

MONITORING REPORT FORM (CDM-MR) *
Version 01 - in effect as of: 28/09/2010

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* as contained within the document entitled "Guidelines for completing the monitoring report form (CDM-MR)" (EB 54 meeting report, annex 34).

MONITORING REPORT
Version Number 1
17/05/2011
LG Chem Naju plant fuel switching project
Reference Number 2475
Monitoring Period 1 (04/06/2009 - 23/02/2011)

SECTION A. General description of the project activity

A.1. Brief description of the project activity:

LG Chem produces octanol, plasticizers and acrylic acid at its Naju plant. In the baseline scenario, steam, which is used in the production process of petrochemical products, is mainly produced in a boiler using bunker fuel oil C (Sulphur 0.5%). The Project activity involves retrofitting the boilers to allow fuel switching from bunker fuel oil C to natural gas. Natural gas is less carbon intensive than bunker fuel oil C. Therefore switching fuel from bunker fuel oil C to natural gas reduces GHG emissions.

The existing boiler has been retrofitted by installing special purpose burners for natural gas combustion as well as other necessary minor modifications. For fuel switching from bunker fuel oil C to natural gas, four natural gas burners have been installed for the main boiler. The total capacity of the four natural gas burners installed is 5,353 Nm³/hr, which is of sufficient capacity for the expected amount of natural gas consumption at Naju plant. The natural gas burners are provided by Hamworthy Combustion.

The start date of the project activity (the purchase date of the natural gas burners) was 21/06/2006. The project boiler retrofit was started on 30/09/2006 and a test-run of the project activity undertaken in November 2006. Project operation began on 20/11/2006. The project was registered on 04/06/2009.

The total emission reductions achieved in this monitoring period (04/06/2009 - 23/02/2011) are 15,534 tCO₂e.

A.2. Project Participants

Name of Party involved(*) ((host) indicates a host Party)	Private and/ or Public entity(ies) Project participants(*) (as applicable)	Kindly indicate if the Party involved wishes to be considered as project participants (Yes/ No)
Korea (host)	LG Chem, Ltd.	No
Japan	Mitsubishi UFJ Morgan Stanley Securities Co., Ltd	No

A.3. Location of the project activity:

The Project site is located at 1, Songwal-dong, Naju, Jeollanam-do, 520-130, Korea. It is located in Naju city about 20 km southwest of Gwangju International Airport.

The coordinates for the plant site are: 35.023013 N, 126.717460 E.

A.4. Technical description of the project

In the project scenario bunker fuel oil C is switched to natural gas. For fuel switching from bunker fuel oil C to natural gas, four natural gas burners have been installed for the main boiler. Total capacity of four natural gas burners installed is 5,353 Nm³/hr, which is sufficient capacity for the amount of natural gas consumption at Naju plant. The natural gas burners are provided by Hamworthy Combustion.

The specifications of the current boiler, the Project boiler (after modification) and natural gas burner are as follows:

Table 1. Boiler specification

	Project scenario
Capacity	70 T/H
Operating pressure	35 kg/cm ² G
Steam Temperature	400 °C
Main fuel used	Natural gas
Efficiency	84 %

Source: LG Chem Ltd. & Manufacturer

Table 2. Burner specification

Description	Specification
Maker	Hamworthy
Model	DF 505
Type	Manifold & Spud
Burning Capacity	
Max	1,405 (Nm ³ /hr)
MCR	1,338 (Nm ³ /hr)
Min	267 (Nm ³ /hr)

