is produced in the gas processing plant during the period y in m ³ . |
| $m_{LPG, B, y}$ | Is the quantity of LPG that is produced in the gas processing plant during the period y in kg. |
| $m_{condensate, B, y}$ | Is the quantity of condensate that is produced in the gas processing plant during the period y in kg. |
| $V_{A, y}$ | Is the volume of gas recovered during the period y in m ³ . |
| $V_{Xi, y}$ | Is the volume of gas recovered from oil well i during the period y in m ³ . |
| $w_{carbon, A, y}$ | Is the average content of carbon in the gas recovered during the period y in kg-C/m ³ . |
| $w_{carbon, dry\ gas, B, y}$ | Is the average content of carbon in dry gas during the period y in kg-C/m ³ . |
| $w_{carbon, LPG, B, y}$ | Is the average content of carbon in LPG during the period y in kg-C/kg. |
| $w_{carbon, condensate, B, y}$ | Is the average content of carbon in condensate during the period y in kg-C/kg. |
| $w_{carbon, Xi, y}$ | Is the average content of carbon in the gas recovered from oil well i during the period y in kg-C/m ³ . |

If other fossil fuels than the recovered gas are consumed at the oil well and if this consumption is a result of the project activity (e.g. substitution of gas for on-site generation or use in the compressor station), CO₂ emissions from combustion of these fuels should also be accounted.

$$PE_{CO_2, other\ fuels, y} = \frac{1}{1000} \cdot \sum_{Fuels} m_{fuel, y} \cdot NCV_{fuel} \cdot EF_{CO_2, fuel}$$

where:

| | |
|------------------------------|---|
| $PE_{CO_2, other\ fuels, y}$ | Are the CO ₂ emissions due to consumption of other fuels than the recovered gas due to the project activity during the period y in tons of CO ₂ . |
| $m_{fuel, y}$ | Is the quantity of a specific fuel type that is consumed due to the project activity during the period y in kg. |
| NCV_{fuel} | Is the net calorific value of the respective fuel type in kJ/kg. |
| $EF_{CO_2, fuel}$ | Is the CO ₂ emission factor of the respective fuel type in kg CO ₂ /kJ. |

During the monitoring period no other fossil fuels have been consumed.

CH₄ emissions from recovery and processing the gas

Fugitive CH₄ emissions occurring during the recovery and processing of gas may in some projects be small, but should be estimated as a conservative approach. Emission factors are taken from the IPCC Good Practice Guidance and/or from the 1995 Protocol for Equipment Leak

Emission Estimates, published by EPA2. Emissions are determined for all relevant activities and all equipment (such as valves, pump seals, connectors, flanges, open-ended lines, etc.)

Methane emissions are calculated for each single equipment by multiplying the CH₄ concentration in the respective stream with the appropriate emission factor as indicated in Table 1 of AM0009/version02.1.

$$PE_{CH_4, plants, y} = GWP_{CH_4} \cdot \frac{1}{1000} \cdot \sum_{equipment} w_{CH_4, stream} \cdot EF_{equipment} \cdot T_{equipment}$$

where:

| | |
|------------------------|---|
| $PE_{CH_4, plants, y}$ | Are the CH ₄ emissions from the project activity at the gas recovery facility and the gas processing plant during the period y in tons of CO ₂ equivalents. |
| GWP_{CH_4} | Is the approved Global Warming Potential for methane. |
| $T_{equipment}$ | Is the operation time of the equipment in hours (in absence of further information, the monitoring period could be considered as a conservative approach). |
| $w_{CH_4, A, y}$ | Is the average methane weight fraction in the respective stream in kg-CH ₄ /kg. |
| $EF_{equipment}$ | Is the appropriate emission factor from Table 1 (AM0009/version02.1) in kg/hour/equipment. |

CH₄ emissions from transport of the gas in pipelines under the normal operation condition

Fugitive CH₄ emissions occurring during the transport of the gas in pipelines are estimated as the same approach as “CH₄ emissions from recovery and processing the gas”, explained above.

$$PE_{CH_4, pipeline, y} = GWP_{CH_4} \cdot \frac{1}{1000} \cdot \sum_{equipment} w_{CH_4, pipeline} \cdot EF_{pipeline} \cdot T_{equipment}$$

where:

| | |
|--------------------------|---|
| $PE_{CH_4, pipeline, y}$ | Are the CH ₄ emissions from the project activity during the transport of the gas in pipelines under the normal operation during the period y in tons of CO ₂ equivalents. |
| GWP_{CH_4} | Is the approved Global Warming Potential for methane. |
| $w_{CH_4, pipeline}$ | Is the average methane weight fraction in the pipeline in kg-CH ₄ /kg. |
| $EF_{pipeline}$ | Is the appropriate emission factor from Table 1 (AM0009/version02.1) in kg/hour/pipeline |
| $T_{equipment}$ | Is the operation time of the equipment in hours (in absence of further information, the monitoring period could be considered as a conservative approach) |

