MONITORING REPORT FORM (CDM-MR) *
Version 01 - in effect as of: 28/09/2010

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* as contained within the document entitled "Guidelines for completing the monitoring report form (CDM-MR)" (EB 54 meeting report, annex 34).

MONITORING REPORT
Version 1.1 – 05/01/2011(dd/mm/yyyy)

N_2O ABATEMENT PROJECT OF CAPRO CORPORATION
4665
Monitoring period #1 (09/06/2011 – 31/08/2011)

SECTION A. General description of the project activity

A.1. Brief description of the project activity:

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1. Purpose of the project activity and the measures taken to reduce greenhouse gas emissions;
   The proposed project is to reduce N_2O emissions of the tail gas emitted from Caprolactam production process in Capro Corporation (hereinafter "Capro") by installing catalytic N_2O destruction system.

2. Brief description of the installed technology and equipments;
   N_2O treatment system for this project is CRI N_2O abatement system, which is N_2O decomposition catalyst at the tail gas. Therefore, CRI system applies to tertiary treatment, which does not affect the existing yield of caprolactam as it just treats the tail gas. In addition, the catalyst system is remarkably efficient as CRI technology is direct N_2O decomposition process that does not require the addition of any reductant and its pressure drop is small.

3. Relevant dates for the project activity.

Relevant dates (dd/mm/yyyy)	The Actions for Implementation of Project activity
04/10/2010	Starting Construction of N_2O abatement system
23/03/2011	Conducting trial run after loading N_2O decomposition catalyst
15/04/2011	Installing of Measuring instruments including AMS
02/05/2011	Completing Construction of N_2O abatement system
23/05/2011 ~27/05/2011	Field Test for Quality Assurance of installation and calibration of AMS (QAL2)
09/06/2011	Starting continued operating of N_2O Abatement System(NAS) and monitoring system
26/9/2011 ~29/9/2011	Additional Field Test for Quality Assurance of installation and calibration of AMS (QAL2)

4. Total emission reductions achieved in this monitoring period: 148441tonCO_2

A.2. Project Participants

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Name of Party involved	Project participants(*) (as applicable)	Party involved considered as project participants
The Republic of Korea(host)	Capro Corporation Hyosung Ebara Engineering Co., Ltd. Hyosung Corporation	No

A.3. Location of the project activity:

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The geographic location of the Capro caprolactam production plant is shown in Figure 1. The plant is located in the south-eastern part of the Republic of Korea: the east longitude is about 129.3280 and the north latitude is about 35.4958. The full address of this facility is 402-1, Bugok-dong, Nam-gu, Ulsan in Korea.

Figure A.1 The location of Capro caprolactam production plant

A.4. Technical description of the project

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1. General Introduction

Caprolactam is produced by cyclohexane, ammonia, and sulphur as its primary raw materials, and Ammonium sulfate comes out as a by-product, which is supplied as nitrogen fertilizer and a chemical feedstock for industrial uses.

In Capro, the main process of caprolactam production is as follows:

Hydroxylamine sulfate preparation ;

Ammonium carbonate preparation

$2NH_4OH + CO_2 \rightarrow (NH_4)_2CO_3 + H_2O$

Ammonia oxidation

$$4NH_3 + 5O_2 \xrightarrow{\text{Pt-Rh catalyst}} 4NO + 6H_2O$$

$(2NO + O_2 \rightarrow 2NO_2)$

Ammonium Nitrite Preparation;

$(NH_4)_2CO_3 + NO + NO_2 \rightarrow 2NH_4NO_2 + CO_2$

Hydroxylamine disulfonic ammonia Preparation;

$NH_4NO_2 + NH_4OH + 2SO_2 \rightarrow NOH(SO_3NH_4)_2$

Hydroxylamine Sulfate Preparation;

$NOH(SO_3NH_4)_2 + H_2O \rightarrow NHOHSO_3NH_4 + NH_4HSO_4$

$2NHOHSO_3NH_4 + 2H_2O \rightarrow (NH_2OH)_2H_2SO_4$ (Hydroxylamine sulfate) + $(NH_4)_2SO_4$

Cyclohexanone preparation

$$C_6H_{12} \xrightarrow{\text{Co catalyst, }[O_2]} C_6H_{10}O \text{ (Cyclohexanone)}$$

Oximation Reaction;

$(NH_2OH)_2H_2SO_4 + 2C_6H_{10}O \rightarrow 2C_6H_{10}NOH$ (Cyclohexanone oxime)+ $H_2SO_4 + H_2O$

Beckmann rearrangement;

$$C_6H_{10}NOH \xrightarrow{H_2SO_4\text{ catalyst}} C_6H_{10}NOH \text{ (Caprolactam)}$$

Cyclohexanone oxime reacts with sulfuric acid catalyst to caprolactam as final product. The structural formula of Beckmann rearrangement is shown in Figure 2.

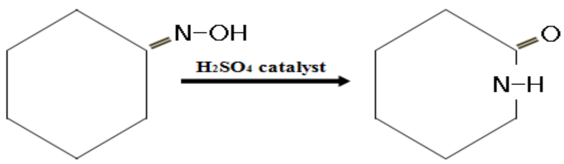

Figure A.2 Structural formula of Beckmann rearrangement

The block flow diagram for existed caprolactam production process of Capro is shown in Figure 3.

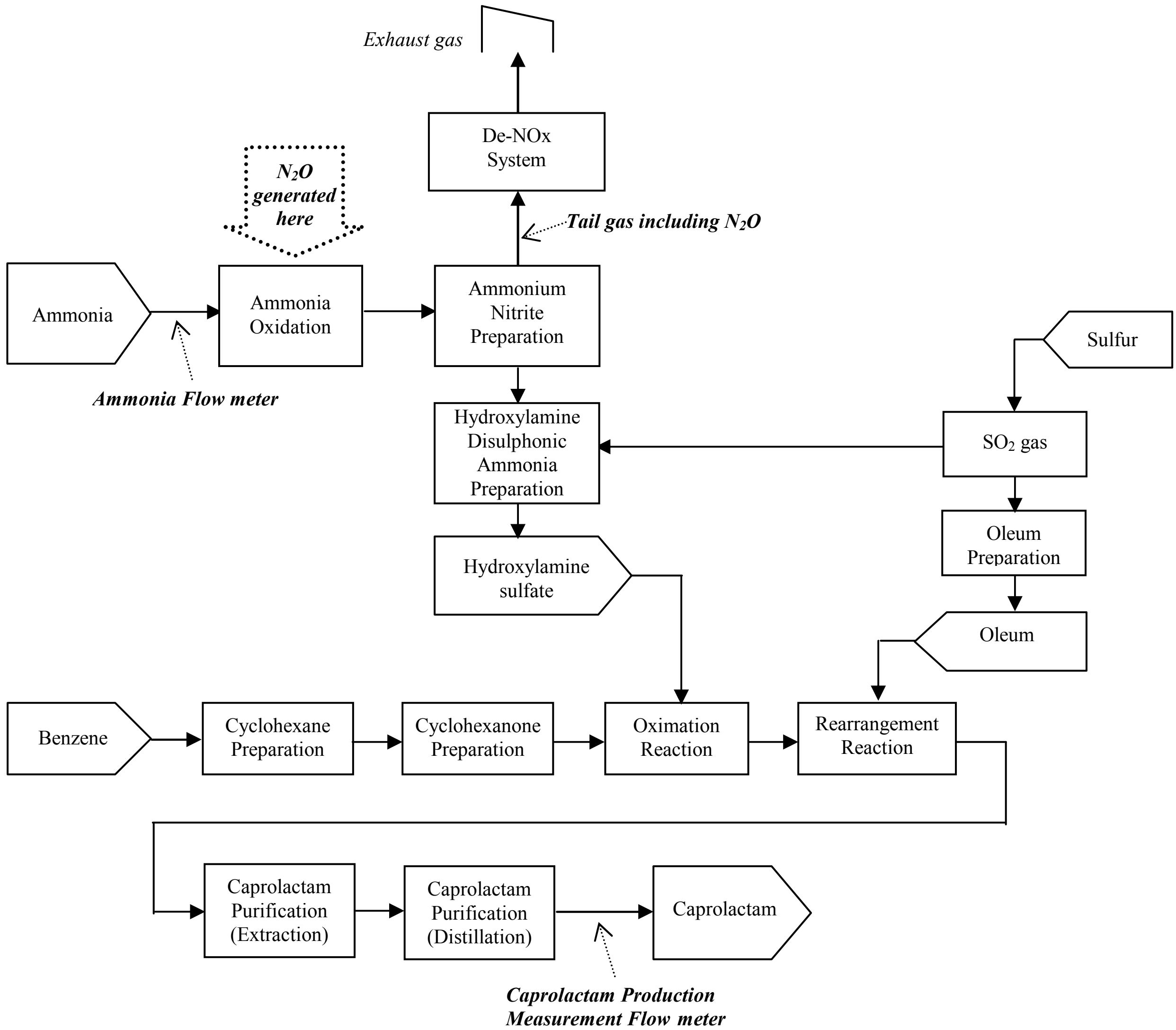

Figure A.3 Block flow diagram for caprolactam production process

Ammonia oxidation reaction is necessary to generate NO and NO_2, which are going to be the reactants for Ammonium nitrite. (This Ammonium nitrite will induce Hydroxylamine sulphate, and finally caprolactam will be produced, through the complicated reaction pathway, as previous stated at the paragraph to explain the main process of caprolactam production.)

Nitrous oxide (N_2O) is generated as an undesired by-product through the side reaction of Ammonia oxidation as follows:

$4NH_3 + 5O_2 \rightarrow 4NO + 6H_2O$	(Main reaction)
$(2NO + O_2 \rightarrow 2NO_2)$	(Desired in the NO oxidation process)
$4NH_3 + 3O_2 \rightarrow 2N_2 + 6H_2O$	(Side reaction)
$4NH_3 + 4O_2 \rightarrow 2N_2O + 6H_2O$	(Side reaction)

In this project, two plants (Plant I, Plant II) are included. In each plant, there are two of the Ammonium Oxidation Reactors (AORs), the ammonia gas is equally fed to the both of AORs through the one line with one flow meter. Input ammonia is oxidized by passing through the Pt-Rh Catalyst gauze located in AOR.

2. Project Specific description

De-N_2O system for this project is to destruct the N_2O included in tail gas by catalyst without any reducing agent.

$$2N_2O \xrightarrow{\text{Catalyst}} 2N_2 + O_2$$

The catalytic reactor designed by Hyosung Ebara Engineering Co. was derived from RTO (Regenerative Thermal Oxidizer) , to save the energy required for catalytic reaction to decompose N_2O, and this N_2O destruction facility is the so-called "Regenerative Catalytic System" (Figure 4). Where, liquefied natural gas (LNG, hereafter "natural gas") is put in to this system as a fuel, not reducing agent, to supply the energy required for the de-N_2O catalytic reaction. Catalyst is provided by CRI.

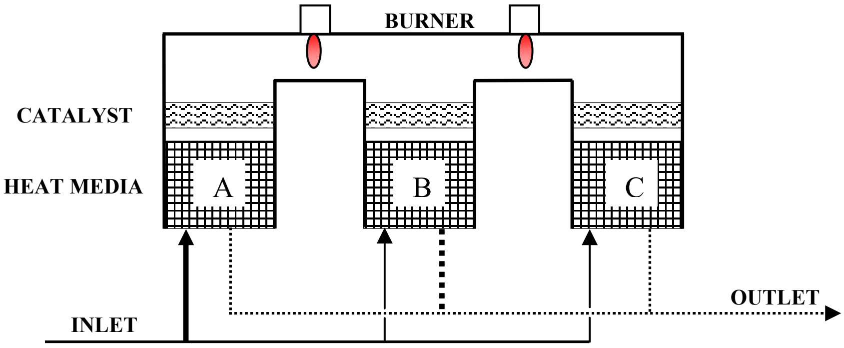

Figure A.4 Overview of Regenerative Catalytic System

The principle of performance can be step-wisely described with Figure 4 as follows: At the inlet of De-N_2O system, in-flowed tail-gas is heated up to 550℃ by going to heat media A(previously heated), before N_2O included in the heated tail is decomposed while that tail gas is pass through catalytic bed located on the top of heat storage media A. And then, N2O in the once treated tail gas is decomposed again by the next catalyst bed and the heat storage media B, to which the heat hold in two-times-treated tail gas is transfer. After this, two-times-treated tail gas is going out. Next, tail gas is injected in to the heat media B which is charged with heat transferred from the outflow according to the way explain just above. And the tail gas passed through the heat storage media B and the upper catalyst bed is going to the other catalyst bed and the heat media C. Finally, the tail gas from the plant goes to the media C heated by the previous outflow, this tail gas is flowed reversely to the media B and comes out. In this way, tail gas in-and-out is continuously rotated. The same De-N_2O processes have been applied to Plant I and II.

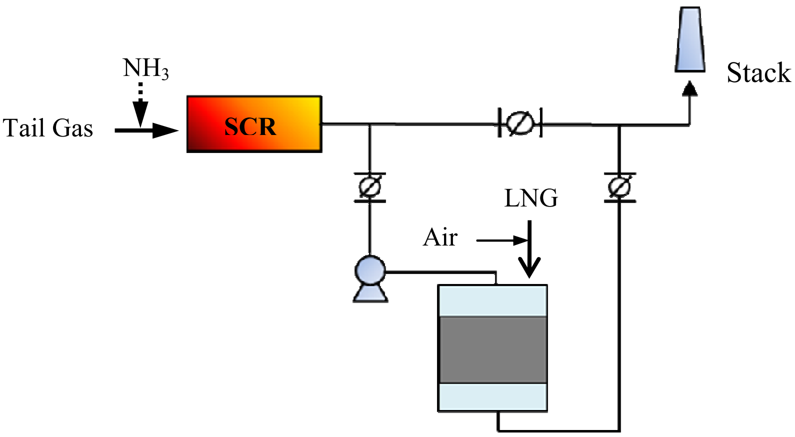

Figure A.5 Overview of the De-N_2O process in Plant I and II

A.5. Title, reference and version of the baseline and monitoring methodology applied to the project activity:

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AM0028 (version 05)

"Catalytic N_2O destruction in the tail gas of Nitric Acid Plants or Caprolactam Production"

A.6. Registration date of the project activity:

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09/06/2011 (dd/mm/yyyy)

A.7. Crediting period of the project activity and related information (start date and choice of crediting period):

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	The date accepted by the Board
The starting date of the crediting period (dd/mm/yyyy)	09/ 06/2011
The length of the crediting period	10years(fixed)

A.8. Name of responsible person(s)/entity(ies):

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The person(s)/entity(ies) responsible for completing CDM-MR

	Capro Corporation	**Hyosung Corporation**	**Hyosung Ebara Engineering Co., Ltd.**
Name	Kim, Heung-jae	Choi, Yung-yul	Park, Jong-hoon
Position	Deputy Senior Manager	Junior Associate	General Manager
E-mail	zkim@hcccapro.co.kr	memories37@hyosung.com	heec-jhpark@hyosung.com
Phone No.	+82-2-399-1243	+82-2-707-7586	+82-2-707-5841

SECTION B. Implementation of the project activity

B.1. Implementation status of the project activity

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1. **The starting date of operation of the project activity : 09/ 06/ 2011 (dd/mm/yyyy)**

2. **The Information of the actual operation in General**

2.1 Operating condition of AOR

In order to avoid that the operation of the caprolactam production plant is manipulated in a way to increase the N_2O generation, thereby increasing the CERs, the operating temperature and pressure of the ammonia oxidation reactor (AOR), and NH_3 input to the AOR, have been monitored every working day.