Source: Hamworthy Combustion

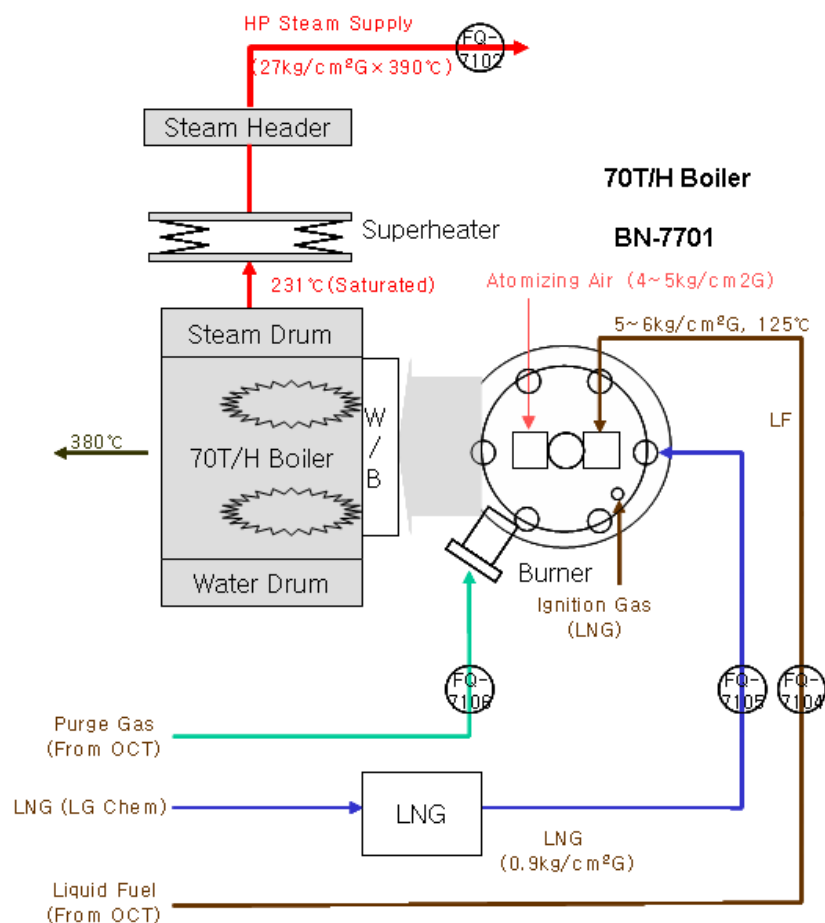


Figure 1. Layout of Boiler

A.5. Title, reference and version of the baseline and monitoring methodology applied to the project activity:

In accordance with Appendix B of the simplified modalities and procedures for small-scale clean development mechanism project activities ("SSC M&P"), the project falls under the following type and category:

Type III: Other project activities
Category B: Switching fossil fuels (Version 12)
Sectoral Scope 1 – Energy industries (renewable - / non-renewable sources)

A.6. Registration date of the project activity:

04/06/2009

A.7. Crediting period of the project activity and related information (start date and choice of crediting period):

The chosen crediting period is: 10 years (fixed)
The start date of the crediting period is: 04/06/2009

A.8. Name of responsible person(s)/entity(ies):

Clean Energy Finance Committee
Mitsubishi UFJ Morgan Stanley Securities Co., Ltd.
5th Floor, Toyosu Front,
3-2-20 Toyosu, Koto-ku,
Tokyo, 135-0061, Japan
Tel: +81-3-6213-6860 Fax: +81-3-6213-6175
Email: watanabe-hajime@sc.mufg.jp

SECTION B. Implementation of the project activity

B.1. Implementation status of the project activity

1. The starting date of the project activity was 21/06/2006 and commercial operation started on 20/11/2006 following retrofit of the boilers.
2. The first monitoring period is from 04/06/2009 to 23/02/2011.
3. The plant was offline for 32 days.
4. The outages were due to boiler cleaning or turn around (annual plant shutdown for maintenance).

There was no event during the monitoring period that had an impact on the applicability of the methodology.

B.2. Revision of the monitoring plan

There has been no revision to the monitoring plan.

B.3. Request for deviation applied to this monitoring period

No deviation has been applied to the monitoring period.

B.4. Notification or request of approval of changes

There is no notification or request of approval of changes from the project activity as described in the registered CDM-PDD.