CH₄ emissions from transport of the gas in pipelines when accidental event occurred

When an accident causes gas leakage from a pipeline, the gas leakage volume is less than the sum of (1) the total amount of gas that flowed during the time the accident occurred until the gas flow is shut and (2) the total amount of gas remaining in the pipeline. In the interest of conservativeness, the volume set out above should be estimated as the gas leakage from a pipeline caused by an accident.

CH₄ emissions from the transport of the gas in pipelines when accidental event occurred can be calculated as:

$$PE_{CH_4, pipeline, accident} = GWP_{CH_4} \cdot \frac{1}{1000} (V_{A, accident} + V_{remain, accident}) \cdot W_{CH_4, pipeline, accident}$$

with:

$$V_{A, accident} = t_{accident} \cdot F = (t_2 - t_1) \cdot F$$

$$V_{remain, accident} = d^2 \cdot \pi \cdot L \cdot \frac{P_p}{P_s} \cdot \frac{T_s}{T_p} \cdot \frac{V_{A, d, accident}}{\sum_i V_{xi, d, accident}}$$

where:

| | |
|--|--|
| PE _{CH₄, pipeline, accident} | Are the CH ₄ emissions from the project activity due to transport of the recovered gas in the pipeline when the accidental event happens in tons of CO ₂ equivalent. |
| GWP _{CH₄} | Is the approved Global Warming Potential for methane. |
| VA _{t, accident} | Is the volume of gas supplied from the oil well from the time the gas leakage started until the shutdown valves closed the pipeline in m ³ . |
| V _{remain, accident} | Is the volume of gas remaining in the pipeline after the shutdown valves close the pipeline in m ³ . |
| W _{CH₄, pipeline, accident} | Is the average methane weight fraction in the gas recovered in kg-CH ₄ /m ³ |
| t _{accident} | Is the time difference between t1 and t2 determined as “retention time” in seconds. |
| t1 | Is the time the gas leakage caused by the accident occurred. “t1” is determined based on the continuous monitoring data such as pressure etc. |
| t2 | Is the time that the shutdown valves closed both the upstream and downstream pipeline. “t2” is determined based on the operation data. |
| F | Is the flow rate of gas supplied from the oil well |
| d | Is the radius of the pipeline in meters. The data is derived from P & I (Piping and Instrument). |
| L | Is the length of the pipeline in meters. The data is derived from P & I (Piping and Instrument). |
| Pp | Is the pressure in the pipeline when the shutdown valves close both the upstream and downstream of the pipeline in atmospheres (atm). |
| Ps | Is the standard pressure in atm. |
| Tp | Is the temperature in the pipeline when the shutdown valves close both the upstream and downstream of the pipeline in degrees Centigrade. |
| Ts | Is the standard temperature in Centigrade. |
| VA _{d, accident} | Is the volume of gas supplied to the pipeline from oil well before the accident occurs during the period day in m ³ . |
| V _{xi, d, accident} | Is the volume of gas supplied to the pipeline from oil well i before the accident occurs during the period day in m ³ . |

During the monitoring period no accidental events occurred.

3.3 Leakage

No leakage reported (see section B.6.1 of the Project Design Document v3.12 dated 13th December 2007, and available upon the UNFCCC website)
(<http://cdm.unfccc.int/Projects/DB/LRQA%20Ltd1180000727.07/view>)

3.4 Emission Reductions

The formula used for determination of the emission reductions is described in section B.7.1 of the Project Design Document v3.12 dated 13th December 2007, and available upon the UNFCCC website (<http://cdm.unfccc.int/Projects/DB/LRQA%20Ltd1180000727.07/view>)