During the monitoring period #1, actual average daily AOR operation conditions are monitored as below Table B.1:

Table B.1 Summary of the AOR operation data

		$T_{g,a}$ (°C)	$T_{g,b}$ (°C)	P_{g-1} (Pa)	$A_{OR,d-1}$ (NH_3/d)
Plant I	Permit range in PDD	656.57~731.66	662.08~743.92	43,320~98,564	42.25
	Actual average in period 1	704.27	730.49	85,081	37.79
	The number of days outside permit range	none	none	none	none
Plant II		$T_{g,c}$ (°C)	$T_{g,d}$ (°C)	Pg_{-2} (Pa)	$A_{OR,d-2}$ (NH_3/d)
	Permit range in PDD	738.95~774.85	734.53~770.57	79,317~96,381	44.557
	Actual average in period 1	750.81	749.39	84,067	40.442
	The number of days outside permit range	none	none	1	none

For Plant I, all of daily average values of the AOR operation condition parameters have been kept within permit range. However, one of daily average value of operation pressure of AOR exceeded the upper limit of permit range on July 7, 2011.

2.2 Ammonia Oxidation Catalyst

The first composition of ammonia oxidation catalyst used during the crediting period shall be of the same kind of catalyst composition already in operation in the specific nitric acid or caprolactam production plant.

If the composition of ammonia oxidation catalysts is changed from the historical one ($G_{sup,hist}$ & $G_{com,hist}$) to the new one (G_{sup} & G_{com}), and the composition is not common practice in the region and not reported as being in use in the relevant literature. The project applicant shall demonstrate that the choice of the new composition was based on considerations other than an attempt to increase the rate of N_2O production, with appropriate and verifiable reasons (either by economic or other arguments). Otherwise, baseline emissions are limited to the maximum specific N_2O emissions of previous periods (tN_2O/t Caprolactam), documented in the verified monitoring reports.

Table B.2 The status of ammonia oxidation catalysts installed in AOR

		Plant I	Plant II
Historical supplier of AOR catalyst $G_{com,hist}$		Pt(90%): Rh(10%)	Pt(90%): Rh(10%)
Historical composition of AOR catalyst $G_{sup,hist}$		Johnson Matthey	Johnson Matthey
in period 1	The composition (G_{com})	Pt(90%): Rh(10%)	Pt(90%): Rh(10%)
	Supplier (G_{sup})	Johnson Matthey	Johnson Matthey

2.3 Plant output of Caprolactam

In the case of a nitric acid plant or a caprolactam plant using the Raschig process, baseline emissions are limited to the design capacity of the existing nitric acid or caprolactam production plant. If the actual production of caprolactam ($P_{\text{product},y}$) exceeds the design capacity ($P_{\text{product,max}}$) then emissions related to the production above $P_{\text{product,max}}$ will not be claimed for the baseline scenario. Therefore $P_{\text{product},y}$ is monitored.

However, it is not able to be decided whether the actual production of caprolactam exceeds $P_{\text{product,max}}$ or not, since those values should be compared on the annual values for comparing each other, and this period is first turn with the number of just 84 days.

Accumulated outputs by two of plants during the first period are described in below table. The actual average daily outputs and the average values converted from the design capacity ($P_{\text{product,max}}$) are also in that, in order to simply make rough estimation to the status of production.

Table B.3 the information of Caprolactam Production

		Plant I	Plant II
PDD	$P_{product,\ max}$	63307	64965
	Maximum operating day(day/yr)	363	355
	Average daily output(ton/day)	174.40	183
Period 1	Sub-total output for period	13363	15741
	No. of operating days(day/period)	84	84
	Average daily output(ton/day)	159.08	187

3. The Information on Special Event

3.1 Events of Plant I

Events information

Initial inspection to the N_2O Abatement System (NAS) of Plant I was carried out before project start until 10th of June (Project was started from 9th of June).

The solenoid valve on the N_2O gas inlet damper (XV-1521B) composing NAS was out of order, and this valve was replaced after by-pass valve was opened 23th of June. Control damper of NAS FD fan (PV-1522) was also repaired because it didn't work well on August, 4th, 2011.

Product facility of Plant I has been unstable for about 5hours on July 25, 2011.

Action of Recalculation

Among the data generated during the time of event caused by shut down or inspection of NAS in Plant I, the data of the volume flow rate and N_2O concentration at the inlet and out of the destruction facility (F_{TI-1}, F_{TE-1}, CI_{N2O-1} and CO_{N2O-1}) have been excluded from the emission reduction calculation. Natural gas input for re-heating the tail gas (Q_{NG-1}) and CH_4 concentration at destruction facility outlet (CO_{CH4-1}) are not excluded in order to be conservative, even though those parameters are related with NAS operating.

All data measured for the time of shut-down of the product facility were ignored, but the data of Q_{NG-1} and CO_{CH4-1} were considered for conservative calculation.

Table B.4 The information of event of Plant I, and the action for calculation

Event		Date			Action for calculation
		dd/mm/yyyy	Time(hourly)		
			from	to	
N_2O Abatement System	inspection	09/06/2011	1:00	24:00	Data from AMS to zero except LNG input and CH_4 concentration at destruction facility outlet during the relevant time of event.
		10/06/2011	1:00	18:00	
	Shut down	23/06/2011	10:00	11:00	
		04/08/2011	11:00	23:00	
Product Facility	Shut down	25/07/2011	16:00	20:00	All data to zero except LNG input, CH_4 concentration at destruction facility outlet during the relevant time of event.

3.2 Events of Plant II

Events information

Inspection to the N_2O Abatement System (NAS) of Plant II was also performed at the same two days with Plant I. (9th and 10th of June, 2011)

The increasing of the pressure of NAS in Plant II was detected with exceeding the normal operation condition range on 4th July, and so the NAS was shut down and fixed with replacing the EMV of RCS (2R-1521) to new one until 5th of July.

Product facility of Plant II has been unstable for about 5hours, August 19th, 2011.

Action of Recalculation

Among the data generated during the time of event caused by shut down or inspection of NAS in Plant II, the data of the volume flow rate and N_2O concentration at the inlet and out of the destruction facility (F_{TI-2}, F_{TE-2}, CI_{N2O-2} and CO_{N2O-2}) have been excluded from the emission reduction calculation. Natural gas input for re-heating the tail gas (Q_{NG-2}) and CH_4 concentration at destruction facility outlet (CO_{CH4-2}) are not excluded in order to be conservative, even though those parameters are related with NAS operating.

All data measured for the time of shut-down of the product facility were ignored, but the data of Q_{NG-2} and CO_{CH4-2} were considered for conservative calculation.

Table B.5 The information of event of Plant II, and the action for calculation

<table>
<tr><th colspan="2" rowspan="3">Event</th><th colspan="3">Date</th><th rowspan="3">Action for calculation</th></tr>
<tr><th rowspan="2">dd/mm/yyyy</th><th colspan="2">Time(hourly)</th></tr>
<tr><th>from</th><th>to</th></tr>
<tr><td rowspan="4">N_2O Abatement System</td><td rowspan="2">inspection</td><td>09/06/2011</td><td>1:00</td><td>24:00</td><td rowspan="4">Data from AMS to zero except LNG input and CH_4 concentration at destruction facility outlet during the relevant time of event.</td></tr>
<tr><td>10/06/2011</td><td>1:00</td><td>19:00</td></tr>
<tr><td rowspan="2">Shut down</td><td>04/07/2011</td><td>9:00</td><td>24:00</td></tr>
<tr><td>05/07/2011</td><td>1:00</td><td>22:00</td></tr>
<tr><td>Product Facility</td><td>Shut down</td><td>19/08/2011</td><td>19:00</td><td>24:00</td><td>All data to zero except LNG input and CH_4 concentration at destruction facility outlet during the relevant time of event.</td></tr>
</table>

B.2. Revision of the monitoring plan

>>
None

B.3. Request for deviation applied to this monitoring period

>>
None

B.4. Notification or request of approval of changes

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None

SECTION C. Description of the monitoring system

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1. Monitoring points to be measured

1.1 Monitoring Points in Plant I

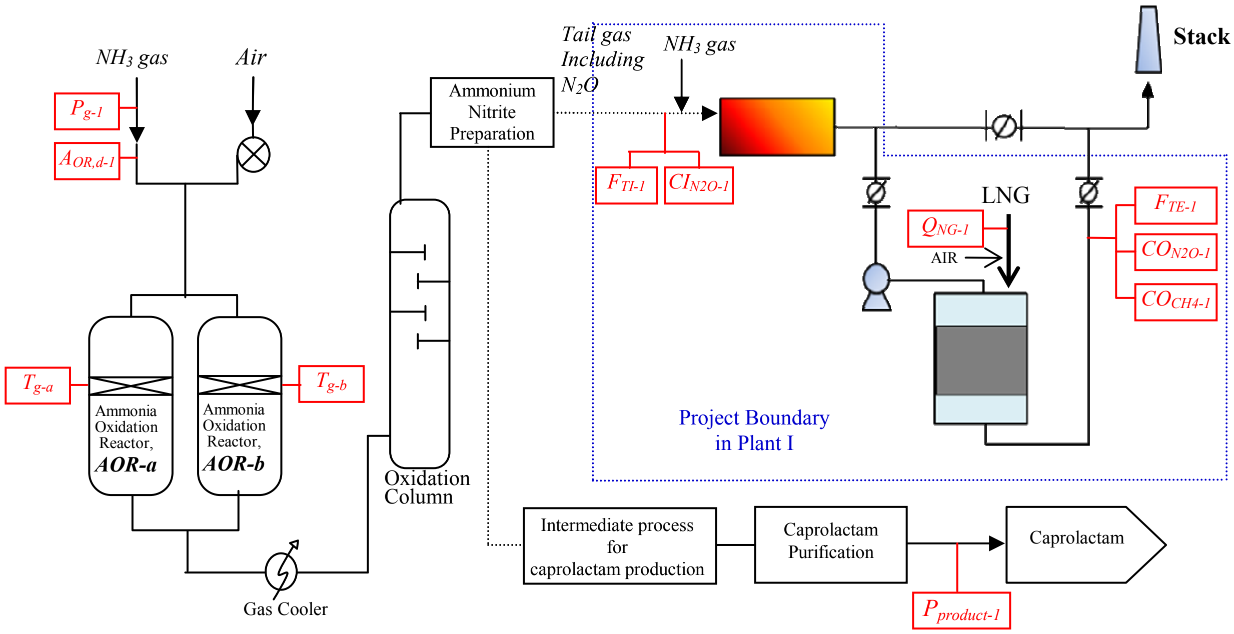

Figure C.1 Monitoring Points in Plant I

Parameter	Description	Tag No.
$A_{OR,d\text{-}1}$	Actual ammonia flow rate to AOR in Plant I	FIC-1201
$P_{g\text{-}1}$	Actual operating pressure of the AOR-a, b in Plant I	PI-1205
$T_{g\text{-}a}$	Actual operating temperature of the AOR-a in Plant I	TI-1204
$T_{g\text{-}b}$	Actual operating temperature of the AOR-b in Plant I	TI-1206
$F_{TI\text{-}1}$	Volume flow rate at the inlet of the destruction facility in Plant 1	FI-1521
$F_{TE\text{-}1}$	Volume flow rate at the exit of the destruction facility in Plant 1	FI-1522
$CI_{N2O\text{-}1}$	N_2O concentration at destruction facility inlet in Plant I	AI-1521
$CO_{N2O\text{-}1}$	N_2O concentration at destruction facility outlet in Plant I	AI-1522(a)
$Q_{NG\text{-}1}$	Additional natural gas input for re-heating the tail gas in Plant I	FI-1523
$CO_{CH4\text{-}1}$	CH_4 concentration at destruction facility outlet in Plant I	AI-1522(b)
$P_{product\text{-}1}$	Plant output of caprolactam in Plant I	FR-7705

Some tag numbers of measuring devices were change to avoid confusion, because the same tag number had been allocated by to two kind of different measuring devices described in PDD. Therefore new tag numbers were given to be clearly identified as follows:

	Parameters	Tag No.in PDD	Actual Tag No. in Period#1
Plant I	$CO_{N2O\text{-}1}$	AI-1522	AI-1522(a)
	$CO_{CH4\text{-}1}$	AI-1522	AI-1522(b)