SECTION C. Description of the monitoring system

LG Chem has organized an Operating and Monitoring Team, as per the PDD, which composes a manager and operators. The manager is responsible for monitoring and archiving all data associated with items depicted in the PDD monitoring plan. Operators working under the manager are assigned to the task of monitoring the different parameters on a timely basis as well as recording and archiving data in an orderly manner. All data collected as part of the monitoring plan will be archived electronically and be kept at least two (2) years after the end of the crediting period. Monitoring reports are reviewed by the manager on a monthly basis in order to ensure that the Project activity meets all requirements.

1. Allocation of Project management responsibilities

The management and operation of the Project is the responsibility of LG Chem, the Project operator. Ensuring the environmental credibility of the Project through accurate and systematic monitoring of the Project's implementation and operation for the purpose of achieving trustworthy CERs is the key responsibility and accountability of the operator.

2. Management and operational systems

The project developers have implemented a management and operational system that meets the requirements of the Project. This includes:

2.1 Data handling

- The establishment of a transparent system for the collection, computation and storage of data, including adequate record keeping and data monitoring systems.

2.2 Quality assurance

- LG Chem has designated a manager to be accountable for the generation of CERs including monitoring, record keeping, computation of CERs, audits and verification. The manager officially sign-offs on all GHG Emission worksheets.
- The manager follows well-defined protocols and routine procedures, with good, professional data entry, extraction and reporting are undertaken to maximise transparency of data archiving.
- Proper management processes and recording of all official data is undertaken.

2.3 Training

- Internal training is made available to operational staff to enable them to undertake the tasks required by the MP.

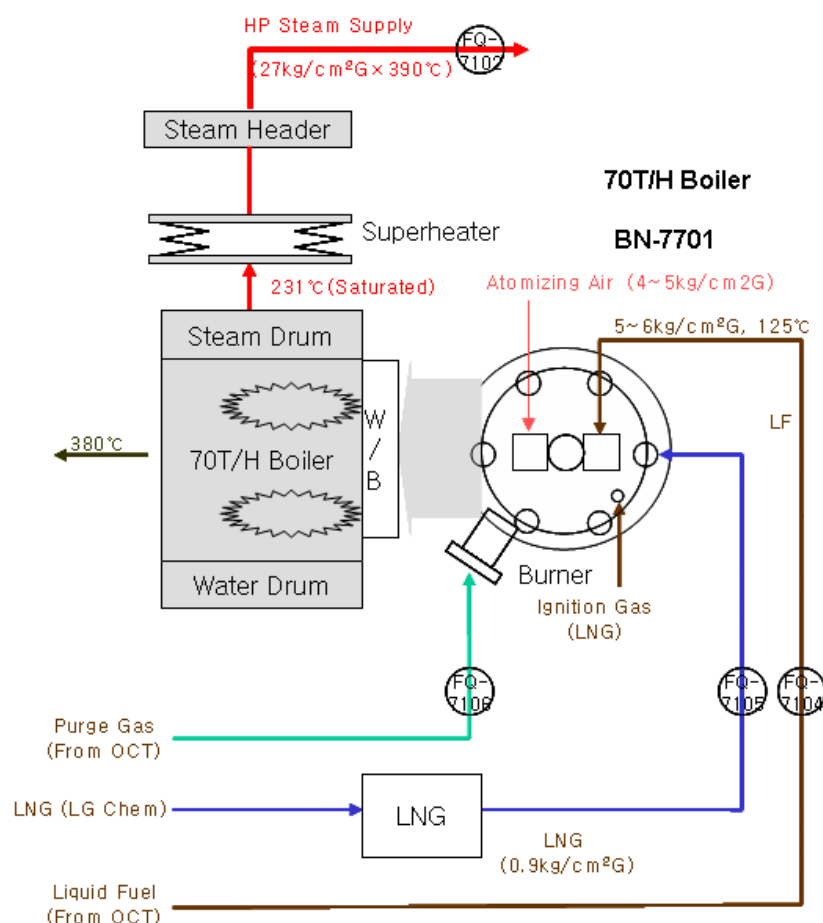


Figure 2. All relevant project monitoring points

SECTION D. Data and parameters

D.1. Data and parameters determined at registration and not monitored during the monitoring period, including default values and factors