Emission reductions are calculated as the difference between baseline and project emissions, taking into account any adjustments for leakage:

$$EF_y = BL_y - PE_{CO_2, other\ fuels, y} - PE_{CH_4, plants, y} - PE_{CH_4, pipeline, y} - PE_{CH_4, pipeline, accident} - L_y \dots\dots\dots$$

where:

| | |
|---------------------------------|---|
| EF_y | Are the emissions reductions of the project activity, adjusted for leakage, during the period y in tons of CO ₂ equivalent. |
| BL_y | Are the baseline emissions during the period y in tons of CO ₂ equivalent. |
| $PE_{CO_2, gas, y}$ | Are the CO ₂ emissions from the project activity due to combustion, flaring or venting of recovered gas during the period y in tons of CO ₂ . |
| $PE_{CO_2, other\ fuels, y}$ | Are the CO ₂ emissions due to consumption of other fuels than the recovered gas due to the project activity during the period y in tons of CO ₂ . |
| $PE_{CH_4, plants, y}$ | Are the CH ₄ emissions from the project activity at the gas recovery facility and the gas processing plant during the period y in tons of CO ₂ equivalent. |
| $PE_{CH_4, pipeline, y}$ | Are the CH ₄ emissions from the project activity due to transport of the recovered gas in the pipeline during the period y in tons of CO ₂ equivalent. |
| $PE_{CH_4, pipeline, accident}$ | Are the CH ₄ emissions from the project activity due to transport of the recovered gas in the pipeline when the accidental event occurs in tons of CO ₂ equivalent. |
| L_y | Are any leakage emissions during the period y in tons of CO ₂ equivalent. |

4. Calculation of Emission Reductions

The data required to calculate baseline emissions, project emissions and leakage emissions is transferred into a protected spreadsheet which will calculate the emission reductions according to the formulae described in previous section. The CDM spreadsheet has been provided to the DOE for verification purposes.

Sections below provide results of the monitoring process for the monitoring period stated.

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4.1 Baseline Emissions

4.1.1 Input Parameters

16 February 2009 – 30 September 2009

| | | | 12" LP Gas | 4" HP Gas | 6" PTG Gas | M01 Dry Gas | LPG | Condensate | | |
|--------------|------|-----------|-------------------|-----------------|---------------|-------------------|-------------------|------------------|------------------|------------------|
| Date | From | To | | | | | | LPG | 1st Grad | 2nd Grad |
| | | Month | mmscf | mmscf | mmscf | mmscf | t | Sm3 | Sm3 | Sm3 |
| 16 | 28 | February | 251.3763 | 0.0000 | 0.0000 | 200.4619 | 1,105.658 | 342.043 | 243.847 | 241.648 |
| 1 | 31 | March | 566.6420 | 0.0000 | 0.0000 | 466.3320 | 2,090.159 | 581.505 | 559.348 | 666.544 |
| 1 | 30 | April | 575.8292 | 0.0000 | 0.0000 | 453.8963 | 2,727.104 | 682.506 | 623.077 | 778.555 |
| 1 | 31 | May | 565.1000 | 0.0000 | 0.0000 | 439.8231 | 3,003.921 | 1,049.236 | 651.317 | 780.349 |
| 1 | 30 | June | 593.6263 | 0.0000 | 0.0000 | 459.7273 | 2,852.472 | 1,010.400 | 736.970 | 927.111 |
| 1 | 31 | July | 667.1160 | 0.0000 | 0.0000 | 521.5360 | 3,251.304 | 1,245.769 | 750.557 | 1,048.786 |
| 1 | 31 | August | 646.7353 | 0.0000 | 0.0000 | 505.3423 | 3,277.541 | 1,186.978 | 743.630 | 975.118 |
| 1 | 30 | September | 507.6707 | 0.0000 | 0.0000 | 400.4665 | 2,714.359 | 1,047.918 | 597.373 | 670.085 |
| Total | | | 4,374.0958 | 0.000000 | 0.0000 | 3,447.5854 | 21,022.518 | 7,146.357 | 4,906.119 | 6,088.196 |

Remarks:

- There are 28316.8466 standard cubic meters in one million standard cubic feet (source: API "Compendium for Greenhouse Gas Emission Methodologies for the Oil and Gas Industry", Feb 2004, American Petroleum Institute).
- On 31 March 2008 the contract PDT ended and no gas was supplied through the 6" pipeline since then.
- On 17 October 2008, the 4 inch line gas input to Odira has been shut off.