1.2 Monitoring Points in Plant II

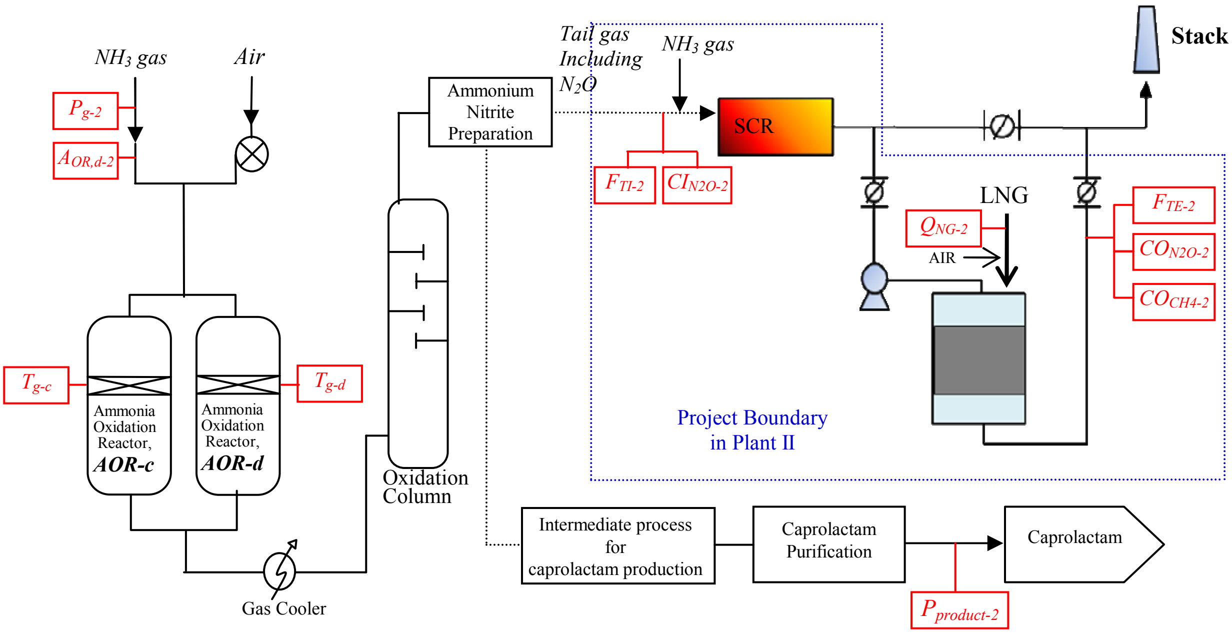

Figure C.2 Monitoring Points in Plant II

Parameter	Description	Tag No.
$A_{OR,d-2}$	Actual ammonia flow rate to AOR in Plant II	2FIC-1201
P_{g-2}	Actual operating pressure of the AOR-c, d in Plant II	2PI-1205
T_{g-c}	Actual operating temperature of the AOR-c in Plant II	2TI-1204
T_{g-d}	Actual operating temperature of the AOR-d in Plant II	2TI-1206
F_{TI-2}	Volume flow rate at the inlet of the destruction facility in Plant II	2FI-1521
F_{TE-2}	Volume flow rate at the exit of the destruction facility in Plant II	2FI-1522
CI_{N2O-2}	N_2O concentration at destruction facility inlet in Plant II	2AI-1521
CO_{N2O-2}	N_2O concentration at destruction facility outlet in Plant II	2AI-1522(a)
Q_{NG-2}	Additional natural gas input for re-heating the tail gas in Plant II	2FI-1523
CO_{CH4-2}	CH_4 concentration at destruction facility outlet in Plant II	2AI-1522(b)
$P_{product-2}$	Plant output of caprolactam in Plant II	2FI-7705

Some tag numbers of measuring devices were change to avoid confusion, because the same tag number had been allocated by to two kind of different measuring devices described in PDD. Therefore new tag numbers were given to be clearly identified as follows:

	Parameters	Tag No.in PDD	Actual Tag No. in Period#1
Plant II	CO_{N2O-2}	2AI-1522	2AI-1522(a)
	CO_{CH4-2}	2AI-1522	2AI-1522(b)

2. Data Collection Procedure

The data of the AOR operating parameters (A_{OR}, T_g, P_g) and the productivity of caprolactam are logged and stored by the existed DCS (Distributed Control System) which has been independently operated for Plant I and II before starting this project.

Besides, DAS (Data Acquisition System) is newly installed to log the relevant data to the N_2O decomposition amount and CH_4 emission by operating N_2O abatement system. DAS consists of an ‘Electronic Evaluation Unit (EEU)’ and two of ‘Data Communication Units (DCUs)’ located at Plant I and II.
Major function of DCU is to record the raw measurement data from Automated Measuring System(AMS), and to transmit those to EEU. DCU can store temporarily the record of raw measurement data with the ring memory of 16days minute values. In addition, the data of AOR operation and caprolactam productivity are delivered from DCS and recorded by DCU respectably, and then transmitted to EEU. Therefore it is aggregated, recorded and stored by EEU that not only the AMS data but also the AOR data and productivity data. However, if there is a discrepancy between the DCS data and the EEU and/or DCU data, DCS data should be taken.
EEU satisfies the requirements described in AM0028 / Version 05 as below:

(a) Evaluation unit needs to take into account registration, mean average determination, validation, and evaluation;
(b) The system and concept of emission data processing needs to be described;
(c) Protocols and out-prints are required.

With EEU, these raw measurement data transmitted from DCUs are integrated after the measurement uncertainty determined by QAL 2 test is subtracted from them. Then, those are converted to the average values at the end of the every integration interval (1 hour), and validated. Negatively validated average values are set to zero. Validated average values outside the valid calibration range are to be stored with the associated time and with their status and are to be logged on EEU at the end of the day and year. EEU has the storage capacity of 5year-ring memory.
The calibration curve for the measuring instrument is determined using a standard reference method. The validity of the calibration curve is proved by EEU. The validity range for the calibration is specified in the calibration report. This calibration reports are printed and kept for back-up.
External hard disk drive (HDD) is installed for back-up and long storage of the data and relevant reports for verification, replaced by new one every 4 years, old HDDs are kept holding with attention during the 10years of crediting period and 2 additional years according to AM0028 / Version 05.

Table C.1 The information of the data collection and storage devices except DCS

		Supplier	Model No.	Serial No.
DCU(Data Communication Unit)	Plant 1	DURAG	D-EMS 500 KE	1301581
	Plant 2	DURAG	D-EMS 500 KE	1301582
EEU (Electronic Evaluation Unit)		DURAG	D-EMS 2000 SWE	1301567
External Hard disk drive(HDD) for backup		DURAG	D-EMS 2000 RED	1301578

The role of the new PC is to display and record the hourly data from EEU, the monthly data of supplied LNG, and the other information including the events list, working diary and so on which could be influence on the verification.

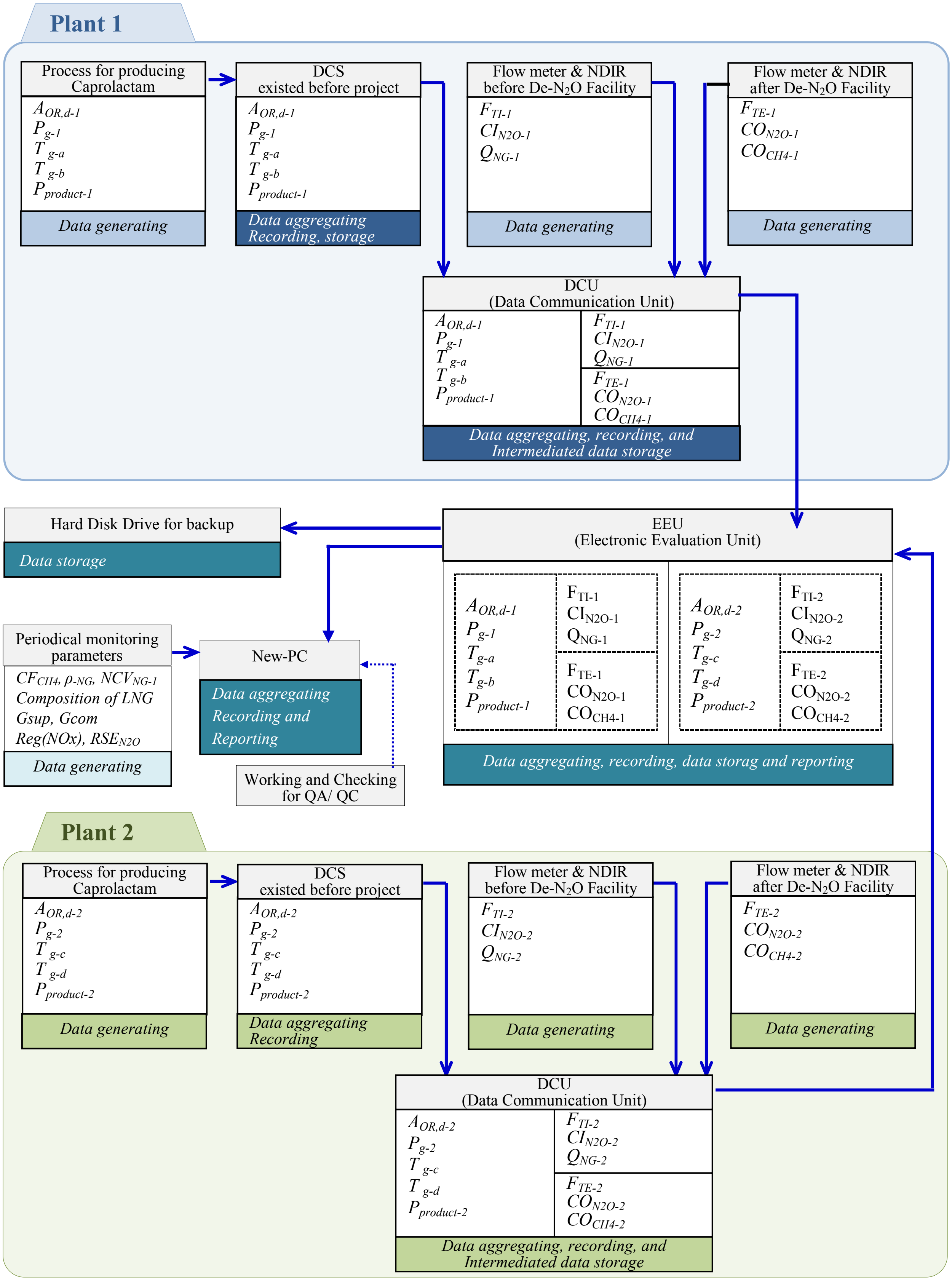

Figure C.3 Data Collecting Flow

3. Organization Structure, roles and responsibilities of personnel

3.1 Organization Structure

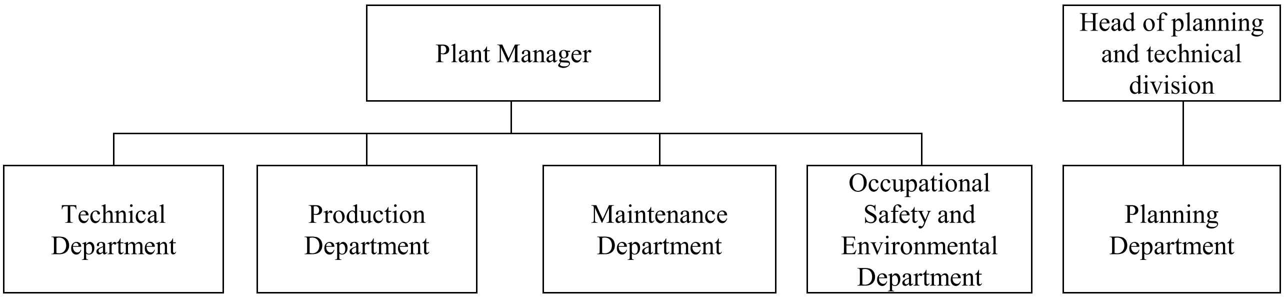

Figure C.4 The scheme of the operational and management structure

3.2 Roles and responsibilities of personnel

• Plant Manager

The Plant Manager takes overall responsibility for the operation and maintenance of the N_2O monitoring system. In addition, the Plant Manager has authority to approve monitoring report provided by the Technical Department.

• Production Department

The responsible Production Engineers in Production Department are in charge of the operation and supervision of N_2O monitoring system that will be implemented to record plant operation data.

• Technical Department

Monitoring engineers in Technical Department are responsible for collecting, validating and processing the data to determine GHG emission reduction and making report periodically. Moreover, the monitoring engineer is in charge of archiving the data as well. The monitoring engineers archive all required data and reports for verification.

• Maintenance Department

Maintenance Department is responsible for maintaining and repairing the instrument associated with this project. Calibration for instruments is concerned by maintenance department as well.

• Occupational Safety and Environment Department

The OSHES Department plays a role for indicating the direction and managing according to the monitoring plan.

• Planning Department

Planning Department conducts the internal audit of N_2O monitoring system periodically.

4. Emergency Procedures for the Monitoring system

In case of the data deviation, following procedures are taken.
- (a) Production Engineer in Production Department identifies whether the deviation results from processing or other factors such as temperature and pressures.
- (b) Production engineer compares the deviated data with other parameter data if the deviation results from processing.
- (c) If the reason for the data deviation is not identified, production engineer informs Maintenance Department to correct the error after inspecting all gauges and analysers.

If the data deviation is not covered by procedures above, Technical Department makes the decision to correct figures or to abandon the data. In addition, any data correction is in compliance with the applied methodology and done in a conservative bias

When the malfunction of measuring instruments is occurred, following procedures are taken.
- (a) If production engineer recognizes the malfunction of measuring instruments, he informs person in Maintenance Department of this abnormal situation.
- (b) Maintenance Department estimates whether performing repairing action to solve problem is appropriate or not.
- (c) If it is decided that self-repairing by Maintenance Department is appropriate, self-repairing is carried out. However, if the instrument is out of repair, Maintenance Department requests external institution specialized in repairing to have it serviced.

If measuring devices have to be replaced, related supporting evidences should be checked and kept by Maintenance Department, in order to demonstrate that the quality of the replaced measuring devices is the same as the quality grade of existed devices, before the copies of the supporting evidences to replaced devices should be delivered to and kept in the Technical Department.

Specially, if any malfunction situation of the measuring devices composing AMS(Automated measuring system) is continued during the 8hrs after it is detected, Maintenance Department should request the service of official measuring agency to measuring the N_2O concentration or flow rate at the monitoring points of inlet and outlet of N_2O decomposition system. If the services by the official measuring agency cannot be taken for some unavoidable reason, it will be taken instead of measuring by the external official measuring agency that the AMS data measured at the most similar operating condition among those of the recent 1 month just before the abnormal situation is happen, with the conservative understanding of that the N_2O concentration of inlet is replaced with the lowest number, and that of outlet is with highest one.