Data / Parameter:	$EF_{NG,CO2}$
Data unit:	tCO ₂ /TJ
Description:	CO ₂ emission factor of the natural gas combusted
Source of data used:	2006 IPCC Guidelines for National Greenhouse Gas Inventories
Value(s) :	56.1
Indicate what the data are used for (Baseline/ Project/ Leakage emission calculations)	Project emission calculations
Additional comment:	The value is set ex-ante

Data / Parameter:	$FF_{baseline}$
Data unit:	Liter
Description:	Quantity of bunker fuel oil C combusted in the baseline situation
Source of data used:	LG Chem.
Value(s) :	70,730,291
Indicate what the data are	Baseline emission calculations

used for (Baseline/ Project/ Leakage emission calculations)	
Additional comment:	The value is set ex-ante. 3 years data prior to the project implementation (from 1 st , November 2003 to 31 st , October 2006) is used.

Data / Parameter:	$NCV_{baseline}$
Data unit:	TJ/liter
Description:	Net calorific value of bunker fuel oil C
Source of data used:	Standard Manual for Calorific Value (current version revised on 4 th , September 2006) approved by Ministry of Knowledge Economy / Korea Energy Management Corporation
Value(s) :	39.1×10^{-6}
Indicate what the data are used for (Baseline/ Project/ Leakage emission calculations)	Baseline emission calculations
Additional comment:	The value is set ex-ante

Data / Parameter:	$EF_{baseline,CO2}$
Data unit:	tCO ₂ /TJ
Description:	CO ₂ emission factor of bunker fuel oil C
Source of data used:	2006 IPCC Guidelines for National Greenhouse Gas Inventories
Value(s) :	77.4
Indicate what the data are used for (Baseline/ Project/ Leakage emission calculations)	Baseline emission calculations
Additional comment:	The value is set ex-ante

Data / Parameter:	$Q_{total,baseline}$
Data unit:	TJ
Description:	Total quantity of steam generated by bunker fuel oil C, purge gas and by-product liquid fuel in the baseline situation
Source of data used:	LG Chem.
Value(s) :	3,701.09
Indicate what the data are used for (Baseline/ Project/ Leakage emission calculations)	Baseline emission calculations
Additional comment:	The value is set ex-ante. 3 years data prior to the project implementation (from 1 st , November 2003 to 31 st , October 2006) is used. LG Chem produces superheated steam at 27 atm, 390 °C. The enthalpy of the superheated steam is 767.7kcal/kg of steam according to the steam table (Spirax Sarco: http://www.spiraxsarco.com/resources/steam-tables.asp). The temperature of the feed water is 104 °C.

Data / Parameter:	$PG_{baseline}$
Data unit:	Nm ³
Description:	Quantity of purge gas combusted in the boiler in the baseline situation
Source of data used:	LG Chem.
Value(s) :	13,203,959

Indicate what the data are used for (Baseline/ Project/ Leakage emission calculations)	Baseline emission calculations
Additional comment:	The value is set ex-ante. 3 years data prior to the project implementation (from 1 st , November 2003 to 31 st , October 2006) is used.

Data / Parameter:	$LF_{baseline}$
Data unit:	liter
Description:	Quantity of by-product liquid fuel combusted in the boiler in the baseline situation
Source of data used:	LG Chem.
Value(s) :	26,297,017
Indicate what the data are used for (Baseline/ Project/ Leakage emission calculations)	Baseline emission calculations
Additional comment:	The value is set ex-ante. 3 years data prior to the project implementation (from 1 st , November 2003 to 31 st , October 2006) is used.