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4.1.2 Baseline

16 February 2009 – 30 September 2009

| Date | | | 12" LP Gas | | | 4" HP Gas | | | 6" PTD Gas | | |
|--------------|----|-----------|------------------------|-----------|--------------------|-----------|-----------|------|------------|-----------|------|
| From | To | Month | Sm3 | kgCO2/Sm3 | tCO2 | Sm3 | kgCO2/Sm3 | tCO2 | Sm3 | kgCO2/Sm3 | tCO2 |
| 16 | 28 | February | 7,118,184.981 | 3.090 | 21,998.187 | - | - | - | - | - | - |
| 1 | 31 | March | 16,045,516.518 | 3.076 | 49,348.712 | - | - | - | - | - | - |
| 1 | 30 | April | 16,305,669.082 | 3.080 | 50,216.151 | - | - | - | - | - | - |
| 1 | 31 | May | 16,001,851.935 | 3.072 | 49,160.342 | - | - | - | - | - | - |
| 1 | 30 | June | 16,809,626.893 | 3.033 | 50,986.168 | - | - | - | - | - | - |
| 1 | 31 | July | 18,890,623.705 | 3.017 | 56,996.715 | - | - | - | - | - | - |
| 1 | 31 | August | 18,313,506.480 | 3.100 | 56,773.651 | - | - | - | - | - | - |
| 1 | 30 | September | 14,017,851.662 | 3.100 | 43,455.921 | - | - | - | - | - | - |
| Total | | | 123,502,831.254 | | 378,935.848 | - | - | - | - | - | - |

Remarks:

- There are 28316.8466 standard cubic meters in one million standard cubic feet (source: API "Compendium for Greenhouse Gas Emission Methodologies for the Oil and Gas Industry", Feb 2004, American Petroleum Institute).
- On 31 March 2008 the contract PDT ended and no gas was supplied through the 6" pipeline since then.
- Since 17 October 2008, no gas was supplied through the 4 inch line gas input.

4.2 Project Emissions (PE)

4.2.1 PE CO₂ gas

16 February 2009 – 30 September 2009

| Date | | | V _A | W _{carbonA} | M _{carbonA} | V _{drygas} | W _{carbondrygas} | M _{carbondrygas} | M _{LPG} | W _{carbonLP} | M _{carbonLPG} |
|--------------|----|-----------|------------------------|----------------------|----------------------|-----------------------|------------------------------------|---------------------------|-------------------|-----------------------|------------------------|
| | | | (Import) | (CO ₂) | | Dry Gas | Dry Gas | Dry Gas | LPG | LPG | LPG |
| From | To | Month | Sm ³ | kgC/Sm ³ | tCO ₂ | Sm ³ | kgCO ₂ /Sm ³ | tCO ₂ | t | tCO ₂ /t | tCO ₂ |
| 16 | 28 | February | 7,118,184.981 | 3.090 | 21,998.187 | 5,676,449.553 | 2.487 | 14,119.127 | 1,105.658 | 3.011 | 3,329.172 |
| 1 | 31 | March | 16,045,516.518 | 3.076 | 49,348.712 | 13,205,053.294 | 2.520 | 33,272.959 | 2,090.159 | 3.010 | 6,291.342 |
| 1 | 30 | April | 16,305,669.082 | 3.080 | 50,216.151 | 12,852,913.443 | 2.485 | 31,940.962 | 2,727.104 | 3.012 | 8,213.678 |
| 1 | 31 | May | 16,001,851.935 | 3.072 | 49,160.342 | 12,454,404.749 | 2.492 | 31,040.390 | 3,003.921 | 3.011 | 9,045.977 |
| 1 | 30 | June | 16,809,626.893 | 3.033 | 50,986.168 | 13,018,028.995 | 2.582 | 33,614.814 | 2,852.472 | 3.011 | 8,590.117 |
| 1 | 31 | July | 18,890,623.705 | 3.017 | 56,996.715 | 14,768,256.682 | 2.426 | 35,826.710 | 3,251.304 | 3.011 | 9,788.744 |
| 1 | 31 | August | 18,313,506.480 | 3.100 | 56,773.651 | 14,309,702.108 | 2.438 | 34,890.437 | 3,277.541 | 3.010 | 9,865.352 |
| 1 | 30 | September | 14,017,851.662 | 3.100 | 43,455.921 | 11,339,949.811 | 2.397 | 27,185.761 | 1,344.210 | 3.011 | 4,047.629 |
| Total | | | 123,502,831.254 | | 335,479.927 | 97,624,758.634 | | 241,891.160 | 19,652.369 | | 59,172.012 |