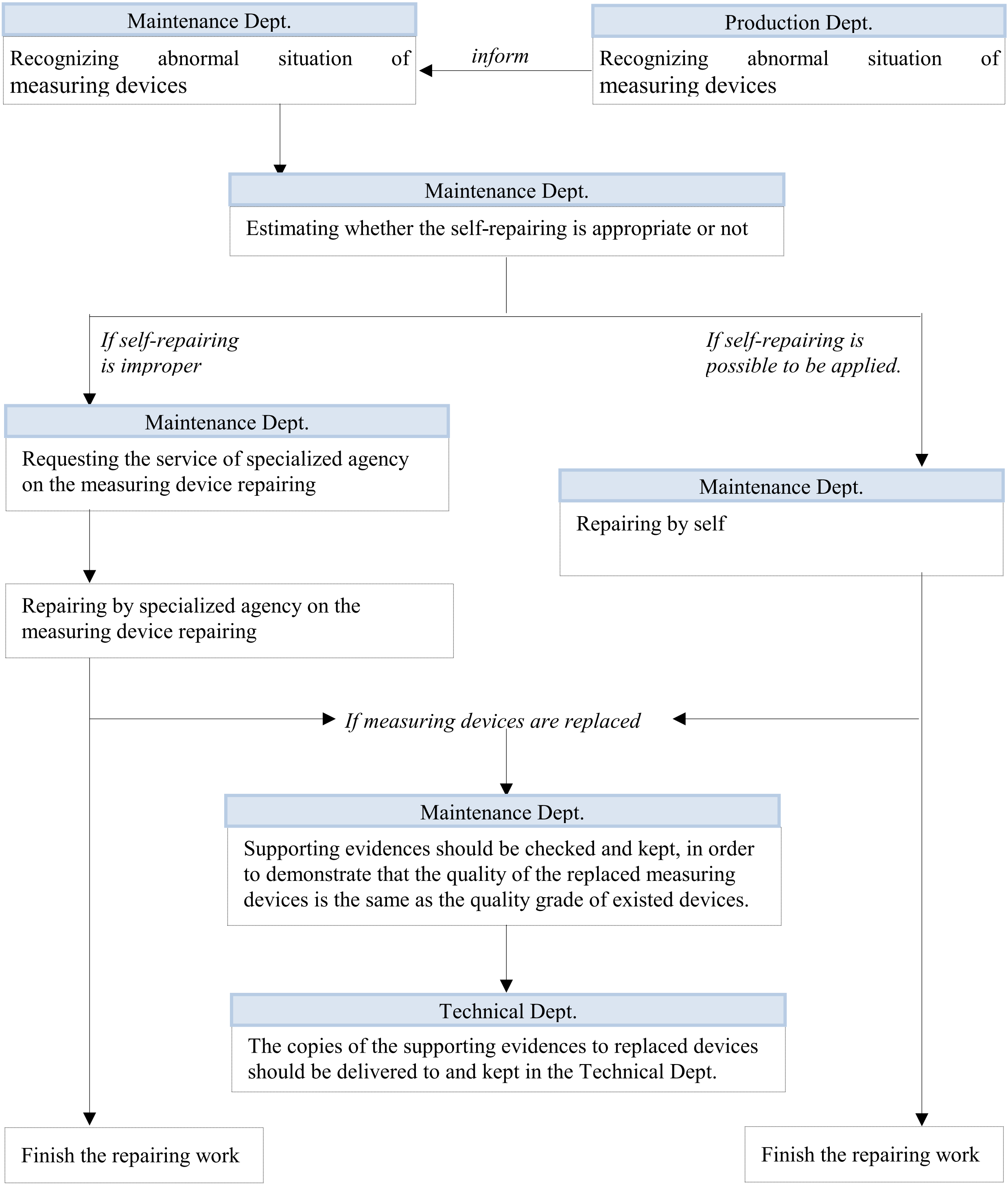

Figure C.5 Emergency Procedures for malfunctions of measuring devices in general

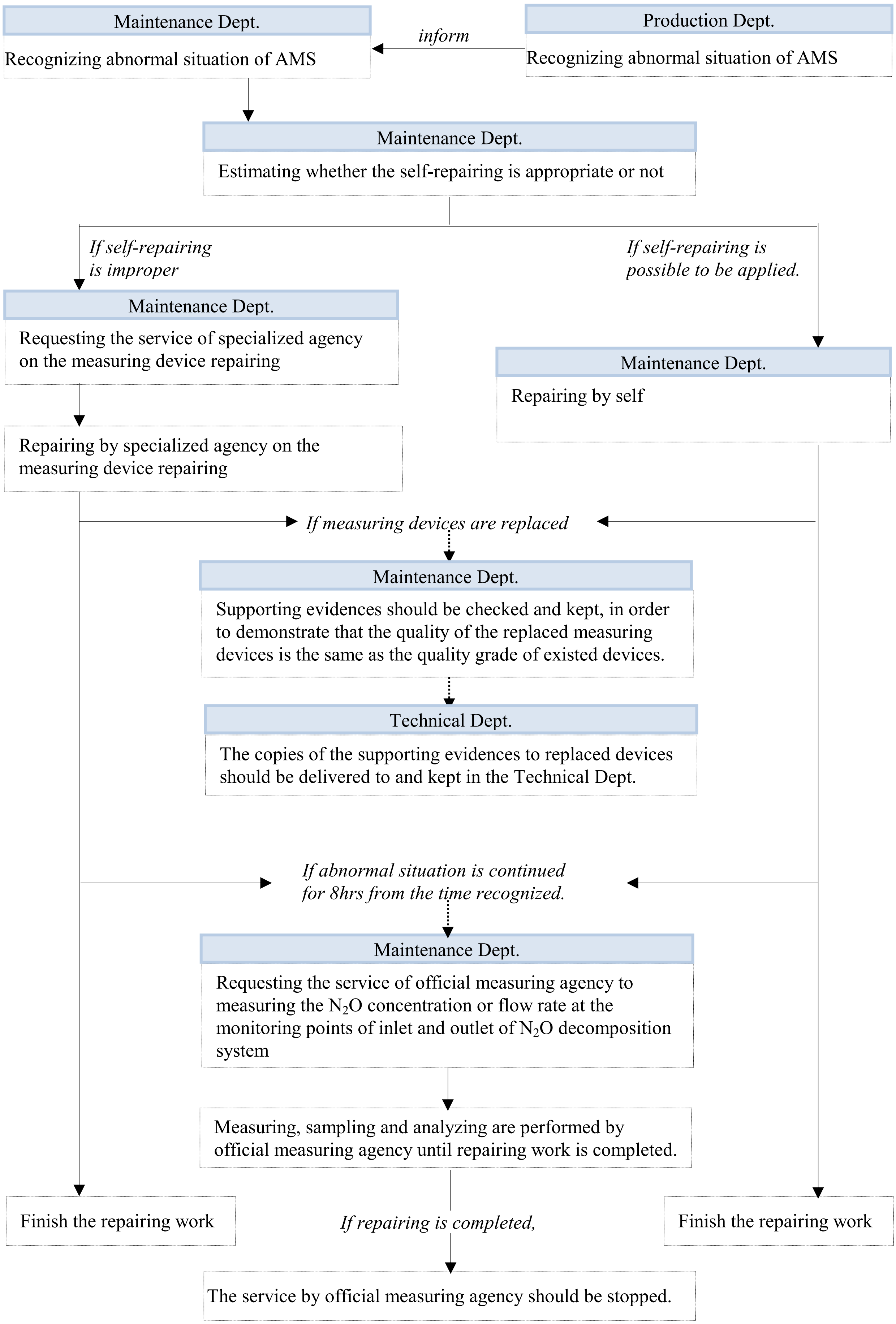

Figure C.6 Emergency Procedures for malfunction of AMS

5. **Reporting**

- **Daily report** consists of the parts printed out from EEU and from New-PC. EEU report is to show the data generated by AMS and related to the AOR operation condition and to the productivity of caprolactam. Daily value of each parameter is calculated based on hourly average or hourly total value on the EEU report. The situation of the AMS failure is also documented on the EEU report. The other hand, new-PC daily report is about checking and maintaining the measuring device and N_2O abatement system, and about monitoring events.

- **Monthly report** integrates the data and information in daily reports. LNG information is also reported monthly. Periodical monitoring parameters such as the composition and supplier of AOR catalysts, the national regulation on NOx and N_2O are checked by monthly report too.

- **Annual report** is a bunch of monthly report files. However there is no annual report, because the this period is first and the length of the periods is just 84 days.

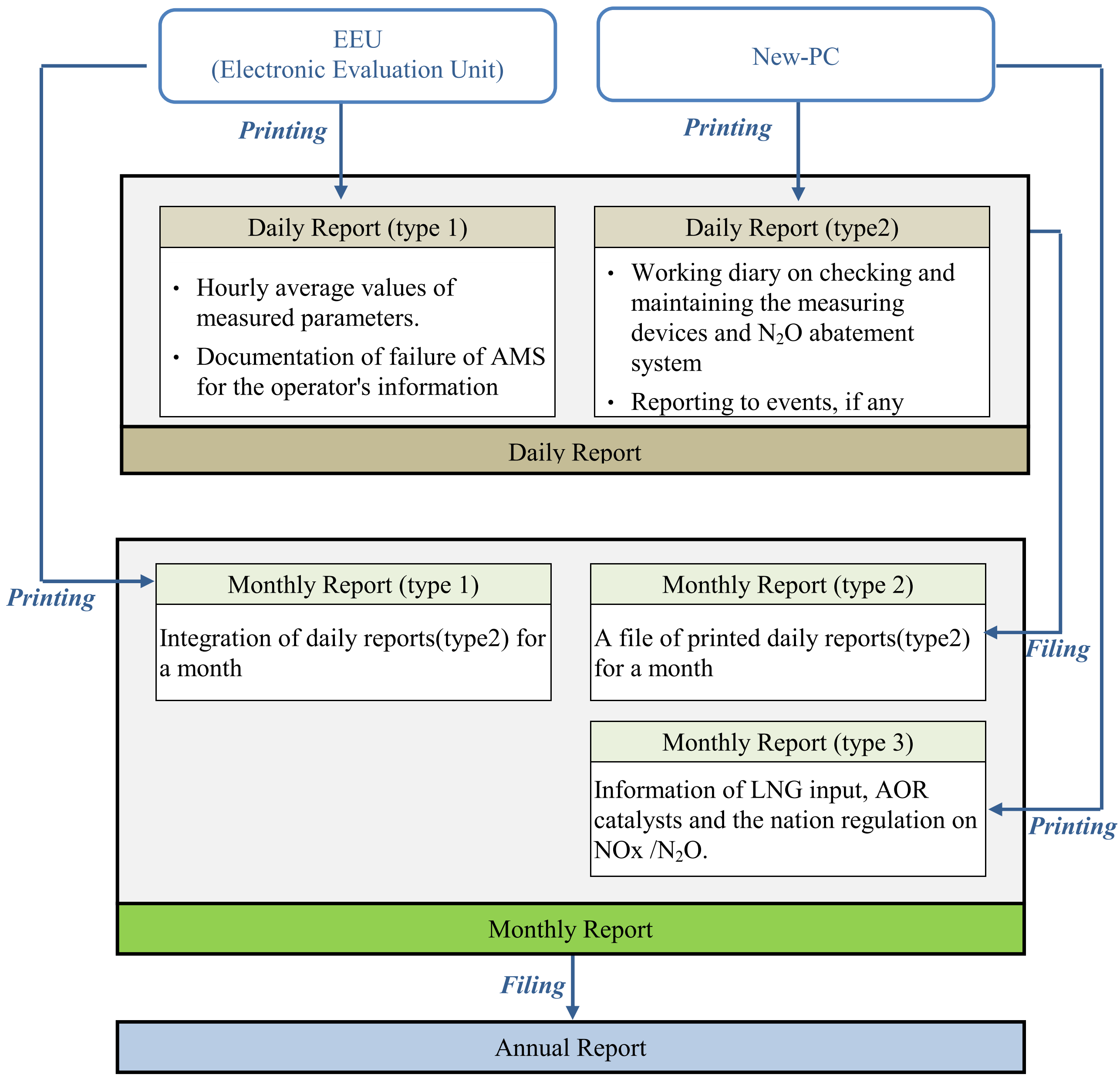

Figure C.7 The consists of the periodical reports

6. Quality Assurance of AMS(Automated measuring system)

AMS(Automated measuring system) has been applied to measure the amount of N_2O emission at the two monitoring points of the inlet and outlet of N_2O destruction facility of each plant involved in this project. By AMS, the concentration of N_2O and the volume flow rate of tail gas are measured simultaneously(F_{Ti}, CI_{N2O}, and F_{TE}, CO_{N2O}) at same basis (wet or dry), and these values are expressed on the same basis (wet or dry) with correcting to normal conditions (101.324kPa, 0deg C) through the algorithm based on procedures of EN14181.

"European Norm EN14181: Quality assurance of automated measuring systems, 2004" is selected as a guidance document to the Quality Assurance and Control procedure of the AMS for this project. This means that the three levels of quality assurance tests(QAL1, QAL2 and QAL3) and one annual functional test must be carried out regarding the selection, installation, and operation of AMS under the monitoring methodology in AM0028(ver.05).

Quality assurance of tested AMS (:QAL1)

The quality assurance of tested AMS was accomplished with that the flow meters and N_2O gas analyzers having the performance certificate with calculation uncertainty were selected as summarized in following tables.

Quality assurance of installation and calibration of AMS (:QAL2)

QAL 2 has been performed two times according to the Standard Reference Measurement Method (23/05/2011~27/05/2011 and 26/09/2011~29/09/2011) by AIR-TEC, which is the one of the organizations having an accredited quality assurance system on ISO/IEC 17025.

The result to the test for QAL2 was summarized on the QAL 2 report in the major items following:

(a) Section of the location of measurement
(b) Duly installation of the monitoring equipment
(c) Correct choice of measurement range
(d) Calibration of AMS using the standard-Reference-Method(SRM) as guidance
(e) Calibration curve either as linear regression or as straight line from absolute zero to centre of a scatter-plot
(f) Calibration of the standard deviation at the 95% confidence interval

Continuous quality Assurance through the local operator/manager (:QAL3)

QAL 3 has been implemented since the project start up. This includes:

- Permanent quality assurance during the plant operation by the operating staff
- Assurance of reliable and correct operation of the monitoring equipment
- Regular controls : zero point, span, drift, meet schedule of manufacturer maintenance intervals

Annual Surveillance test (AST)

Annual functionality test has not been carried out yet, because only 84 days have passed since the crediting period was started.