Data / Parameter:	$NCV_{PG,baseline}$
Data unit:	TJ/Nm ³
Description:	Net calorific value of purge gas
Source of data used:	LG Chem
Value(s) :	52.15×10^{-6}
Indicate what the data are used for (Baseline/ Project/ Leakage emission calculations)	Baseline emission calculations
Additional comment:	The value is set ex-ante. 3 years data prior to the project implementation (from 1 st , November 2003 to 31 st , October 2006) is used.

Data / Parameter:	$NCV_{LF,baseline}$
Data unit:	TJ/liter
Description:	Net calorific value of by-product liquid fuel
Source of data used:	LG Chem
Value(s) :	30.576×10^{-6}
Indicate what the data are used for (Baseline/ Project/ Leakage emission calculations)	Baseline emission calculations
Additional comment:	The value is set ex-ante. Due to the absence of the reliable data for the period of 3 year prior to the project implementation (from 1 st , November 2003 to 31 st , October 2006) does not exist, the data recently measured by the independent laboratory is used.

D.2. Data and parameters monitored

Data / Parameter:	FF _{project,y}	
Data unit:	Nm ³	
Description:	Quantity of natural gas combusted in the project boiler during the year, y	
Measured /Calculated /Default:	Measured	
Source of data:	On-site measurement	
Value(s) of monitored parameter:	21,401,607	
Indicate what the data are used for (Baseline/ Project/ Leakage emission calculations)	Project emission calculations	
Monitoring equipment (type, accuracy class, serial number, calibration frequency, date of last calibration, validity)		
	Type	True RMS Voltmeter
	Accuracy Class	±2.0%
	Serial Number	7105
	Calibration frequency	Yearly
	Date of last calibration	5-Nov-2010
	Validity	One Year
Measuring/ Reading/ Recording frequency:	Continuous	
Calculation method (if applicable):	N/A	
QA/QC procedures applied:	The meter (Tag No. FQ-7105) has been calibrated periodically and a calibration certificate has been issued. No erroneous measurement or malfunction was detected during the monitoring period. The amount of natural gas combusted will be double checked with the receipt of purchase.	

Data / Parameter:	$NCV_{NG,y}$	
Data unit:	TJ/Nm^3	
Description:	Net calorific value of natural gas in year, y	
Measured /Calculated /Default:	Measured	
Source of data:	Standard Manual for Calorific Value	
Value(s) of monitored parameter:	40.0×10^{-6}	
Indicate what the data are used for (Baseline/ Project/ Leakage emission calculations)	Project emission calculations	
Monitoring equipment (type, accuracy class, serial number, calibration frequency, date of last calibration, validity)	N/A	
Measuring/ Reading/ Recording frequency:	Yearly	
Calculation method (if applicable):	N/A	

applicable):	
QA/QC procedures applied:	The value is from the “Standard Manual for Calorific Value” (current version revised on 4 th , September 2006) approved by Ministry of Knowledge Economy / Korea Energy Management Corporation.

Data / Parameter:	$Q_{total,y}$												
Data unit:	TJ												
Description:	Total quantity of steam generated by natural gas, purge gas and by-product liquid fuel in the project boiler during the year, y												
Measured /Calculated /Default:	Measured												
Source of data:	On-site measurement												
Value(s) of monitored parameter:	1,549												
Indicate what the data are used for (Baseline/ Project/ Leakage emission calculations)	Baseline emission calculations												
Monitoring equipment (type, accuracy class, serial number, calibration frequency, date of last calibration, validity)	<table border="1"> <tr> <td>Type</td><td>Digital Manometer and Multimeter</td></tr> <tr> <td>Accuracy Class</td><td>±0.2%</td></tr> <tr> <td>Serial Number</td><td>7102</td></tr> <tr> <td>Calibration frequency</td><td>Yearly</td></tr> <tr> <td>Date of last calibration</td><td>6-Nov-2010</td></tr> <tr> <td>Validity</td><td>One Year</td></tr> </table>	Type	Digital Manometer and Multimeter	Accuracy Class	±0.2%	Serial Number	7102	Calibration frequency	Yearly	Date of last calibration	6-Nov-2010	Validity	One Year
Type	Digital Manometer and Multimeter												
Accuracy Class	±0.2%												
Serial Number	7102												
Calibration frequency	Yearly												
Date of last calibration	6-Nov-2010												
Validity	One Year												
Measuring/ Reading/ Recording frequency:	Continuous												
Calculation method (if applicable):	N/A												
QA/QC procedures applied:	The meter (Tag No. FIC-7102) has been calibrated periodically and a calibration certificate has been issued. No erroneous measurement or malfunction was detected during the monitoring period.												