| Date | | | V _{condensate} | SG _{Condensate} | M _{condensate} | W _{carboncondensate} | M _{carboncondensate} | M _{carbonB} |
|--------------|----|-----------|-------------------------|--------------------------|-------------------------|-------------------------------|-------------------------------|----------------------|
| | | | Cond | Cond | Cond | Cond | Cond | |
| From | To | Month | Sm ³ | kg/lit | t | tCO ₂ /t | tCO ₂ | tCO ₂ |
| 16 | 28 | February | 827.538 | 0.673 | 557.169 | 3.062 | 1,705.859 | 19,154.158 |
| 1 | 31 | March | 1,807.398 | 0.674 | 1,217.463 | 3.061 | 3,726.420 | 43,290.721 |
| 1 | 30 | April | 2,084.139 | 0.676 | 1,408.691 | 3.063 | 4,314.408 | 44,469.048 |
| 1 | 31 | May | 2,480.902 | 0.675 | 1,673.782 | 3.069 | 5,136.680 | 45,223.047 |
| 1 | 30 | June | 2,674.482 | 0.675 | 1,806.345 | 3.054 | 5,516.980 | 47,721.911 |
| 1 | 31 | July | 3,045.112 | 0.675 | 2,056.669 | 3.052 | 6,276.886 | 51,892.340 |
| 1 | 31 | August | 2,905.726 | 0.675 | 1,962.527 | 3.049 | 5,984.214 | 50,740.003 |
| 1 | 30 | September | 1,123.330 | 0.675 | 758.697 | 3.060 | 2,321.566 | 33,554.957 |
| Total | | | 16,948.626 | | 11,441.343 | | 34,983.012 | 336,046.185 |

16 February 2009 – 30 September 2009

| | | | V _{condLPG} | SG _{CondLPG} | M _{condLPG} | W _{carboncondLPG} | M _{carboncondLPG} | V _{cond1stGrad} | SG _{Cond1stGrad} | M _{cond1stGrad} |
|-------|----|-----------|----------------------|-----------------------|----------------------|----------------------------|----------------------------|--------------------------|---------------------------|--------------------------|
| Date | | | Cond | Cond | Cond | Cond | Cond | Cond | Cond | Cond |
| From | To | Month | Sm3 | kg/lit | t | tCO2/t | tCO2 | Sm3 | kg/lit | t |
| 16 | 28 | February | 342.04 | 0.64 | 219.79 | 3.05 | 671.15 | 243.85 | 0.68 | 164.81 |
| 1 | 31 | March | 581.51 | 0.64 | 374.14 | 3.05 | 1,140.84 | 559.35 | 0.68 | 378.55 |
| 1 | 30 | April | 682.51 | 0.65 | 445.15 | 3.05 | 1,357.31 | 623.08 | 0.68 | 421.22 |
| 1 | 31 | May | 1,049.24 | 0.65 | 681.50 | 3.06 | 2,086.33 | 651.32 | 0.68 | 440.98 |
| 1 | 30 | June | 1,010.40 | 0.65 | 656.76 | 3.06 | 2,008.54 | 736.97 | 0.68 | 498.34 |
| 1 | 31 | July | 1,245.77 | 0.65 | 809.75 | 3.05 | 2,470.57 | 750.56 | 0.68 | 507.53 |
| 1 | 31 | August | 1,186.98 | 0.65 | 771.54 | 3.04 | 2,349.31 | 743.63 | 0.68 | 502.84 |
| 1 | 30 | September | 489.62 | 0.65 | 318.25 | 3.05 | 971.30 | 286.42 | 0.68 | 193.68 |
| Total | | | 6,588.06 | | 4,276.88 | | 13,055.35 | 4,595.17 | | 3,107.95 |

| | | | W _{carboncond1stGrad} | M _{carboncond1stGrad} | V _{cond2ndGrad} | SG _{Cond2ndGrad} | M _{cond2ndGrad} | W _{carboncond2ndGrad} | M _{carboncond2ndGrad} |
|-------|----|-----------|--------------------------------|--------------------------------|--------------------------|---------------------------|--------------------------|--------------------------------|--------------------------------|
| Date | | | Cond | Cond | Cond | Cond | Cond | Cond | Cond |
| From | To | Month | tCO2/t | tCO2 | Sm3 | kg/lit | t | tCO2/t | tCO2 |
| 16 | 28 | February | 3.06 | 504.84 | 241.65 | 0.70 | 169.50 | 3.07 | 520.03 |
| 1 | 31 | March | 3.06 | 1,159.83 | 666.54 | 0.70 | 467.00 | 3.07 | 1,433.37 |
| 1 | 30 | April | 3.06 | 1,290.85 | 778.56 | 0.70 | 544.57 | 3.07 | 1,674.28 |
| 1 | 31 | May | 3.07 | 1,353.55 | 780.35 | 0.70 | 544.23 | 3.08 | 1,674.01 |
| 1 | 30 | June | 3.05 | 1,520.20 | 927.11 | 0.70 | 648.98 | 3.05 | 1,981.91 |
| 1 | 31 | July | 3.05 | 1,548.64 | 1,048.79 | 0.70 | 734.15 | 3.05 | 2,241.74 |
| 1 | 31 | August | 3.05 | 1,533.85 | 975.12 | 0.70 | 682.58 | 3.05 | 2,083.50 |
| 1 | 30 | September | 3.06 | 592.80 | 347.28 | 0.70 | 243.10 | 3.07 | 745.61 |
| Total | | | | 9,504.57 | 5,765.40 | | 4,034.11 | | 12,354.45 |