Table C.2 (a) Information of the quality assurance of tested AMS in Plant I

Location	Parameters	Type	model	serial number	Standard for Performance certification	Certificate No.	The date of Certificate Issued (dd/mm/yyyy)	Approved methods to caculate of uncertainty
Inlet	FTI_{-1}	Ultrasonic flowmeter	D-FL 200 Flow Monitor	HEAD A: 1217007 HEAD B: 1217008 EVALUATION UNIT : 1216861 CASE OF EVALUATION : 1216999	MCERTS	Sira MC 060072/01	22/05/2007	
	CI_{N2O-1}	NDIR	ULTRAMAT 6	AO-748	TUV	BB-EG1-KAR Gr02X	29/07/2003	EN 50016 EN 60079-14 Guidelines for expolosion protection of GB Chemie(GRG 104)
					FM Approvals	3016050	15/07/2003	
					CSA INTERNATIONAL	1431560	17/04/2003	
Outlet	FTE_{-1}	Ultrasonic flowmeter	D-FL 200 Flow Monitor	HEAD A: 1217009 HEAD B: 1217010 EVALUATION UNIT : 1216862 CASE OF EVALUATION : 1217001	MCERTS	Sira MC 060072/01	22/05/2007	
	CO_{N2O-1}	NDIR	ULTRAMAT 6	AO-750	TUV	BB-EG1-KAR Gr02X	29/09/2003	EN 50016 EN 60079-14 Guidelines for expolosion protection of GB Chemie(GRG 104)
					FM Approvals	3016050	15/07/2003	
					CSA INTERNATIONAL	1431560	17/04/2003	

Table C.2 (b) Information of the quality assurance of tested AMS in Plant II

Location	Parameters	Type	model	serial number	Standard for Performance certification	Certificate No.	The date of Certificate Issued (dd/mm/yyyy)	Approved methods to caculate of uncertainty
Inlet	FTI_{-2}	Ultrasonic flowmeter	D-FL 200 Flow Monitor	HEAD A: 1217011 HEAD B: 1217012 EVALUATION UNIT : 1216866 CASE OF EVALUATION : 1217002	MCERTS	Sira MC 060072/01	22/05/2007	
	CI_{N2O-2}	NDIR	ULTRAMAT 6	AO-749	TUV	BB-EG1-KAR Gr02X	29/09/2003	EN 50016 EN 60079-14 Guidelines for expolosion protection of GB Chemie(GRG 104)
					FM Approvals	3016050	15/07/2003	
					CSA INTERNATIONAL	1431560	17/04/2003	
Outlet	FTE_{-2}	Ultrasonic flowmeter	D-FL 200 Flow Monitor	HEAD A: 1217013 HEAD B: 1217014 EVALUATION UNIT : 1216867 CASE OF EVALUATION : 1217003	MCERTS	Sira MC 060072/01	22/05/2007	
	CO_{N2O-2}	NDIR	ULTRAMAT 6	AO-751	TUV	BB-EG1-KAR Gr02X	29/09/2003	EN 50016 EN 60079-14 Guidelines for expolosion protection of GB Chemie(GRG 104)
					FM Approvals	3016050	15/07/2003	
					CSA INTERNATIONAL	1431560	17/04/2003	

7. Conservative calculation on tail gas flow

Measurement value by a flow meter at inlet of destruction facility (F_{TI}) and Measurement value by a flow meter at outlet of destruction facility (F_{TE}), both parameters shall be cross checked to ensure that no leak of N_2O is taking place, and in case of discrepancy, conservative calculation of emission reduction is provided. In order to achieve conservative approach, the measured inlet flow (F_{TI}) would be adjusted to the value (F_{TI}*) by the below equation.

$$F_{TI}^{*} = \min\left[F_{TI} ; \left(\frac{F_{TE}}{1+VEF} - Q_{NG} \times \frac{Q_{NG\ combustion\ gas}}{Q_{NG}} \right)\right]$$

Where:

F_{TI}^{*}	: Conservative volume flow at the inlet of destruction facility used for emission reduction calculation (Nm^3/h)
F_{TI}	: Measurement value by a flow meter at inlet of destruction facility (Nm^3/h)
F_{TE}	: Measurement value by a flow meter at outlet of destruction facility (Nm^3/h)
Q_{NG}	: Natural gas input for re-heating the tail gas (Nm^3/h)
$Q_{NG\ combustion\ gas}$	: Combustion gas of natural gas (Nm^3/h)
VEF	: Volumetric Expansion Factor

For monitoring, the gas generated by combusting natural gas($Q_{NG\ combustion\ gas}$) has been estimated on the supposition that air input according to the theoretical oxygen demand on the natural gas composition which information is provided by the natural gas supplier for Capro (Kyung Dong city gas CO., Ltd).

And for the conservative approach, any volume change from De-NOx and/or De-N_2O system will be considered by the Volumetric Expansion Factor (VEF). Before the first monitoring period, the Volumetric Expansion Factor (VEF) was determined as 0.003 which was provided by CRI, N_2O abatement catalysts supplier. This value of VEF is applied as a fixed official value.

8. Training

The supplier of the NDIR system provided complete training to the monitoring engineers in charge of operation and maintenance of the monitoring system. The provider of the De-N_2O system, (Hyosung Ebara Engineering Co., Ltd.) initiated the operation technique for the system to the staff in the Technical department of Capro.

SECTION D. Data and parameters

D.1. Data and parameters determined at registration and not monitored during the monitoring period, including default values and factors	
Data / Parameter:	GWP_{N2O}
Data unit:	Not applicable
Description:	Global warming potential of the nitrous oxide
Source of data used:	IPCC, The Second Assessment Report
Value(s) :	310
Indicate what the data are used for (Baseline/ Project/ Leakage emission calculations)	Baseline Emission / Project Emission
Additional comment:	Not applicable

Data / Parameter:	GWP_{CH4}
Data unit:	Not applicable
Description:	Global warming potential of the methane
Source of data used:	IPCC, The Second Assessment Report
Value(s) :	21
Indicate what the data are used for (Baseline/ Project/ Leakage emission calculations)	Project Emission Calculation
Additional comment:	Not applicable

Data / Parameter:	$P_{product, max}$
Data unit:	t Caprolactam /yr
Description:	Design capacity of caprolactam production of the targeted line
Source of data used:	PDD
Value(s) :	$P_{product1, max}$: 63,307 ton/yr (design capacity in Plant I) $P_{product2, max}$: 64,965 ton/yr (design capacity in Plant II) Each plant has an individual design capacity.
Indicate what the data are used for (Baseline/ Project/ Leakage emission calculations)	Baseline Emission Calculation
Additional comment:	Not applicable

Data / Parameter:	$A_{OR,hist}$
Data unit:	tNH_3/day
Description:	Maximum of historical ammonia flow rate of the ammonia oxidation reactor (AOR)
Source of data used:	PDD
Value(s) :	$A_{OR,hist-1}$: 42.250tNH_3/d (total flow rate for AOR-a and AOR-b in Plant I) $A_{OR,hist-2}$: 44.557tNH_3/d (total flow rate for AOR-c and AOR-d in Plant II)
Indicate what the data are used for (Baseline/ Project/ Leakage emission calculations)	Baseline Emission Calculation

Additional comment:	Not applicable
Data / Parameter:	***$T_{g,hist}$***
Data unit:	^oC
Description:	Historical operating temperature range of the ammonia oxidation reactor
Source of data used:	PDD
Value(s) :	$T_{g,hist-a}$: 656.57− 731.66°C (for AOR-a in Plant I) $T_{g,hist-b}$: 662.08−743.92 °C (for AOR-b in Plant I) $T_{g,hist-c}$: 738.95− 774.85°C (for AOR-c in Plant II) $T_{g,hist-d}$: 734.53− 770.57°C (for AOR-d in Plant II)
Indicate what the data are used for (Baseline/ Project/ Leakage emission calculations)	Baseline Emission Calculation
Additional comment:	Not applicable

Data / Parameter:	***$P_{g,hist}$***
Data unit:	*Pa gauge*
Description:	Historical operating pressure range of the ammonia oxidation reactor
Source of data used:	PDD
Value(s) :	$P_{g,hist\_1}$: 43,320− 98,564 Pa gauge (for AOR-a and AOR-b in Plant I) $P_{g,hist\_2}$: 79,317− 96,381 Pa gauge (for AOR-c and AOR-d in Plant II)
Indicate what the data are used for (Baseline/ Project/ Leakage emission calculations)	Baseline Emission Calculation
Additional comment:	Not applicable

Data / Parameter:	***$G_{sup,hist}$***
Data unit:	-
Description:	Historical supplier of the ammonia oxidation catalyst
Source of data used:	PDD
Value(s) :	Name of the supplier: Johnson Matthey
Indicate what the data are used for (Baseline/ Project/ Leakage emission calculations)	Baseline Emission Calculation
Additional comment:	Not applicable

Data / Parameter:	***$G_{com,hist}$***
Data unit:	%
Description:	Historical composition of the ammonia oxidation catalyst
Source of data used:	PDD
Value(s) :	Pt (90%): Rh (10%)
Indicate what the data are used for (Baseline/ Project/ Leakage emission calculations)	Baseline Emission Calculation
Additional comment:	Not applicable

Data / Parameter:	***$OXID_{HC}$***
Data unit:	%
Description:	Oxidation factor of natural gas, with two or more molecules of carbon
Source of data used:	PDD
Value(s) :	100%

Indicate what the data are used for (Baseline/ Project/ Leakage emission calculations)	Project Emission Calculation
Additional comment:	Not applicable

Data / Parameter:	EF_{CH4}
Data unit:	tCO_2/tCH_4
Description:	Emission factor of methane
Source of data used:	PDD
Value(s) :	2.75(tCO_2/tCH_4)
Indicate what the data are used for (Baseline/ Project/ Leakage emission calculations)	Project Emission Calculation
Additional comment:	Not applicable

Data / Parameter:	ρ_{CH4}
Data unit:	t/m^3
Description:	Density of methane
Source of data used:	Tool to determine project emissions from flaring gases containing methane
Value(s) :	0.000716 t/m^3
Indicate what the data are used for (Baseline/ Project/ Leakage emission calculations)	Project Emission Calculation
Additional comment:	Not applicable

Data / Parameter:	M_i
Data unit:	hour
Description:	Length of measuring interval
Source of data used:	AMS
Value(s) :	1 hour (to be measured continuously for 24 hours)
Indicate what the data are used for (Baseline/ Project/ Leakage emission calculations)	Baseline Emission Calculation / Project Emission Calculation
Additional comment:	Not applicable

Data / Parameter:	Reg_{NOx}
Data unit:	$tNOx/Nm^3$
Description:	National regulation on NOx emissions
Source of data used:	The "Clean Air Conservation Act", one of the National environmental legislation, Ministry of Environment
Value(s) :	4.10714×10^{-7} $tNOx/Nm^3$ (as a NO_2 concentration)
Indicate what the data are used for (Baseline/ Project/ Leakage emission calculations)	Not applicable
Additional comment:	Not applicable

D.2. Data and parameters monitored	
Data / Parameter:	$F_{TI,i}$
Data unit:	Nm^3/hr
Description:	Volume flow rate at the exit of the destruction facility
Measured /Calculated /Default:	Measured
Source of data:	Flow meter with normalizing functions
Value(s) of monitored parameter:	For this period, the average values of F_{TI} | | Plant I | Plant II | | F_{TI} as Nm^3/hr in average | 40,702 | 38,487 |
Indicate what the data are used for (Baseline/ Project/ Leakage emission calculations)	Baseline Emission Calculation
Monitoring equipment (type, accuracy class, serial number, calibration frequency, date of last calibration, validity)	Refer to **Table C.2** of this monitoring report
Measuring/ Reading/ Recording frequency:	•Measuring period : Continuously •Reading frequency : hourly •Recording frequency : Daily
Calculation method (if applicable):	Not applicable
QA/QC procedures applied:	QAL 1, 2,3 and AST for AMS

Data / Parameter:	$F_{TE,i}$
Data unit:	Nm^3/hr
Description:	Volume flow rate at the exit of the destruction facility
Measured /Calculated /Default:	Measured
Source of data:	Flow meter with normalizing functions
Value(s) of monitored parameter:	For this period, the average values of F_{TE} | | Plant I | Plant II | | F_{TE} as Nm^3/hr in average | 45150 | 47074 |
Indicate what the data are used for (Baseline/ Project/ Leakage emission calculations)	Project Emission Calculation
Monitoring equipment (type, accuracy class, serial number, calibration frequency, date of last calibration, validity)	Refer to **Table C.2** of this monitoring report
Measuring/ Reading/ Recording frequency:	•Measuring period : Continuously •Reading frequency : hourly •Recording frequency : Daily
Calculation method (if applicable):	Not applicable
QA/QC procedures applied:	QAL 1, 2,3 and AST for AMS

Data / Parameter:	***$CI_{N2O,i}$***
Data unit:	tN_2O/Nm^3
Description:	N_2O concentration at destruction facility inlet
Measured /Calculated /Default:	Measured
Source of data:	Non-dispersion infrared absorption analyzer (NDIR)
Value(s) of monitored parameter:	<table><tr><td></td><td>Plant I</td><td>Plant II</td></tr><tr><td>$CI_{N2O,i}$ as tN_2O/Nm^3</td><td>3.923E-06</td><td>3.098E-06</td></tr></table>
Indicate what the data are used for (Baseline/ Project/ Leakage emission calculations)	Baseline Emission Calculation
Monitoring equipment (type, accuracy class, serial number, calibration frequency, date of last calibration, validity)	Refer to **Table C.2** of this monitoring report
Measuring/ Reading/ Recording frequency:	•Measuring period : Continuously •Reading frequency : hourly •Recording frequency : Daily
Calculation method (if applicable):	Not applicable
QA/QC procedures applied:	QAL 1, 2,3 and AST for AMS

Data / Parameter:	***$CO_{N2O,i}$***
Data unit:	tN_2O/Nm^3
Description:	N_2O concentration at destruction facility outlet
Measured /Calculated /Default:	Measured
Source of data:	Non-dispersion infrared absorption analyzer (NDIR)
Value(s) of monitored parameter:	<table><tr><td></td><td>Plant I</td><td>Plant II</td></tr><tr><td>$CO_{N2O,i}$ as tN_2O/Nm^3</td><td>3.811E-07</td><td>2.762E-07</td></tr></table>
Indicate what the data are used for (Baseline/ Project/ Leakage emission calculations)	Project Emission Calculation
Monitoring equipment (type, accuracy class, serial number, calibration frequency, date of last calibration, validity)	Refer to **Table C.2** of this monitoring report
Measuring/ Reading/ Recording frequency:	•Measuring period : Continuously •Reading frequency : hourly •Recording frequency : Daily
Calculation method (if applicable):	Not applicable
QA/QC procedures applied:	QAL 1, 2,3 and AST for AMS

Data / Parameter:	$P_{product,y}$
Data unit:	t Caprolactam/yr
Description:	Plant output of caprolactam
Measured /Calculated /Default:	Measured
Source of data:	the value measured by Mass flow meter
Value(s) of monitored parameter:	For, this period <table><tr><td></td><td>Plant I</td><td>Plant II</td></tr><tr><td>$P_{product,}$ period, (ton /period)</td><td>13363</td><td>15741</td></tr></table>
Indicate what the data are used for (Baseline/ Project/ Leakage emission calculations)	Baseline Calculation
Monitoring equipment (type, accuracy class, serial number, calibration frequency, date of last calibration, validity)	<table><tr><td></td><td>**Plant I**</td><td>**Plant II**</td></tr><tr><td>Type</td><td>mass flow meter</td><td>mass flow meter</td></tr><tr><td>Accuracy class</td><td>± 0.15%</td><td>± 0.15%</td></tr><tr><td>Serial No.</td><td>6T 681125</td><td>28 29138</td></tr><tr><td>Calibration frequency</td><td>2years</td><td>2years</td></tr><tr><td>Date of last calibration</td><td>2010-Oct-07</td><td>2010-Oct-07</td></tr><tr><td>Validity</td><td>N/A</td><td>N/A</td></tr><tr><td>Model</td><td>PROMASS63</td><td>PROMASS60</td></tr><tr><td>Maker</td><td colspan="2">ENDRESS HAUSER</td></tr></table>
Measuring/ Reading/ Recording frequency:	•Measuring period : Continuously •Reading frequency : hourly •Recording frequency : Daily
Calculation method (if applicable):	Not applicable
QA/QC procedures applied:	Cross-check of amount of the produced caprolactam is performed on the basis of stock change data and weighbridge data.