Data / Parameter:	PG_y
Data unit:	Nm ³
Description:	Quantity of purge gas combusted in the project boiler during the year, y
Measured /Calculated /Default:	Measured
Source of data:	On-site measurement
Value(s) of monitored parameter:	12,079,729
Indicate what the data are used for (Baseline/ Project/ Leakage emission calculations)	Baseline emission calculations

Monitoring equipment (type, accuracy class, serial number, calibration frequency, date of last calibration, validity)	Type	Digital Manometer and Multimeter
	Accuracy Class	±0.2%
	Serial Number	7106
	Calibration frequency	Yearly
	Date of last calibration	6-Nov-2010
	Validity	One Year
Measuring/ Reading/ Recording frequency:	Continuous	
Calculation method (if applicable):	N/A	
QA/QC procedures applied:	The meters (Tag No. FIC-7106) has been calibrated periodically and a calibration certificate has been issued. No erroneous measurement or malfunction was detected during the monitoring period.	

Data / Parameter:	LF_y	
Data unit:	Liter	
Description:	Quantity of by-product liquid fuel combusted in the project boiler during the year, y	
Measured /Calculated /Default:	Default	
Source of data:	On-site measurement	
Value(s) of monitored parameter:	14,815,842	
Indicate what the data are used for (Baseline/ Project/ Leakage emission calculations)	Baseline emission calculations	
Monitoring equipment (type, accuracy class, serial number, calibration frequency, date of last calibration, validity)	Type	Digital Manometer and Multimeter
	Accuracy Class	C
	Serial Number	7104
	Calibration frequency	Calibrate when/if necessary
	Date of last calibration	24-Aug-2004
	Validity	Calibrate when/if necessary
Measuring/ Reading/ Recording frequency:	Continuous	
Calculation method (if applicable):	N/A	
QA/QC procedures applied:	The meters (Tag No. FQ-7104) has been calibrated and a calibration certificate has been issued. No erroneous measurement or malfunction was detected during the monitoring period.	

Data / Parameter:	$NCV_{WG,y}$
Data unit:	TJ/Nm ³
Description:	Net calorific value of purge gas
Measured /Calculated /Default:	Measured
Source of data:	On-site measurement

Value(s) of monitored parameter:	46.10×10^{-6}
Indicate what the data are used for (Baseline/ Project/ Leakage emission calculations)	Baseline emission calculations
Monitoring equipment (type, accuracy class, serial number, calibration frequency, date of last calibration, validity)	N/A
Measuring/ Reading/ Recording frequency:	Monitored quarterly and yearly average value used
Calculation method (if applicable):	N/A
QA/QC procedures applied:	-

Data / Parameter:	$NCV_{LF,y}$
Data unit:	TJ/liter
Description:	Net calorific value of by-product liquid fuel
Measured /Calculated /Default:	Measured
Source of data:	On-site measurement
Value(s) of monitored parameter:	30.02×10^{-6}
Indicate what the data are used for (Baseline/ Project/ Leakage emission calculations)	Baseline emission calculations
Monitoring equipment (type, accuracy class, serial number, calibration frequency, date of last calibration, validity)	N/A
Measuring/ Reading/ Recording frequency:	Monitored quarterly and yearly average value used
Calculation method (if applicable):	N/A
QA/QC procedures applied:	-