4.2.2 Project Emissions (PE) Other fossil fuels

During the reporting period no other fossil fuels have been used.

4.2.3 Fugitive LPG Plant Emissions (PECH₄ Plant)

16 February 2009 – 30 September 2009
Fugitive LPG plant emissions (PECH₄Plant)

| Equipment Type | Factor kg/hr | Number | CH ₄ ton | CO ₂ e ton | Notes |
|------------------------|-----------------|--------|------------------------|--------------------------|--|
| | | | | | |
| Valves | 4.50E-03 | 215 | 3.41 | 71.59 | Annual Op Hours 8592 Wt CH ₄ % 41.0116055 Equipment inventory spreadsheet CH ₄ - average wet gas HP and LP Time assumes one week TAR CH ₄ GWP - 21 |
| Pump seals | 2.40E-03 | 0 | 0.00 | 0.00 | |
| Other | 8.80E-03 | 229 | 7.10 | 149.12 | |
| Connectors | 2.00E-04 | 0 | 0.00 | 0.00 | |
| Flanges | 3.90E-04 | 64 | 0.09 | 1.85 | |
| Open ended lines | 2.00E-03 | 0 | 0.00 | 0.00 | |
| Valves (light oil) | 2.50E-03 | 444 | 3.91 | 82.14 | |
| Pump seals (light oil) | 1.30E-02 | 0 | 0.00 | 0.00 | |
| Other (light oil) | 7.50E-03 | 0 | 0.00 | 0.00 | |
| Connectors (light oil) | 2.10E-04 | 0 | 0.00 | 0.00 | |
| Flanges (light oil) | 1.10E-04 | 481 | 0.19 | 3.92 | |
| Open ended lines | 1.40E-03 | 0 | 0.00 | 0.00 | |
| Total | | | 14.70 | 308.61 | |
| | | | | | PE _{CH₄Plant} 308.61 tCO ₂ |

(*) source: US EPA-453/R-95-017 Table 2.4,page 2-15.

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4.2.4 Fugitive Emissions from Pipeline (PE CH₄ Pipeline)

16 February 2009 – 30 September 2009

Fugitive emissions from pipeline (PECH4Pipeline)

| Equipment Type | Factor kg/hr | Number | CH ₄ ton | CO ₂ e ton | Notes Annual Op Hours 8592 Wt CH ₄ % 56.3134617 Source - Equipment inventory s/s CH ₄ - average dry gas analysis Time assumes one week TAR CH ₄ GWP - 21 |
|------------------|-----------------|--------|------------------------|--------------------------|--|
| Valves | 4.50E-03 | 4 | 0.09 | 1.83 | |
| Pump seals | 2.40E-03 | 0 | 0.00 | 0.00 | |
| Other | 8.80E-03 | 2 | 0.09 | 1.79 | |
| Connectors | 2.00E-04 | 0 | 0.00 | 0.00 | |
| Flanges | 3.90E-04 | 20 | 0.04 | 0.79 | |
| Open ended lines | 2.00E-03 | 0 | 0.00 | 0.00 | |
| Total | | | 0.21 | 4.41 | |
| | | | | | PE _{CH4Pipeline} 4.41 tCO ₂ |

(*) source: US EPA-453/R-95-017 Table 2.4,page 2-15.

4.2.5 Project Emissions Pipeline Accident (PE CH₄ pipeline accident)

During the reporting period no accidental events occurred.

4.3 Leakage

N/A.