Data / Parameter:	***$T_{g,d}$***
Data unit:	^{o}C
Description:	Actual operating temperature of the ammonia oxidation reactor on day *d*
Measured /Calculated /Default:	Measured
Source of data:	Thermocouple
Value(s) of monitored parameter:	(see table below)
Indicate what the data are used for (Baseline/ Project/ Leakage emission calculations)	Baseline Calculation
Monitoring equipment (type, accuracy class, serial number, calibration frequency, date of last calibration, validity)	(see tables below)
Measuring/ Reading/ Recording frequency:	•Measuring period : Continuously •Reading frequency : Not applicable •Recording frequency : Daily
Calculation method (if applicable):	Not applicable
QA/QC procedures applied:	Not applicable

Value(s) of monitored parameter:

		Average value of ^{o}C/day in period #1
Plant I	T_{g-a}	713
	T_{g-b}	739
Plant II	T_{g-c}	760
	T_{g-d}	758

Monitoring equipment:

Plant I

	T_{g-a}	T_{g-b}
Type	Thermocouple K	Thermocouple K
Accuracy class	± 2.5°C	± 2.5°C
Serial No.	2170447	2170446
Calibration frequency	2 years	2 years
Date of last calibration	N/A	N/A
Validity	N/A	N/A
Model	R121	
Maker	WISE	

Plant II

	T_{g-c}	T_{g-d}
Type	Thermocouple K	Thermocouple K
Accuracy class	± 5.6 °C	± 5.6 °C
Serial No.	11564	11563
Calibration frequency	2years	2years
Date of last calibration	N/A	N/A
Validity	N/A	N/A
Model	TE	
Maker	YAMARI	

<table>
<tr><td>Data / Parameter:</td><td>$P_{g,d}$</td></tr>
<tr><td>Data unit:</td><td>Pa gauge</td></tr>
<tr><td>Description:</td><td>Actual operating pressure of the ammonia oxidation reactor on day d</td></tr>
<tr><td>Measured /Calculated /Default:</td><td>Measured</td></tr>
<tr><td>Source of data:</td><td>Pressure gauge</td></tr>
<tr><td>Value(s) of monitored parameter:</td><td>
<table>
<tr><td></td><td></td><td>Average value of Pa/day in period #1</td></tr>
<tr><td>Plant I</td><td>P_{g-1}</td><td>86106</td></tr>
<tr><td>Plant II</td><td>P_{g-2}</td><td>86118</td></tr>
</table>
</td></tr>
<tr><td>Indicate what the data are used for (Baseline/ Project/ Leakage emission calculations)</td><td>Baseline Calculation</td></tr>
<tr><td>Monitoring equipment (type, accuracy class, serial number, calibration frequency, date of last calibration, validity)</td><td>
<table>
<tr><td></td><td>Plant I (P_{g-1})</td><td>Plant II (P_{g-2})</td></tr>
<tr><td>Type</td><td>Gauge Pressure</td><td>Gauge Pressure</td></tr>
<tr><td>Accuracy class</td><td>± 0.1%</td><td>± 0.1%</td></tr>
<tr><td>Serial No.</td><td>10530360183</td><td>10530360212</td></tr>
<tr><td>Calibration frequency</td><td>2yrs</td><td>2yrs</td></tr>
<tr><td>Date of last calibration</td><td>-</td><td>-</td></tr>
<tr><td>Validity</td><td>-</td><td>-</td></tr>
<tr><td>Model</td><td colspan="2">STG 944</td></tr>
<tr><td>Maker</td><td colspan="2">Honeywell</td></tr>
</table>
</td></tr>
<tr><td>Measuring/ Reading/ Recording frequency:</td><td>•Measuring period : Continuously
•Reading frequency : Not applicable
•Recording frequency : Daily</td></tr>
<tr><td>Calculation method (if applicable):</td><td>Not applicable</td></tr>
<tr><td>QA/QC procedures applied:</td><td>Not applicable</td></tr>
</table>

Data / Parameter:	$A_{OR,d}$
Data unit:	tNH_3/day
Description:	Actual ammonia flow rate to the ammonia oxidation reactor (AOR)
Measured /Calculated /Default:	Measured
Source of data:	Differential pressure transmitter with normalizing functions
Value(s) of monitored parameter:	(see table below)
Indicate what the data are used for (Baseline/ Project/ Leakage emission calculations)	Baseline Calculation
Monitoring equipment (type, accuracy class, serial number, calibration frequency, date of last calibration, validity)	(see table below)
Measuring/ Reading/ Recording frequency:	•Measuring period : Continuously •Reading frequency : Not applicable •Recording frequency : Daily
Calculation method (if applicable):	Not applicable
QA/QC procedures applied:	Not applicable

Value(s) of monitored parameter:

		Average value of day in period #1
Plant I	FIC-1201	38.25
Plant II	2FIC-1201	40.93

Monitoring equipment:

	Plant I (P_{g-1})	Plant II (P_{g-2})
Type	Differential Pressure	Differential Pressure
Accuracy class	± 0.1% Span	± 0.1%
Serial No.	10530360038	10530360080
Calibration frequency	3yrs	3yrs
Date of last calibration	-	-
Validity	-	-
Model	STD 924	
Maker	Honeywell	

Data / Parameter:	G_{sup}
Data unit:	-
Description:	Supplier of the ammonia oxidation catalyst
Measured /Calculated /Default:	Not applicable
Source of data:	Supplier information on catalyst delivery confirmation document
Value(s) of monitored parameter:	Johnson Matthey
Indicate what the data are used for (Baseline/ Project/ Leakage emission calculations)	Baseline Calculation
Monitoring equipment (type, accuracy class, serial number, calibration frequency, date of last calibration, validity)	Not applicable
Measuring/ Reading/ Recording frequency:	Recording frequency : Date of changing ctalyst
Calculation method (if applicable):	Not applicable
QA/QC procedures applied:	Not applicable

Data / Parameter:	G_{com}
Data unit:	%
Description:	Composition of the ammonia oxidation catalyst
Measured /Calculated /Default:	Not applicable
Source of data:	Supplier information on catalyst delivery confirmation document
Value(s) of monitored parameter:	Pt (90)% : Rh(10)%
Indicate what the data are used for (Baseline/ Project/ Leakage emission calculations)	Baseline Calculation
Monitoring equipment (type, accuracy class, serial number, calibration frequency, date of last calibration, validity)	Not applicable
Measuring/ Reading/ Recording frequency:	Recording frequency : Date of changing ctalyst
Calculation method (if applicable):	Not applicable
QA/QC procedures applied:	Not applicable

Data / Parameter:	***$Type_{HC}$***
Data unit:	Not applicable
Description:	Type of hydrocarbon
Measured /Calculated /Default:	Not applicable
Source of data:	Hydrocarbon supplier
Value(s) of monitored parameter:	Not applicable
Indicate what the data are used for (Baseline/ Project/ Leakage emission calculations)	Project emission
Monitoring equipment (type, accuracy class, serial number, calibration frequency, date of last calibration, validity)	Not applicable
Measuring/ Reading/ Recording frequency:	Month
Calculation method (if applicable):	Not applicable
QA/QC procedures applied:	Not applicable

Data / Parameter:	***$Q_{NG,y}$***
Data unit:	Nm^3
Description:	Natural gas input for re-heating the tail gas
Measured /Calculated /Default:	Measured
Source of data:	Flow meter with normalizing functions
Value(s) of monitored parameter:	<table><tr><th>Q_{NG}</th><th>Plant I</th><th>Plant II</th></tr><tr><td>Average value of (Nm^3/day) in period #1</td><td>468.72</td><td>822.12</td></tr></table>
Indicate what the data are used for (Baseline/ Project/ Leakage emission calculations)	Project emission
Monitoring equipment (type, accuracy class, serial number, calibration frequency, date of last calibration, validity)	<table><tr><th></th><th>Plant I (P_{g-1})</th><th>Plant II(P_{g-2})</th></tr><tr><td>Type</td><td>Orifice</td><td>Orifice</td></tr><tr><td>Accuracy class</td><td>±0.90%</td><td>±0.90%</td></tr><tr><td>Serial No.</td><td>02319622</td><td>02319623</td></tr><tr><td>Calibration frequency</td><td>2 years</td><td>2 years</td></tr><tr><td>Date of last calibration</td><td>-</td><td>-</td></tr><tr><td>Validity</td><td>-</td><td>-</td></tr></table>
Measuring/ Reading/ Recording frequency:	Once every two years
Calculation method (if applicable):	
QA/QC procedures applied:	Not applicable

Data / Parameter:	CF_{CH4}
Data unit:	-
Description:	Methane content of hydrocarbon (natural gas)
Measured /Calculated /Default:	Not applicable
Source of data:	Information provided by the natural gas supplier
Value(s) of monitored parameter:	<table><tr><th>Month</th><th>June, 2011</th><th>July, 2011</th><th>August, 2011</th><th>Period 1</th></tr><tr><td>CF_{CH4}</td><td>0.9152</td><td>0.9159</td><td>0.9138</td><td>0.9150</td></tr></table>
Indicate what the data are used for (Baseline/ Project/ Leakage emission calculations)	Not applicable
Monitoring equipment (type, accuracy class, serial number, calibration frequency, date of last calibration, validity)	Not applicable
Measuring/ Reading/ Recording frequency:	Recording frequency : Monthly
Calculation method (if applicable):	Not applicable
QA/QC procedures applied:	Not applicable

Data / Parameter:	$Q_{CH4,y}$
Data unit:	Nm^3/yr
Description:	Methane part of the natural gas used.
Measured /Calculated /Default:	Calculated
Source of data:	Information provided by the natural gas supplier
Value(s) of monitored parameter:	<table><tr><th>Month</th><th>June, 2011</th><th>July, 2011</th><th>August, 2011</th><th>Period 1</th></tr><tr><td>Plant I</td><td>462.44</td><td>405.86</td><td>418.29</td><td>428.86</td></tr><tr><td>Plant II</td><td>760.33</td><td>747.46</td><td>749.43</td><td>752.41</td></tr></table>
Indicate what the data are used for (Baseline/ Project/ Leakage emission calculations)	Not applicable
Monitoring equipment (type, accuracy class, serial number, calibration frequency, date of last calibration, validity)	Not applicable
Measuring/ Reading/ Recording frequency:	Not applicable
Calculation method (if applicable):	$Q_{HC,y} = Q_{NG,y} \times CF_{CH4}$
QA/QC procedures applied:	Not applicable

Data / Parameter:	$Q_{HC,y}$
Data unit:	Nm^3
Description:	The hydrocarbon with two or more molecules of carbon in natural gas used
Measured /Calculated /Default:	Calculated
Source of data:	Information provided by the natural gas supplier
Value(s) of monitored parameter:	Month / June, 2011 / July, 2011 / August, 2011 / Period 1 Plant I: 42.85 / 37.27 / 39.46 / 39.86 Plant II: 70.45 / 69.26 / 69.44 / 69.72
Indicate what the data are used for (Baseline/ Project/ Leakage emission calculations)	Not applicable
Monitoring equipment (type, accuracy class, serial number, calibration frequency, date of last calibration, validity)	Not applicable
Measuring/ Reading/ Recording frequency:	Not applicable
Calculation method (if applicable):	$Q_{HC,y} = Q_{NG,y} \times (1-CF_{CH4})$
QA/QC procedures applied:	Not applicable

Month	June, 2011	July, 2011	August, 2011	Period 1
Plant I	42.85	37.27	39.46	39.86
Plant II	70.45	69.26	69.44	69.72

Data / Parameter:	ρ_{NG}
Data unit:	t/Nm^3
Description:	Density of the natural gas
Measured /Calculated /Default:	Not applicable
Source of data:	Monthly report provided by the fuel supplier
Value(s) of monitored parameter:	Month / June, 2011 / July, 2011 / August, 2011 / Period 1 ρ_{NG}: 0.800 / 0.7966 / 0.7962 / 0.798
Indicate what the data are used for (Baseline/ Project/ Leakage emission calculations)	Not applicable
Monitoring equipment (type, accuracy class, serial number, calibration frequency, date of last calibration, validity)	Not applicable
Measuring/ Reading/ Recording frequency:	Recording frequency : Monthly
Calculation method (if applicable):	Not applicable

Month	June, 2011	July, 2011	August, 2011	Period 1
ρ_{NG}	0.800	0.7966	0.7962	0.798

QA/QC procedures applied:	Not applicable
Data / Parameter:	$\boldsymbol{\rho_{HC}}$
Data unit:	t/m^3
Description:	Density of the hydrocarbon with two or more molecules of carbon in natural gas
Measured /Calculated /Default:	Calculated
Source of data:	Information provided by the natural gas supplier
Value(s) of monitored parameter:	<table><tr><td>Month</td><td>June, 2011</td><td>July, 2011</td><td>August, 2011</td><td>Period 1</td></tr><tr><td>$\boldsymbol{\rho_{HC}}$</td><td>0.00167</td><td>0.00167</td><td>0.00165</td><td>0.00166</td></tr></table>
Indicate what the data are used for (Baseline/ Project/ Leakage emission calculations)	Not applicable
Monitoring equipment (type, accuracy class, serial number, calibration frequency, date of last calibration, validity)	Not applicable
Measuring/ Reading/ Recording frequency:	Not applicable
Calculation method (if applicable):	$\rho_{HC} = (\rho_{NG}-\rho_{CH4} \times CF_{CH4}) / (1-CF_{CH4})$
QA/QC procedures applied:	Not applicable