Data / Parameter:	$\epsilon_{project,y}$
Data unit:	%
Description:	Energy efficiency of the boiler during the year, y
Measured /Calculated /Default:	Calculated
Source of data:	Calculated using measured data
Value(s) of monitored parameter:	84
Indicate what the data are used for (Baseline/ Project/ Leakage emission calculations)	Project emission calculations
Monitoring equipment (type, accuracy class, serial	N/A

number, calibration frequency, date of last calibration, validity)	
Measuring/ Reading/ Recording frequency:	Quarterly
Calculation method (if applicable):	The energy efficiency of the boiler will be calculated by the direct method (dividing the net heat generation by the energy content of the fuels fired).
QA/QC procedures applied:	The meters used for monitoring of the relevant parameters (steam generation, fuel consumption) will be calibrated periodically. Once the erroneous measurement or malfunction is detected, corrective actions will be taken by LG Chem.

SECTION E. Emission reductions calculation

E.1. Baseline emissions calculation

Baseline emission factor for the baseline situation, $EF_{baseline}$

$$\begin{aligned}
 EF_{baseline} &= FF_{baseline} \times EF_{baseline, CO_2} \times NCV_{baseline} / Q_{baseline} \\
 &= 70,730,291 (liter) \times 77.4 (tCO_2 / TJ) \times 39.1 \times 10^{-6} (TJ / liter) / 2,403.73 (TJ) \\
 &= 89.05 tCO_2 / TJ
 \end{aligned}$$

Where:

$FF_{baseline}$	Quantity of bunker fuel oil C combusted in the baseline situation (liter)
$EF_{baseline, CO_2}$	CO ₂ emission factor of bunker fuel oil C (tCO ₂ /TJ)
$NCV_{baseline}$	Net calorific value of bunker fuel oil C (TJ/liter)
$Q_{baseline}$	Quantity of steam generated by bunker fuel oil C in the baseline situation (TJ)

For quantity of bunker fuel oil C combusted, $FF_{baseline}$, and quantity of steam generated by bunker fuel oil C, $Q_{baseline}$, 3 years data prior to project implementation (from 1st, November, 2003 to 31st, October 2006) is used.

$$\begin{aligned}
 Q_{baseline} &= Q_{total, baseline} \times \frac{FF_{baseline} \times NCV_{baseline}}{(FF_{baseline} \times NCV_{baseline} + PG_{baseline} \times NCV_{PG, baseline} + LF_{baseline} \times NCV_{LF, baseline})} \\
 &= 3,701.09 \times \frac{70,730,291 \times 39.1 \times 10^{-6}}{(70,730,291 \times 39.1 \times 10^{-6} + 13,203,959 \times 52.15 \times 10^{-6} + 26,297,017 \times 30.576 \times 10^{-6})} \\
 &= 2,403.73 TJ
 \end{aligned}$$

Where:

$Q_{total, baseline}$	Total quantity of steam generated by bunker fuel oil C, waste gas and by-product liquid fuel in the baseline situation (TJ)
$PG_{baseline}$	Quantity of purge gas combusted in the boiler in the baseline situation (Nm ³)

$NCV_{PG,baseline}$	Net calorific value of purge gas (TJ/Nm ³)
$LF_{baseline}$	Quantity of by-product liquid fuel combusted in the boiler in the baseline situation (liter)
$NCV_{LF,baseline}$	Net calorific value of by-product liquid fuel (TJ/liter)

Quantity of steam generated by natural gas, Q_y

Since purge gas and by-product liquid fuel are also combusted in the boiler, the quantity of steam generated by natural gas, Q_y , is calculated based on the proportion of fuel used as follows:

$$Q_y = Q_{total,y} \times \frac{FF_{project,y} \times NCV_{NG,y}}{(FF_{project,y} \times NCV_{NG,y} + PG_y \times NCV_{WG,y} + LF_y \times NCV_{LF,y})}$$

$$= 1,549 \times \frac{21,401,607 \times 40.0 \times 10^{-6}}{(21,401,607 \times 40.0 \times 10^{-6} + 12,079,729 \times 46.1 \times 10^{-6} + 14,815,842 \times 30.02 \times 10^{-6})}$$

$$= 713.75 TJ$$

Where:

$Q_{total,y}$	Total quantity of steam generated by natural gas, purge gas and by-product liquid fuel during year, y (TJ)
$FF_{project,y}$	Quantity of natural gas combusted in the project boiler during the year, y (Nm ³)
PG_y	Quantity of purge gas combusted in the boiler during year, y (Nm ³)
$NCV_{PG,y}$	Net calorific value of purge gas (TJ/Nm ³)
LF_y	Quantity of by-product liquid fuel combusted in the boiler during year, y (liter)
$NCV_{LF,y}$	Net calorific value of by-product liquid fuel (TJ/liter)

Baseline emission, BE_y

$$BE_y = EF_{baseline} \times Q_y$$

$$= 89.05 (tCO_2 / TJ) \times 713.75 (TJ)$$

$$= 63,559 tCO_2$$

Where:

BE_y	Baseline emission during the year y (tCO ₂ e)
$EF_{baseline}$	Baseline emission factor for the baseline situation (tCO ₂ /TJ)
Q_y	Quantity of steam generated by natural gas (TJ)

E.2. Project emissions calculation

Project emissions consist of those emissions related with the use of fossil fuel after the fuel switch. Project emissions are calculated as follows:

$$\begin{aligned}
PE_y &= FF_{project,y} \times NCV_{NG,y} \times EF_{NG,CO_2} \\
&= 21,401,607 \text{ (Nm}^3\text{)} \times 40.0 \times 10^{-6} \text{ (TJ/Nm}^3\text{)} \times 56.1 \text{ (tCO}_2\text{/TJ)} \\
&= 48,025 \text{ tCO}_2
\end{aligned}$$

Where:

PE_y	Project emissions during the year, y (tCO ₂ e)
$FF_{project,y}$	Quantity of natural gas combusted in the project boiler during the year, y (Nm ³)
$NCV_{NG,y}$	Net calorific value of the natural gas combusted in year, y (TJ/Nm ³)
EF_{NG,CO_2}	CO ₂ emission factor of the natural gas combusted in the project boiler (tCO ₂ /TJ)

E.3. Leakage calculation

As described in AMS III.B, no leakage calculation is required.

E.4. Emission reductions calculation / table

The emission reduction calculation of the first monitoring period (04/06/2009 – 23/02/2011) is calculated as follows:

$$\begin{aligned}
ER_y &= BE_y - PE_y \\
&= 63,559 \text{ tCO}_2\text{e} - 48,025 \text{ tCO}_2\text{e} \\
&= 15,534 \text{ tCO}_2\text{e}
\end{aligned}$$

Where:

ER_y	Total emissions reductions of the project activity during the year, y (tCO ₂ e)
BE_y	Total baseline emissions during the year, y (tCO ₂ e)
PE_y	Total project emissions during the year, y (tCO ₂ e)

E.5. Comparison of actual emission reductions with estimates in the CDM-PDD

A comparison of actual emission reductions during the monitoring period with the estimates in the registered CDM-PDD is shown below:

Item	Values applied in ex-ante calculation of the registered CDM-PDD	Actual values reached during the monitoring period
Emission reductions (tCO₂e) (annual: 365 days)	19,635	9,014*
Emission reductions (tCO₂e) (monitored: 629 days)	33,836	15,534

*Actual value reached for the monitored period (629 days) is adjusted accordingly for comparison with ex-ante annual (365 days) calculation of the registered PDD.

E.6. Remarks on difference from estimated value in the PDD

The actual emission reductions reached during the monitoring period has decreased from the value estimated in the registered PDD.

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History of the document

Version	Date	Nature of revision
01	EB 54, Annex 34 28 May 2010	Initial adoption.
Decision Class: Regulatory Document Type: Guideline, Form Business Function: Issuance		