4.4 Emission Reductions (tCO₂eq)

16 February 2009 – 30 September 2009

| Date | | Month | BL | PECO ₂ gas | PECO ₂ Other | PECH ₄ Plant | PECH ₄ Pipeline | PECH ₄ Accident | CER |
|--------------|----|-----------|--------------------|-----------------------|-------------------------|-------------------------|----------------------------|----------------------------|----------------|
| From | To | | | | | | | | |
| 16 | 28 | February | 21,998.187 | 2,844.029 | 0.000 | 11.940 | 0.171 | 0.000 | 19,142.047 |
| 1 | 31 | March | 49,348.712 | 6,057.991 | 0.000 | 25.718 | 0.367 | 0.000 | 43,264.636 |
| 1 | 30 | April | 50,216.151 | 5,747.102 | 0.000 | 25.718 | 0.367 | 0.000 | 44,442.963 |
| 1 | 31 | May | 49,160.342 | 3,937.295 | 0.000 | 25.718 | 0.367 | 0.000 | 45,196.962 |
| 1 | 30 | June | 50,986.168 | 3,264.258 | 0.000 | 25.718 | 0.367 | 0.000 | 47,695.825 |
| 1 | 31 | July | 56,996.715 | 5,104.374 | 0.000 | 25.718 | 0.367 | 0.000 | 51,866.255 |
| 1 | 31 | August | 56,773.651 | 6,033.649 | 0.000 | 25.718 | 0.367 | 0.000 | 50,713.918 |
| 1 | 30 | September | 44,565.065 | 4,420.790 | 0.000 | 25.718 | 0.367 | 0.000 | 40,118.189 |
| Total | | | 380,044.991 | 37,409.489 | 0.000 | 191.965 | 2.743 | 0.000 | 342,441 |

Total 16 February 2009 – 30 September 2009 (inclusive) = 342,441 tCO₂eq.

4.5 Comparison Actual Emission Reductions with PDD estimate (tCO₂eq)

| PDD Estimate | | | Actual Achieved | | | | Difference PDD/Actual Achieved (%) | | Comment |
|--------------|------|---------|-------------------|------------|------|--------|------------------------------------|---------|----------|
| Year | | CER PDD | Monitoring Period | | | | Difference PDD | | |
| | | | Begin date | End date | Days | CERs | / Actual | Report | |
| 3 | 2009 | 682202 | 1/01/2009 | 15/02/2009 | 47 | 65549 | | MR4 | Estimate |
| | | | 16/02/2009 | 30/09/2009 | 226 | 342441 | | MR5 | |
| | | | 1/10/2009 | 31/12/2009 | 92 | 133855 | | | |
| | | | Total 2009 | | 365 | 541845 | | -20,57% | |

Annex A Monitored Parameters

| Parameter | Data Set / Document | Data | | Storage | Soft Copies | | Retention Time |
|------------------------------------|---|---|----------------------------|--------------------------------------|-----------------------------------|--------------------------|--------------------------|
| | | Output | Format | | Transcribed to | Location | |
| V _{A,y} | Flow Meter 12" (Orifice Meter) | Hourly data, Flow Computer Pertamina | Soft/Hard copy (print out) | Pertamina Control Room / | Morning and Monthly Report | Odira Office, SCC Office | Crediting Period +2 year |
| | | Barton charts | Hard copy (card read out) | Pertamina Control Room | Morning reports back-up | Odira Office, SCC Office | Crediting Period +2 year |
| | Flow Meter 4" (Orifice Meter) | Hourly data, Flow Computer Pertamina | Soft/Hard copy (print out) | Pertamina Control Room / Odira Plant | Morning and Monthly Report | Odira Office, SCC Office | Crediting Period +2 year |
| | | Barton charts | Hard copy (card read out) | Pertamina Control Room | Morning reports back-up | Odira Office, SCC Office | Crediting Period +2 year |
| W _{carbon,A, y} | Pertamina Tegal Gede Gas Chromatograph (GC) | Weekly Composition | Hard copy | Pertamina Lab/ Odira Plant | CDM Monitoring Report Spreadsheet | Odira Office, SCC Office | Crediting Period +2 year |
| V _{B, dry gas,y} | Flow Meter M-01 (Orifice Meter) | Hourly data, Flow computer | Soft/Hard copy (print out) | Odira Plant | Morning and Monthly Report | Odira Office, SCC Office | Crediting Period +2 year |
| | | Barton charts | Hard copy (card read out) | Odira Plant | Morning reports back-up | Odira Office, SCC Office | Crediting Period +2 year |
| W _{carbon, dry gas, B, y} | Pertamina GC | Weekly Composition | Hard copy | Pertamina Lab/ Odira Plant | CDM Monitoring Report Spreadsheet | Odira Office, SCC Office | Crediting Period +2 year |
| M _{LPG, B, y} | Orifice meter | Continuous Recording, Daily Aggregation | Hard copy | Odira Plant | Morning and Monthly Report | Odira Office, SCC Office | Crediting Period +2 year |
| W _{carbon, LPG, B, y} | Odira Gas Chromatograph | Weekly Composition | Hard copy | Odira Plant | CDM Monitoring Report Spreadsheet | Odira Office, SCC Office | Crediting Period +2 year |
| M _{Condensate, B, y} | Orifice meter, Micro meter, Turbine meter, weighbridge, roadtankers | Continuous Recording, Daily Aggregation | Hard copy | Odira Plant | Morning and Monthly Report | Odira Office, SCC Office | Crediting Period +2 year |