<table>
<tr><td>Data / Parameter:</td><td>$\boldsymbol{EF_{NG}}$</td></tr>
<tr><td>Data unit:</td><td>tCO_2/tNG</td></tr>
<tr><td>Description:</td><td>Emission factor of the natural gas</td></tr>
<tr><td>Measured /Calculated /Default:</td><td>Calculated</td></tr>
<tr><td>Source of data:</td><td>Information provided by the natural gas supplier</td></tr>
<tr><td>Value(s) of monitored parameter:</td><td><table><tr><td>Month</td><td>June, 2011</td><td>July, 2011</td><td>Aug. 2011</td><td>Period 1</td></tr><tr><td>$\boldsymbol{EF_{NG}}$</td><td>2.770</td><td>2.770</td><td>2.771</td><td>2.770</td></tr></table></td></tr>
<tr><td>Indicate what the data are used for (Baseline/ Project/ Leakage emission calculations)</td><td>Project emission</td></tr>
<tr><td>Monitoring equipment (type, accuracy class, serial number, calibration frequency, date of last calibration, validity)</td><td>Not applicable</td></tr>
<tr><td>Measuring/ Reading/ Recording frequency:</td><td>Not applicable</td></tr>
<tr><td>Calculation method (if applicable):</td><td>$EF_{NG} = COEF_{NG} \times NCV_{NG}/\rho_{NG} \times 44/12$

Where
$COEF_{NG}$: Carbon Emission factor of natural gas [tC/TJ]
15.3[tC/TJ] is applied to this project as Ex-ante value by IPCC DEFAULT VALUES OF CARBON CONTENT of “Natural Gas” in TABLE 1.3 (2006 IPCC Guidelines for National Greenhouse Gas Inventories Volume 2, Energy)

NCV_{NG} : Net calorific value of the natural gas [TJ/Nm^3]
For this project, 9,393 $kcal/Nm^3$ is offered by KOGAS.
9,393$kcal/Nm^3$ is able to be converted to 3.9327×10^{-5} TJ/Nm^3
ρ_{NG} : Density of the natural gas[t/Nm^3]
For this project, 0.000797t/Nm^3 is set based on data source by natural gas supplier.</td></tr>
<tr><td>QA/QC procedures applied:</td><td>Not applicable</td></tr>
</table>

Data / Parameter:	EF_{HC}
Data unit:	tCO_2/tHC
Description:	Emission factor of the hydrocarbon with two or more molecular of carbon, which is existed as a contents of the natural gas
Measured /Calculated /Default:	Calculated
Source of data:	Calculated based on the followings: Methane content offered by the fuel supplier ; The density of the natural gas provided by the fuel supplier ; Estimated emission factor of the natural gas, and Specified methane density
Value(s) of monitored parameter:	Month / June, 2011 / July, 2011 / August, 2011 / Period 1 EF_{HC} / 2.860 / 2.863 / 2.869 / 2.864
Indicate what the data are used for (Baseline/ Project/ Leakage emission calculations)	Project emission
Monitoring equipment (type, accuracy class, serial number, calibration frequency, date of last calibration, validity)	Not applicable
Measuring/ Reading/ Recording frequency:	Not applicable
Calculation method (if applicable):	$EF_{HC} = (EF_{NG} \times \rho_{NG} - EF_{CH4} \times \rho_{CH4} \times CF_{CH4}) / (1-CF_{CH4}) / \rho_{HC}$ Where EF_{NG} : CO_2 emission factor of NG[tCO_2/tNG] For this project, 2.768 [tCO_2/tNG] is taken as described above ρ_{NG} : Density of natural gas (tNG/m^3) The value ρ_{NG} for this is 0.000797 (tNG/m^3) in this project EF_{CH4} : CO_2 emission factor of CH_4(tCO_2/tCH_4) 2.75(tCO_2/tCH_4) by theoretical calculation. ρ_{CH4} : Density of methane (tCH_4/m^3), 0.000716 as a characteristic number CF_{CH4} : Methane fraction in the natural gas 0.9123 is set based on data source by natural gas supplier.
QA/QC procedures applied:	Not applicable

Data / Parameter:	***SE_{N2O}***
Data unit:	$kgN_2O/tCaprolactam$
Description:	N_2O emission rate per ton of caprolactam
Measured /Calculated /Default:	Calculated
Source of data:	Baseline and Monitoring Methodology (AM28 ver05)
Value(s) of monitored parameter:	<table><tr><th></th><th>Plant I</th><th>Plant II</th></tr><tr><td>SE_{N2O, period}(kgN₂O/tCaprolactam)</td><td>23.349</td><td>14.444</td></tr></table>
Indicate what the data are used for (Baseline/ Project/ Leakage emission calculations)	Baseline emission
Monitoring equipment (type, accuracy class, serial number, calibration frequency, date of last calibration, validity)	Not applicable
Measuring/ Reading/ Recording frequency:	Not applicable
Calculation method (if applicable):	$SE_{N2O,y} = QI_{N2O,y} / P_{product,y} \times 1000$ Where, $QI_{N2O,y}$ means Quantity of N_2O emissions at the inlet of the destruction facility in year, y (t N_2O) given by : $QI_{N2O,y} = \sum_{i}^{n} F_{TI,i} \times CI_{N2O,i} \times M_i$
QA/QC procedures applied:	Not applicable

Data / Parameter:	***$OXID_{CH4}$***
Data unit:	%
Description:	Oxidation factor of CH_4 in natural gas for re-heating tail gas
Measured /Calculated /Default:	Calculated
Source of data:	Not applicable
Value(s) of monitored parameter:	<table><tr><th>OXID_{CH4}</th><th>Plant I</th><th>Plant II</th></tr><tr><td>Average value of (%) in period #1</td><td>93.58</td><td>98.11</td></tr></table>
Indicate what the data are used for (Baseline/ Project/ Leakage emission calculations)	Project emission
Monitoring equipment (type, accuracy class, serial number, calibration frequency, date of last calibration, validity)	Not applicable

Measuring/ Reading/ Recording frequency:	Not applicable
Calculation method (if applicable):	$OXID_{CH4}=\{ Q_{CH4} -(\sum_{i}^{n} F_{TE,i} \times CO_{CH4,i} \times 10^{-6})\} / Q_{CH4} \times 100$
QA/QC procedures applied:	Not applicable

Data / Parameter:	***CO_{CH4}***
Data unit:	ppm (v)
Description:	Methane concentration at destruction facility outlet.
Measured /Calculated /Default:	Measured
Source of data:	Non-dispersion infrared absorption analyzer with dual-channel as a gas path
Value(s) of monitored parameter:	see table below
Indicate what the data are used for (Baseline/ Project/ Leakage emission calculations)	Project emission
Monitoring equipment (type, accuracy class, serial number, calibration frequency, date of last calibration, validity)	see table below
Measuring/ Reading/ Recording frequency:	•Measuring period : Continuously •Reading frequency : Not applicable •Recording frequency : Daily
Calculation method (if applicable):	Not applicable
QA/QC procedures applied:	Not applicable

Value(s) of monitored parameter:

CO_{CH4}	Plant I	Plant II
Average value of (ppm_v) in period #1	25.15	13.68

Monitoring equipment:

	Plant I CO_{CH4-1}	Plant II CO_{CH4-2}
Type	NDIR	NDIR
Accuracy class	>95%	>95%
Serial No.	AO-750	AO-751
Calibration frequency	Every 2weeks	Every 2weeks
Date of last calibration	2011-August-25	2011-August-25
Validity	-	-
Model	ULTRAMAT 6, SIEMENS	ULTRAMAT 6, SIEMENS

Data / Parameter:	***Reg_{NOx}***
Data unit:	tNO_x/Nm^3
Description:	National regulation on NO_x emissions
Measured /Calculated /Default:	Not applicable
Source of data:	The "Clean Air Conservation Act", one of the National environmental legislation, Ministry of Environment
Value(s) of monitored parameter:	
Indicate what the data are used for (Baseline/ Project/ Leakage emission calculations)	Baseline emission
Monitoring equipment (type, accuracy class, serial number, calibration frequency, date of last calibration, validity)	Not applicable
Measuring/ Reading/ Recording frequency:	Not applicable
Calculation method (if applicable):	Recording frequency : Date of Regulation
QA/QC procedures applied:	Not applicable

Data / Parameter:	***$RSE_{N2O,y}$***
Data unit:	tN_2O/tCaprolactam
Description:	Regulatory limit of N_2O emissions per unit of outlet of caprolactam (tN_2O/t caprolactam)
Measured /Calculated /Default:	Not applicable
Source of data:	National legislation in Republic of Korea. (That may be mostly like environmental regulation.)
Value(s) of monitored parameter:	Not applicable
Indicate what the data are used for (Baseline/ Project/ Leakage emission calculations)	Baseline emission
Monitoring equipment (type, accuracy class, serial number, calibration frequency, date of last calibration, validity)	Not applicable
Measuring/ Reading/ Recording frequency:	Not applicable
Calculation method (if applicable):	Recording frequency : Date of Regulation
QA/QC procedures applied:	Not applicable

SECTION E. Emission reductions calculation

E.1. Baseline emissions calculation

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Based on the production of caprolactam during this first period, it is not available to be decided whether the yearly production($P_{product,y}$) exceeds the design capacity ($P_{\text{product,max}}$). Therefore on the assumption $P_{product,y} < P_{product,\ max}$, baseline emissions (*BE*)for this period are given by following equation :

$$BE_{\ period} = \left(\sum_{i}^{n} F_{TI,i} \times CI_{N2O,i} \times M_i\right) \times GWP_{N2O}$$

Where

M_i	Length of Measuring Interval (hr), (1hr: fixed value)
GWP_{N2O}	Global warming potential of the nitrous oxide, (310: default value).
n	Number of intervals during this period
$F_{TI,i}$	Volume flow rate at the inlet of the DF during interval (Nm^3/hr)
$CI_{N2O,i}$	N_2O concentration in the tail gas of the DF inlet during interval ($tN_2O/\ Nm^3$)

If the actual average daily operating temperature and/or pressure in the ammonia oxidation reactor (T_g and P_g) are outside a "permitted range" of operating temperatures and/or pressures ($T_{g,hist}$ and $P_{g,hist}$), the baseline emission is integrated of the daily daseline emission($BE,_{daily,\ out\ of\ permit\ range}$) for the respective day in which AOR operation conditions were outside of "permitted range". The daily baseline emission is calculated for the respective time period as follows:

$$BE,_{daily,\ out\ of\ permit\ range} = P_{product,\ day} \times EF_{N2O} \times GWP_{N2O} / 1000$$

Where

$BE,_{daily,\ out\ of\ permit\ range}$	The daily daseline emission for the respective day in which AOR operation conditions were outside of "permitted range (tonCO_2/day)
$P_{product,\ day}$	The daily output of caprolactam for the respective day in which AOR operation conditions were outside of permitted range (ton caprolactam/day)
EF_{N2O}	N_2O Emission factor to the process of caprolactam production (kgN_2O/ton caprolactam)

Emission factor of N_2O(EF_{N2O}) is the lowest value among (a) $EF_{N2O,IPCC}$, (b) $SE_{N2O,y}$ and (c) any related value as a result of legal regulation(e.g. $RSE_{N2O,y}$). In Republic of Korea, there is no mandatory regulation for N_2O emission. Therefore, actually *EF of* N_2O is the lower value between (a) $F_{N2O,IPCC}$ and (b) $SE_{N2O,y}$.

$F_{N2O,IPCC}$ means Conservative IPCC default value of the latest IPCC GHG Inventory Guidelines accepted by the IPCC for the equivalent N_2O emission process. At this time, $F_{N2O,IPCC}$ is 5.4kgN_2O/tonne of caprolactam.

$SE_{N2O,y}$ is the specific N_2O emission per unit of output of caprolactam defined as :

$$SE_{N2O,y} = QI_{N2O,y} / P_{product,y} \times 1000$$

Where, $QI_{N2O,y}$ means Quantity of N_2O emissions at the inlet of the destruction facility in year, y (t N_2O) given by :

$$QI_{N2O,y} = \sum_{i}^{n} F_{TI,i} \times CI_{N2O,i} \times M_i$$

For this period, $SE_{N2O,y}$ should be converted as $SE_{N2O,period}$ as follows :

$$SE_{N2O,period} = QI_{N2O,period} / P_{product,period}$$

On condition of that the actual daily ammonia flow rate exceeds the (upper) limit on maximum historical daily permitted ammonia flow rate, the baseline N_2O emissions for this operating day are capped at conservative IPCC default values. Where, the upper limit on ammonia flow should be determined based on “the historical operating data on maximum daily average ammonia flow”.

1. Plant I

BE in Plant I with AOR operation conditions within “permitted range”

Hourly BE ($BE_{,hr-1}$) calculated on hourly integrated measured values of $F_{TI,i-1}$and $CI_{N2O,-1i}$ are aggregated to the daily BE($BE_{,day-1}$), and total BE on the period ($BE_{,period-1}$) are estimate as sum of $BE_{,day-1}$. Below table is to show the values of parameters and amount of BE.

Table E.1 BEin Plant I with AOR operation conditions within “permitted range”

			(dd~dd/mm/yyyy) 09~30/06/2011	(dd~dd/mm/yyyy) 01~31/07/2011	(dd~dd/mm/yyyy) 01~31/08/2011	Period #1
No. of days corresponding			22days	31days	31 days	84days
Value of Parameters	n	: Total	482	739	728	1949
	$F_{TI,i}$ (Nm^3/hr)	: Average	40,824	41,160.2801	40,121.7709	40,702
	$CI_{N2O,i}$(tN_2O/ Nm^3)	: Average	3.88057E-06	3.90000E-06	3.98697E-06	3.92E-06
BE	$BE_{,period}$: Total of BE_{day}		23650.462	36,766.77	36,306.04	96723.275

BE in case of AOR operation conditions outside of “permitted range”.

In case of Plant I, permit range of AOR operation condition has been kept for period 1. Therefore it is not necessary that the baseline emission calculation for period 1 depending on IPCC default values or ($SE_{N2O,y}$)the specific N_2O emission per unit of output of caprolactam.

2. Plant II

BE by Plant 2 with AOR operation conditions outside of “permitted range”

Hourly BE ($BE_{,hr-2}$) calculated on hourly integrated measured values of $F_{T\,i-2}$ and $CI_{N2O,i-2}$ are aggregated to the daily BE($BE_{,day-2}$), and total BE on the period ($BE_{,period-2}$) are estimate as sum of $BE_{,day-2}$. Below table is to show the values of parameters and amount of BE.

Except 1day (7 July, 2011), all of daily average values of the AOR operation condition parameters have been kept within permit range. So, it is excluded for calculation that measured values of relevant parameters with BE calculation ($F_{TI,2}$, and $CI_{N2O,i}$) of the day in which AOR was operated outside of permit range.

Table E.2 BE in Plant 2 with AOR operation conditions within "permitted range"

			(dd~dd/mm/yyyy) 09~30/06/2011	(dd~dd/mm/yyyy) 01~31/07/2011	(dd~dd/mm/yyyy) 01~31/08/2011	Period #1
No. of days corresponding			22days	31days	31 days	84days
Value of Parameters	N	: Total	485	684	739	1908
	$F_{TI,i}$ (Nm^3/hr)	: Average	38,803	38,738	37,919	38,487
	$CI_{N2O,i}$(tN_2O/ Nm^3)	: Average	3.36E-06	3.02E-06	2.92E-06	3.098E-06
$BE_{,period ,permit}$	Total of $BE_{day,permit}$		19579.198	24,709.55	25,336.60	69625.347

BE in case of AOR operation conditions outside of "permitted range".

In order to determined the daily BE($BE_{, day-2}$) to the day in which AOR was operated outside of permit range, EF_{N2O} is determined to 5.4 kgN_2O/tCaprolactam because that it the the lower value between (a) $F_{N2O,IPCC}$ and (b) $SE_{N2O,period}$ as below table.

EF_{N2O}	Value	Note			
$EF_{N2O,IPCC}$	5.4	Unit : kgN_2O/tCaprolactam			
$SE_{N2O,period}$	14.444	parameter	Valuse	Unit	note
		$QI_{N2O,period\text{-}2}$	70482	kg N_2O/period	Intergrated $QI_{N2O,hr}$ which is calculated on N_2O concentration and tail gas flow rate measured in inlet of DF.
		$P_{product,period,-2}$	15741	ton/period	
		Unit : kgN_2O/tCaprolactam			

Baseline emission is integrated of the daily daseline emission($BE,_{daily, out of permit range}$) for the respective day in which AOR operation conditions were outside of "permitted range". The daily daseline emission is calculated given by:

$$BE,_{daily,\ out\ of\ permit\ range} = P_{product,\ day} \times EF_{N2O,IPCC} \times GWP_{N2O} / 1000$$

Table E.3 BE in Plant 2 with AOR operation conditions outside of "permitted range"

Date(dd/mm/yyyy)	$P_{product,\ day,\ out\ of\ permit\ range}$	$BE,_{daily,\ out\ of\ permit\ range}$
07/07/2011	213.120 (t/day)	356.76 ($tonCO_2$/day)
Total ($BE_{periodout\ of\ permit\ range}$)	356.76 ($tonCO_2$/period)	

Total BE in this period is 166705ton CO2 as shown below table

Table E.4 BE in Period#1

		Plant I ($BE_{period-1}$)	Plant II ($BE_{period-2}$)
BE_{period} on AOR condition	within "permitted range	96723.275	69625.347
	Outside "permitted range	0	356.763
BE_{period} total	BE_{period} for each plant	96723.275	69982.11
	BE_{period} for both plants	166705.4	

E.2. Project emissions calculation

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The emission due to the project activity are composed of (a) the emissions of not destroyed N2O, (b) on-site emissions due to the hydrocarbons (; LNG) use as input to the N2O destruction facility, and (c) the emissions from the operation of the destruction facility.

Hydrocarbons can be used as reducing agent and/or re-heating the tail gas to enhance the catalytic N_2O reduction efficiency. In this project, natural gas is used for re-heating the tail gas to enhance the catalytic N_2O reduction efficiency

$$PE_{period} = \left(\sum_{i}^{n} F_{TE,i} \times CO_{N2O,i} \times M_i\right) \times \mathrm{GWP_{N2\,O}}$$
$$+ \left[(\rho_{HC} \times Q_{HC,y} \times EF_{HC} \times OXID_{HC}/100) + (\rho_{CH4} \times Q_{CH4,y} \times EF_{CH4} \times OXID_{CH4}/100) \right]$$
$$+ \left[\rho_{CH4} \times Q_{CH4,y} \times GWP_{CH4} \times (1-OXID_{CH4}/100) \right]$$

n	: Number of intervals during the year ($period^{-1}$)
M_i	: Length of Measuring Interval (hr), 1hr (: Fixed value)
$F_{TE,i}$	: Volume flow rate at the exit of the DF during interval *i* (Nm^3/hr)
$CO_{N2O,i}$	: N_2O concentration in the tail gas of the DF exit during interval *i* (tN_2O/ m^3)
GWP_{CH4}	: Global warming potential of CH_4, 21 (: default value)
GWP_{N2O}	: Global warming potential of the nitrous oxide, 310 (: default value)
ρ_{CH4}	: Density of methane (tCH_4/m^3) , 0.000716
ρ_{HC}	: Density of HC (tHC/m^3)
EF_{CH4}	: CO_2 emission factor of CH_4 (tCO_2e/tCH_4), 2.75
EF_{HC}	: CO_2 emission factor of HC with two or more carbon molecule in natural gas (tCO_2e/tHC)
$Q_{CH4,y}$	: Methane used in period (Nm^3/period)
$Q_{HC,y}$	: HC with two or more carbon molecule in natural gas used in period (Nm^3/period)
$OXID_{CH4}$	: Oxidation factor of methane (%)
$OXID_{HC}$	: Oxidation factor of HC(%), 100% (Fixed value)

Hourly calculated PE ($PE_{,hr}$) are aggregated into the daily PE($PE_{,day}$), and total PE on the period ($PE_{,period}$) are estimated as sum of $PE_{,day}$. Below tables are to show the values of all of parameters required for calculating PE, and PE_{period}.

Table E.5 Project Emission generated in Plant I ($PE,_{period-1}$)

	Parameters	Unit	(dd~dd/mm/yyyy) 09~30/06/2011	(dd~dd/mm/yyyy) 01~31/07/2011	(dd~dd/mm/yyyy) 01~31/08/2011	Period#1	Note
			22days	31days	31 days	84days	
Measured Value	F_{TE-1}	Nm^3/hr	45258.76	45336.89	44853.25	45149.63	daily average
	CO_{N2O-1}	tN_2O/ Nm^3	3.74.E-07	3.77.E-07	3.92.E-07	3.81.E-07	daily average
	$Q_{NG,day-1}$	m^3/day	505.29	443.13	457.74	468.72	daily average
	CO_{CH4-1}	ppm_v	23.27	25.40	26.78	25.15	daily average
LNG information (Monthly monitored)	ρ_{NG}	tNG/ m^3	0.8	0.7966	0.7962	0.80	Provided by supplier
	CF_{CH4}	%	91.52	91.59	91.38	91.50	Provided by supplier
	NCV_{NG}	$kcal/N\ m^3$	9395.2	9394.7	9393.9	9394.60	Provided by supplier
		$TJ/ N\ m^3$	3.93E-05	3.93E-05	3.93E-05	3.93E-05	NCV_{NG} (kcal/N m^3) $\times$ 4.1868 $\times 10^{-9}$
Calculated	ρ_{HC}	$tHC/N\ m^3$	0.00167	0.00167	0.00165	0.001663	$\rho_{HC} = (\rho_{NG}-\rho_{CH4} \times CF_{CH4}) /(1-CF_{CH4})$
	EF_{NG}	tCO_2/tNG	2.770	2.770	2.771	2.770	$EF_{NG} = COEF_{NG} \times NCV_{NG} /\rho_{NG} \times 44/12$
	EF_{HC}	tCO_2/tHC	2.860	2.863	2.869	2.864	$EF_{HC}= (EF_{NG} \times \rho_{NG} -EF_{CH4} \times \rho_{CH4} \times CF_{CH4})/(1-CF_{CH4})/\rho_{HC}$
	$Q_{HC,day}$	Nm^3/day	42.85	37.27	39.46	39.86	$Q_{HC,d}= Q_{NG,d} \times (1-CF_{CH4})]$
	$Q_{CH4,day}$	Nm^3/day	462.44	405.86	418.29	428.86	$Q_{CH4,d} = Q_{NG,d} \times CF_{CH})$
	$OXID_{CH4}$	%	94.44	93.17	93.12	93.58	$OXID_{CH4}=\{Q_{CH4}-(\sum F_{TE,\ i} \times CO_{CH4,I} \times 10^{-6})\} / Q_{CH4} \times 100$
Fixed Value	$OXID_{HC}$	%				100	
	EF_{CH4}	tCO_2/tCH_4				2.75	
	ρ_{CH4}	t/m^3				0.000716	
	GWP_{N2O}	N/A				310	
	GWP_{CH4}	N/A				21	
	$COEF_{NG}$	tC/TJ				15.3	
PE	$PE,_{period}$	tonCO2	2517.40	3943.70	4028.27	10489.37	Integration of PE_{day}

Table E.6 Project Emission generated in Plant II ($PE,_{period-2}$)

	Parameters	Unit	(dd~dd/mm/yyyy) 09~30/06/2011	(dd~dd/mm/yyyy) 01~31/07/2011	(dd~dd/mm/yyyy) 01~31/08/2011	Period#1	Note
			22days	31days	31 days	84days	
Measured Value	F_{TE-2}	Nm^3/hr	47775.77	47284.51	46160.86	47073.71	daily average
	CO_{N2O-2}	tN_2O/ Nm^3	2.91.E-07	2.72.E-07	2.65.E-07	2.76.E-07	daily average
	$Q_{NG,hr-2}$	m^3/day	830.78	816.72	818.87	822.12	daily average
	CO_{CH4-2}	ppm_v	14.25	14.59	12.21	13.68	daily average
LNG information (Monthly monitored)	ρ_{NG}	tNG/ m^3	0.8	0.7966	0.7962	0.80	Provided by supplier
	CF_{CH4}	%	91.52	91.59	91.38	91.50	Provided by supplier
	NCV_{NG}	$kcal/N\ m^3$	9395.2	9394.7	9393.9	9394.60	Provided by supplier
		$TJ/ N\ m^3$	3.93E-05	3.93E-05	3.93E-05	3.93E-05	NCV_{NG} (kcal/N m^3) × 4.1868 × 10^{-9}
Calculated	ρ_{HC}	$tHC/N\ m^3$	0.00167	0.00167	0.00165	0.001663	$\rho_{HC} = (\rho_{NG}-\rho_{CH4} \times CF_{CH4}) /(1-CF_{CH4})$
	EF_{NG}	tCO_2/tNG	2.770	2.770	2.771	2.770	$EF_{NG} = COEF_{NG} \times NCV_{NG} /\rho_{NG} \times 44/12$
	EF_{HC}	tCO_2/tHC	2.860	2.863	2.869	2.864	$EF_{HC}= (EF_{NG} \times \rho_{NG} -EF_{CH4} \times \rho_{CH4} \times CF_{CH4})/(1-CF_{CH4})/\rho_{HC}$
	$Q_{HC,day}$	Nm^3/day	70.45	69.26	69.44	69.72	$Q_{HC,d}= Q_{NG,d} \times (1-CF_{CH4})]$
	$Q_{CH4,day}$	Nm^3/day	760.33	747.46	749.43	752.41	$Q_{CH4,d} = Q_{NG,d} \times CF_{CH4})$
	$OXID_{CH4}$	%	97.98	98.15	98.20	98.11	$OXID_{CH4}=\{Q_{CH4}-(\sum F_{TE,i} \times CO_{CH4,I} \times 10^{-6})\} / Q_{CH4} \times 100$
Fixed Value	$OXID_{HC}$	%				100	98.15
	EF_{CH4}	tCO_2/tCH_4				2.75	
	ρ_{CH4}	t/m^3				0.000716	
	GWP_{N2O}	N/A				310	
	GWP_{CH4}	N/A				21	
	$COEF_{NG}$	tC/TJ				15.3	
PE	$PE,_{period}$	$tonCO_2$	2096.93	2839.83	2838.17	7774.92	Integration of PE_{day-2}

E.3. Leakage calculation

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The installation of the N_2O destruction facility doesn't result in significant additional energy consumption at the caprolactam production plant. In conclusion, no leakage is expected at this project.

The emission by leakage is accounted as zero ($LE_y = 0$)

E.4. Emission reductions calculation / table

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The emission reduction ER_{period} by the project activity during a given year y is the difference between the baseline emissions (BE_{period}) and project emissions (PE_{period}), as follows:

$$ER_{period} = BE_{period} - PE_{period} - LE_{period}$$

Table E.7 ER in Period#1

	BE_{period}	PE_{period}	ER_{period}
Plant I	96723.275	10489.37	86233.91
Plant II	69982.11	7774.92	62207.19
Total	166705.39	18264.29	148441.10

E.5. Comparison of actual emission reductions with estimates in the CDM-PDD

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Below table is to show comparison of actual values of the emission reductions achieved during the monitoring period with the estimations in the registered CDM-PDD.

Item		Values applied in ex-ante calculation of the registered CDM-PDD	Actual values reached during the monitoring period
BE,	Plant I	358,086	96723.275
	Plant II	381,323	69982.11
	Total	739,409	166705.39
PE,	Plant I	37,947	10489.37
	Plant II	40,467	7774.92
	Total	78,414	18264.29
LE,	Plant I	0	0
	Plant II	0	0
	Total	0	0
ER,	Plant I	320,139	86233.91
	Plant II	340,856	62207.19
	Total	660,995	148441.1
N_2O decomposition efficiency	Plant I	90%	89%
	Plant II	90%	89%
n	Plant I	8,712	1,949
	Plant II	8,520	1,908

It is not rational that the actual ER for this period is directly compared with ex-ante ER, since ex-ante ER in PDD are yearly value, and the actual ER values for this period is generated by just 84 operating

days. Therefore those values are converted to the daily values, in order to compare them on even ground as following table.

Item		Values applied in ex-ante calculation of the registered CDM-PDD	Actual values reached during the monitoring period
$BE,_d$	Plant I	986.46	1151.47
	Plant II	1074.15	833.12
	Total	2060.61	1984.59
$PE,_d$	Plant I	104.54	124.87
	Plant II	113.99	92.56
	Total	218.53	217.43
$LE,_d$	Plant I	0	0
	Plant II	0	0
	Total	0	0
$ER,_d$	Plant I	881.93	1026.59
	Plant II	960.16	740.56
	Total	1842.08	1767.16
$n,_{dily\ average}$	Plant I	24.00	23.20
	Plant II	24.00	22.71

Actual value of $ER,_d$ is as about 75CO_2 ton/day less than that of ex-ante $ER_{,d}$.

E.6. Remarks on difference from estimated value in the PDD

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Not applicable

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History of the document

Version	Date	Nature of revision
01	EB 54, Annex 34 28 May 2010	Initial adoption.
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