CDM Monitoring Report

Project 1144 : Tambun LPG Associated Gas Recovery and Utilization Project.

| Parameter | Data Set / Document | Data | | Storage | Soft Copies | | Retention Time |
|---------------------------------------|----------------------------|-------------------------|----------------|--|-----------------------------------|--------------------------|--------------------------|
| | | Output | Format | Location | Transcribed to | Location | |
| W _{Carbon, Condensate, B, y} | Lemigas Lab Instruments | Monthly Composition | Hard copy | Lemigas/ Odira Plant | CDM Monitoring Report Spreadsheet | Odira Office, SCC Office | Crediting Period +2 year |
| M _{fuel, y} | Not applicable | | | | | | |
| W _{carbon, IPCC} | Not applicable | | | | | | |
| Fugitive Emissions | Plant Survey | Survey Report | Hard/Soft Copy | SCC Office (S server) | CDM Monitoring Report Spreadsheet | Odira Office, SCC Office | Crediting Period +2 year |
| T _{equipment} | Time recording | Operation Data | Hard Copy | Odira Operational Control Room | CDM Monitoring Report Spreadsheet | Odira Office, SCC Office | Crediting Period +2 year |
| W _{CH4, A, y} | Plant Survey | Survey Report | Hard/Soft Copy | SCC Office (S server) | CDM Monitoring Report Spreadsheet | Odira Office, SCC Office | Crediting Period +2 year |
| Fugitive Emissions | Plant Survey | Survey Report | Hard/Soft Copy | SCC Office (S server) | CDM Monitoring Report Spreadsheet | Odira Office, SCC Office | Crediting Period +2 year |
| T _{equipment, pipeline} | Time recording | Operation Data | Hard Copy | Odira Operational Control Room | CDM Monitoring Report Spreadsheet | Odira Office, SCC Office | Crediting Period +2 year |
| W _{CH4, pipeline} | Plant Survey | Survey Report | Hard/Soft Copy | SCC Office (S server) | CDM Monitoring Report Spreadsheet | Odira Office, SCC Office | Crediting Period +2 year |
| T1, T2 | Time recording | Operation Data | Hard Copy | Odira Operational Control Room | CDM Monitoring Report Spreadsheet | Odira Office, SCC Office | Crediting Period +2 year |
| P | Pressure Pipeline | Operation Data | Hard Copy | Odira Operational Control Room | CDM Monitoring Report Spreadsheet | Odira Office, SCC Office | Crediting Period +2 year |
| T | Temperature Pipeline | Operation Data | Hard Copy | Odira Operational Control Room | CDM Monitoring Report Spreadsheet | Odira Office, SCC Office | Crediting Period +2 year |
| CER Calculation | CDM Monitoring Spreadsheet | Emission reduction data | Xls format | SCC Office (S-server) | | | Crediting Period +2 year |
| CDM Monitoring Report | | Emission reduction data | Soft/hard Copy | SCC Office (S server) | | | Crediting Period +2 year |
| Internal Audit Report(s) | | QC/QA | Soft Copy | SCC Office (S server) | | | Crediting Period +2 year |
| Maintenance Reports | | QC/QA | Hard/soft copy | Odira Plant (Maintenance Dept) | | | Crediting Period +2 year |
| Calibration Records | | QC/QA | Hard/soft copy | Odira Plant (Maintenance Dept)/SCC Office (S-server) | | | Crediting Period +2 year |
| Project Design Document | | | | UNFCC Website / SCC Office (S server) | | | Crediting Period +2 year |
| Approved Methodology | | | | UNFCC Website / SCC Office (S server) | | | Crediting Period +2 year |
| DOE verification reports | | | | SCC Office (S server) | | | Crediting Period +2 year |